

Catalytic activation of 3D printed AlSi10Mg Periodic Open Cellular Structures (POCSs) by combined dip/spin coating method for the intensification of ammonia synthesis

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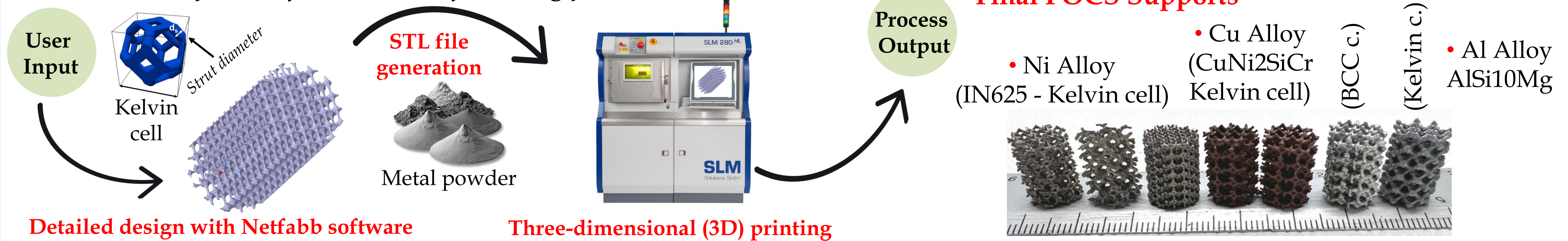
INTRODUCTION

The present work deals with the design, manufacturing (by Laser Powder Bed Fusion), characterization, and catalytic activation (by a wash-coating method) of Periodical Cellular Structures (POCS) 3D-printed in a cylindrical shape ($\varnothing = 1\text{cm}$, Length = 1.5 cm), in different materials (Al-, Cu-, Ni-alloys) and with various structural parameters (porosity, density, cell type and strut dimensions). The general aim is to intensify the ammonia synthesis throughout the development of structured catalysts with geometries that allow the integration with ammonia selective membranes in a membrane-based reactor to increase productivity at low temperatures (250-300°C) and pressure (20-25bar).

RESULTS

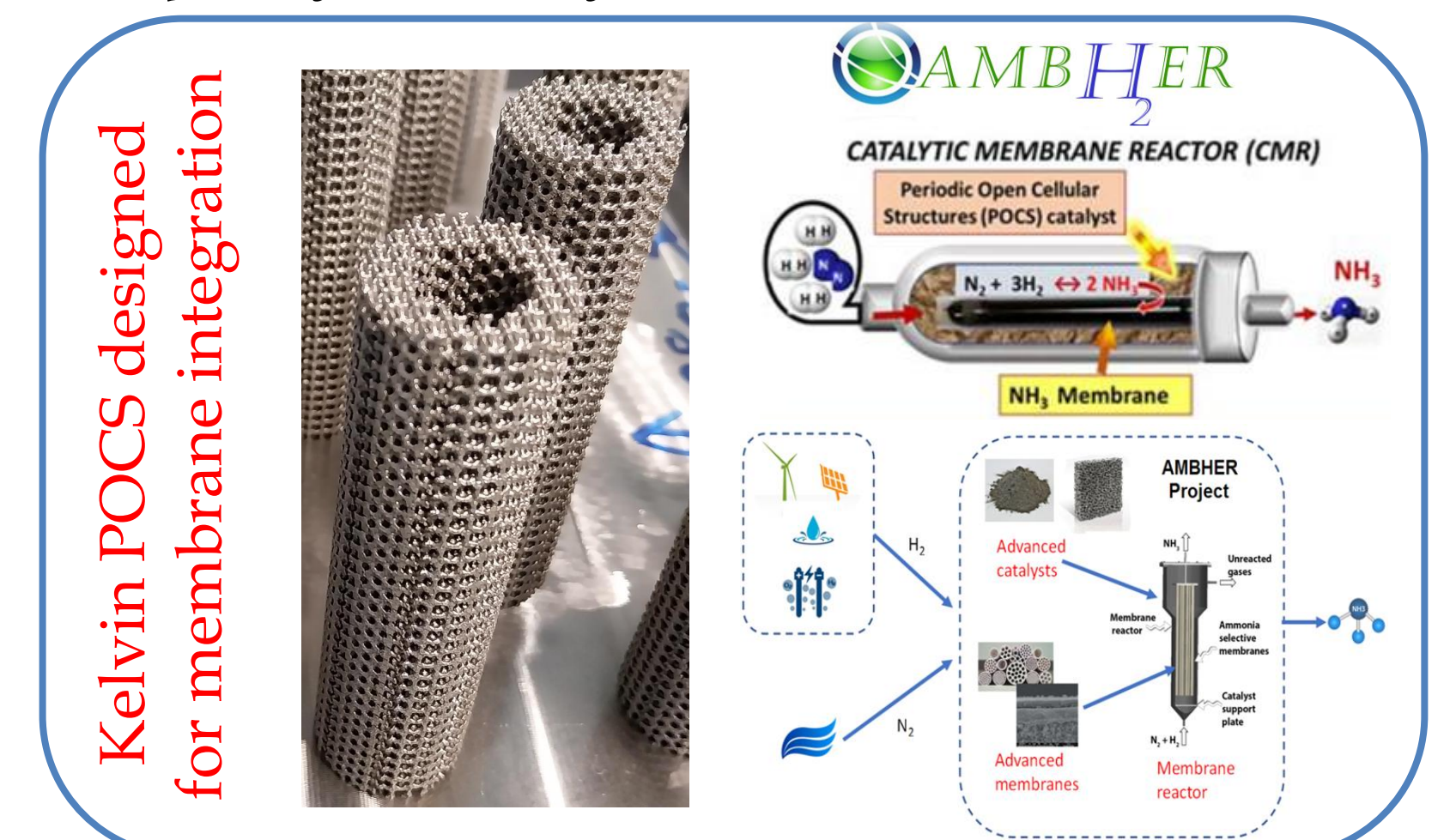
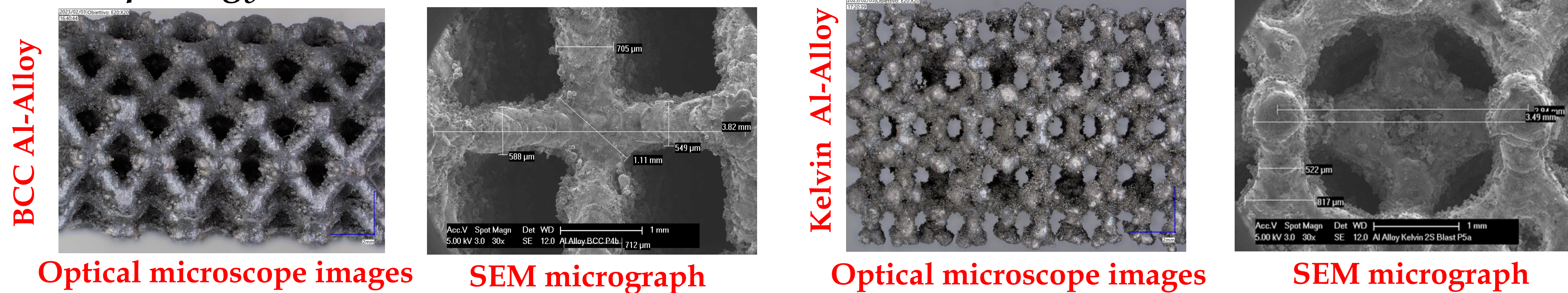
ADDITIVE MANUFACTURING (AM) fast, easy, highly accurate and productive, part of the digital industry...!!

Schematic sequence of POCS manufacturing process



POCS CHARACTERIZATION (AS BUILT)... complex geometry, high porosity and Specific Surface Area...!!

Morphology



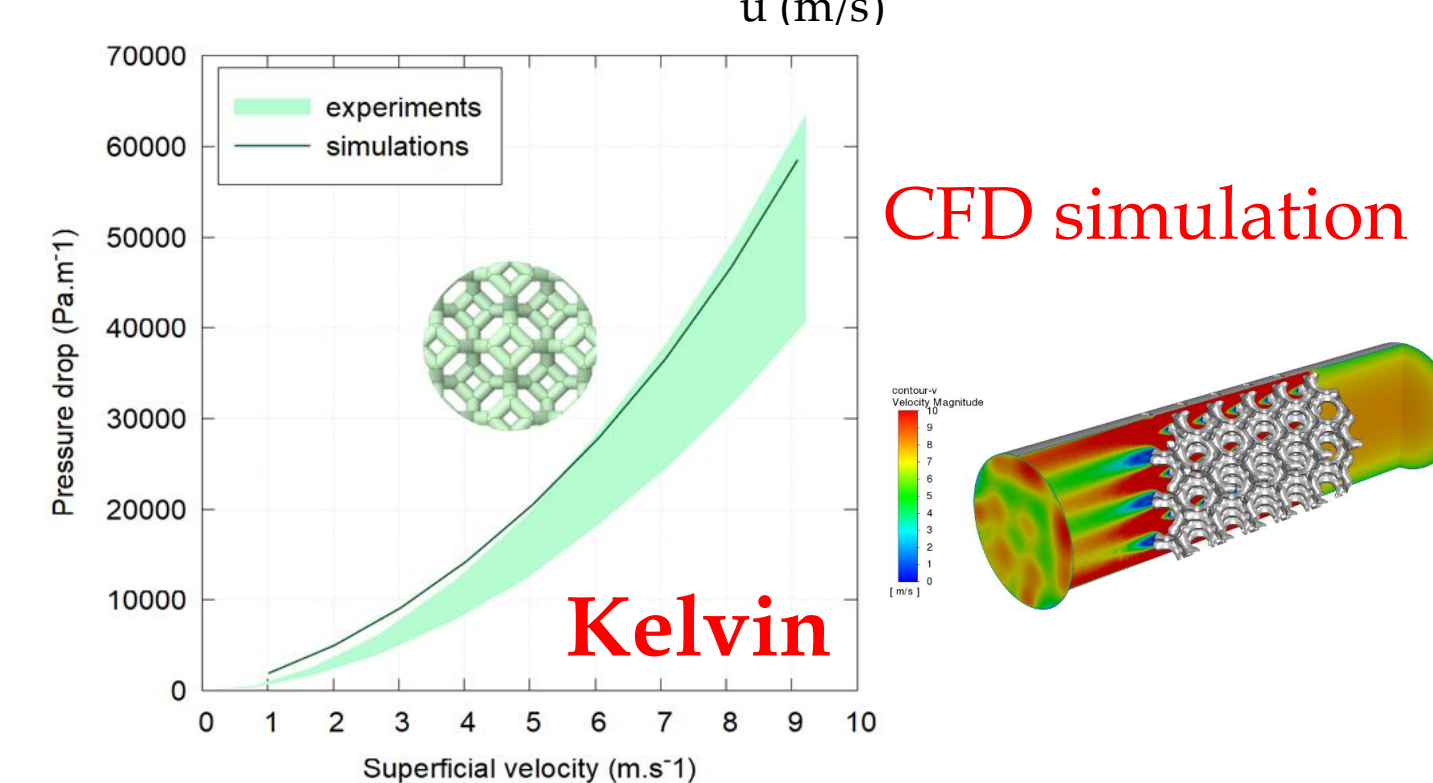
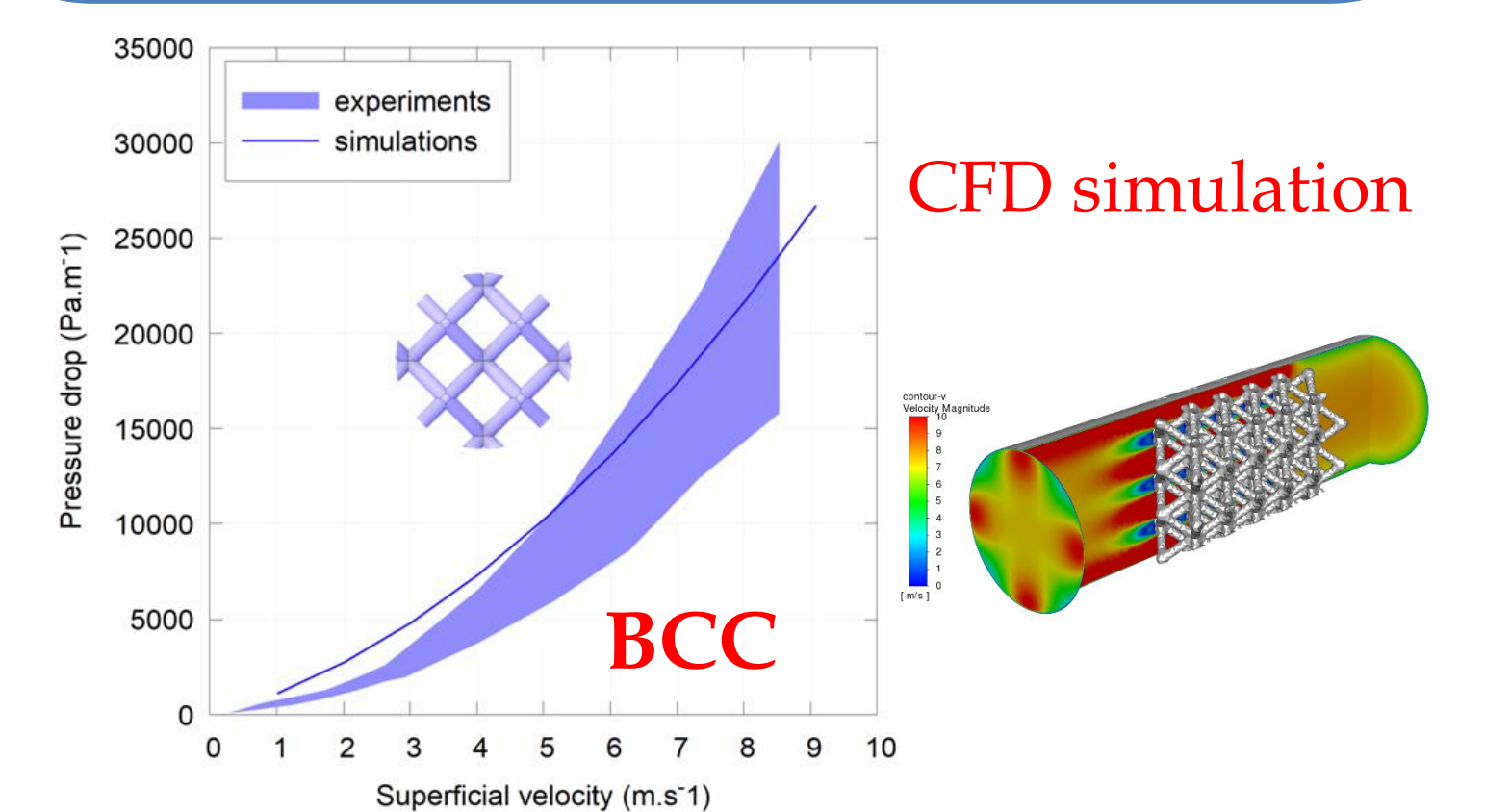
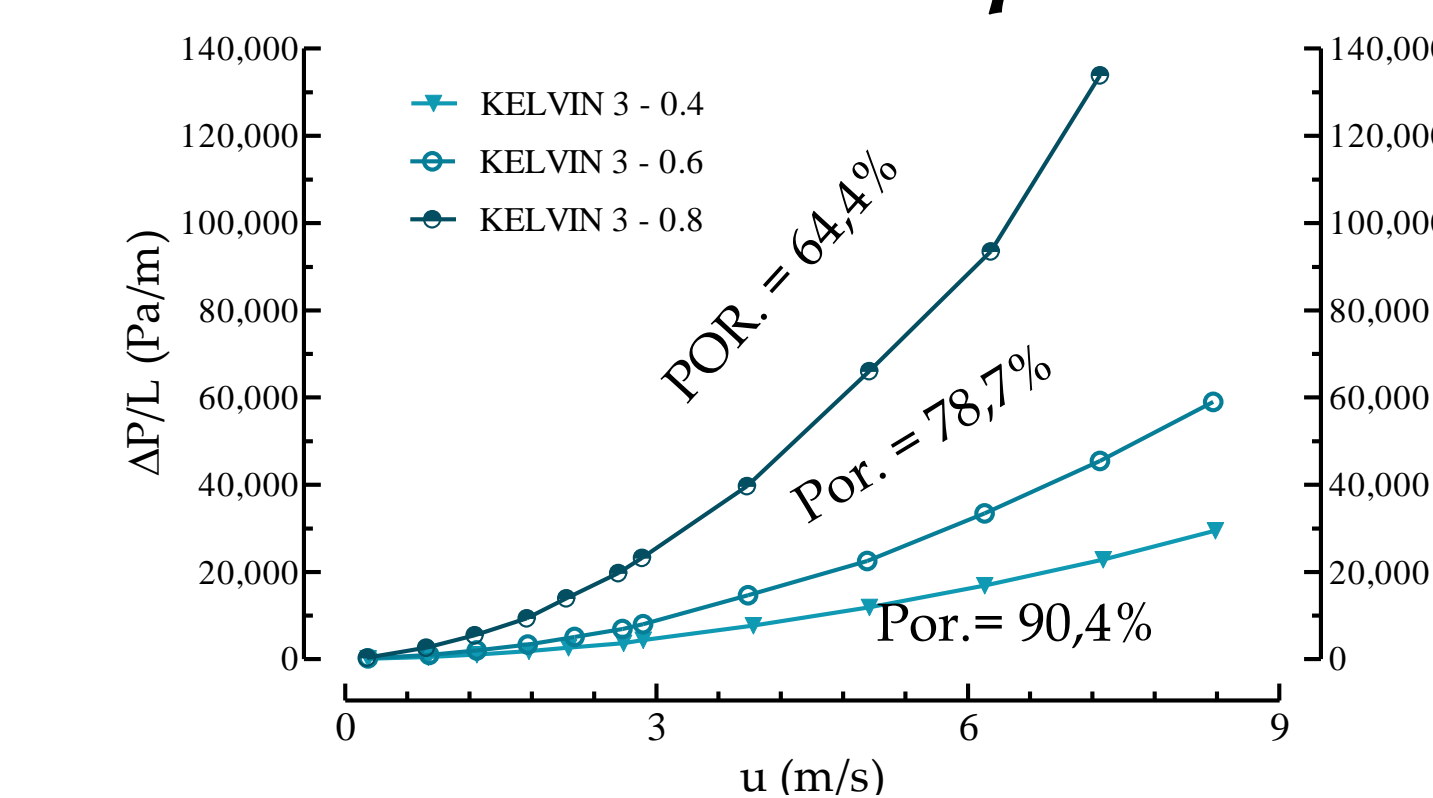
Summary of the Ni-alloy POCSs and related geometric features

Pressure drop

Cell type	Cell size (mm)	Strut diameter (mm)	** Solid Volume (cm ³)	** Solid density (g/cm ³)	Internal Surface area (cm ²)	** Porosity (%)	Geom. density (g/cm ³)	Specific surf. area (cm ² /cm ³)	Relative density
BCC	2 (2*)	0.4 (0.41*)	0.219	10.87	9.45	82.9	2.80	87.03	0.17
BCC	2 (2*)	0.6 (0.6*)	0.489	8.79	24.52	63.9	2.02	48.77	0.36
BCC	3 (3*)	0.4 (0.4*)	0.099	11.31	19.06	92.1	3.65	95.66	0.08
BCC	3 (3*)	0.6 (0.59*)	0.220	8.86	23.85	85.3	0.95	58.82	0.17
BCC	4 (4*)	0.6 (0.62*)	0.116	9.14	12.94	91.2	1.48	64.48	0.09
BCC	3 (3*)	0.8 (0.75*)	0.206	16.02	15.41	83.2	0.90	45.85	0.15
BCC	1.5(1.5*)	0.3 (0.3*)	0.212	12.08	7.48	83.3	2.80	115.66	0.17

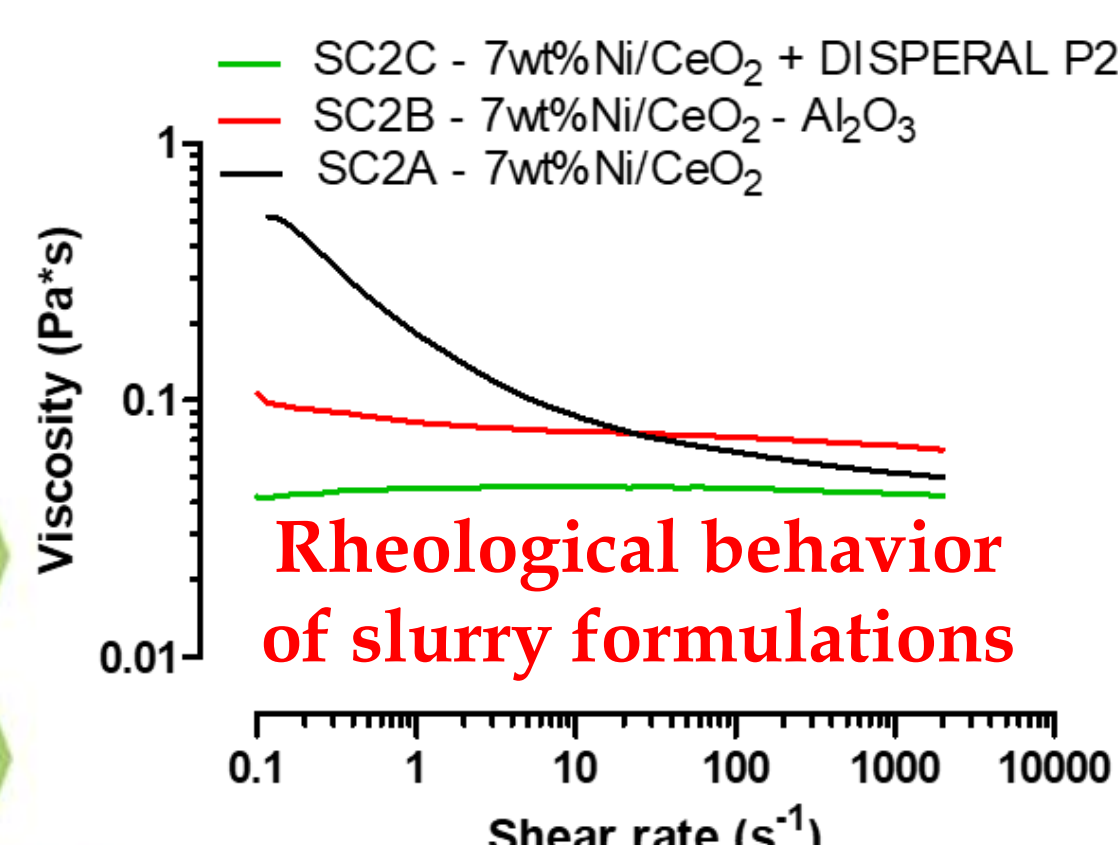
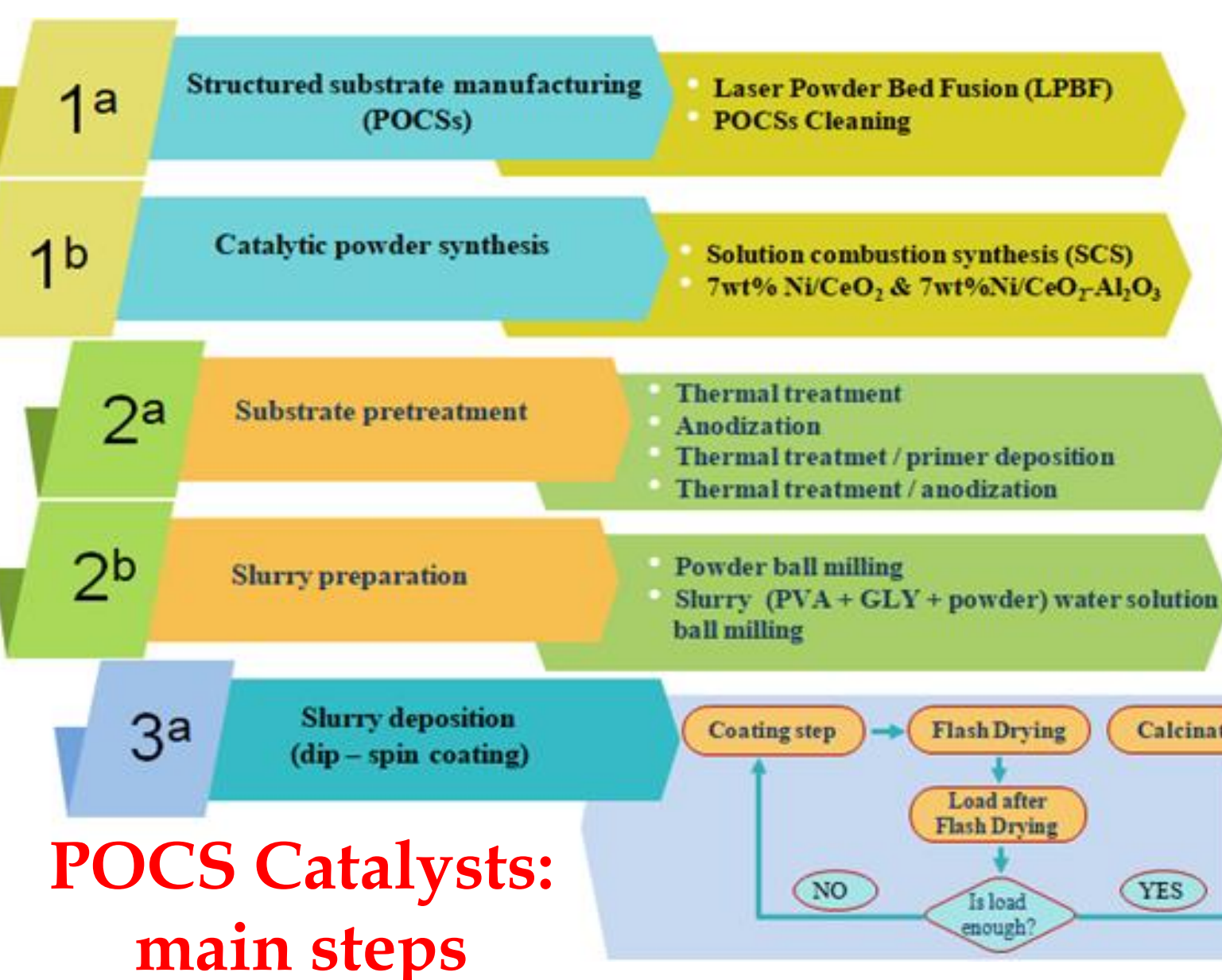
Cell type	Cell size (mm)	Strut diameter (mm)	** Solid Volume (cm ³)	** Solid density (g/cm ³)	Internal Surface area (cm ²)	** Porosity (%)	Geom. density (g/cm ³)	Specific surf. area (cm ² /cm ³)	Relative density
KELVIN	3 (3.04*)	0.4 (0.44*)	0.126	14.21	11.21	90.4	1.52	88.97	90.4
KELVIN	3 (3*)	0.6 (0.69*)	0.290	10.14	15.23	78.7	2.50	52.52	78.7
KELVIN	3 (3*)	0.8 (0.86*)	0.518	9.42	16.93	64.4	4.14	32.68	64.4
KELVIN	4 (4*)	0.6 (0.61*)	0.153	10.85	9.08	88.6	1.41	59.37	88.6

*Calculated from optical images, **Calculated from He pycnometer measurement

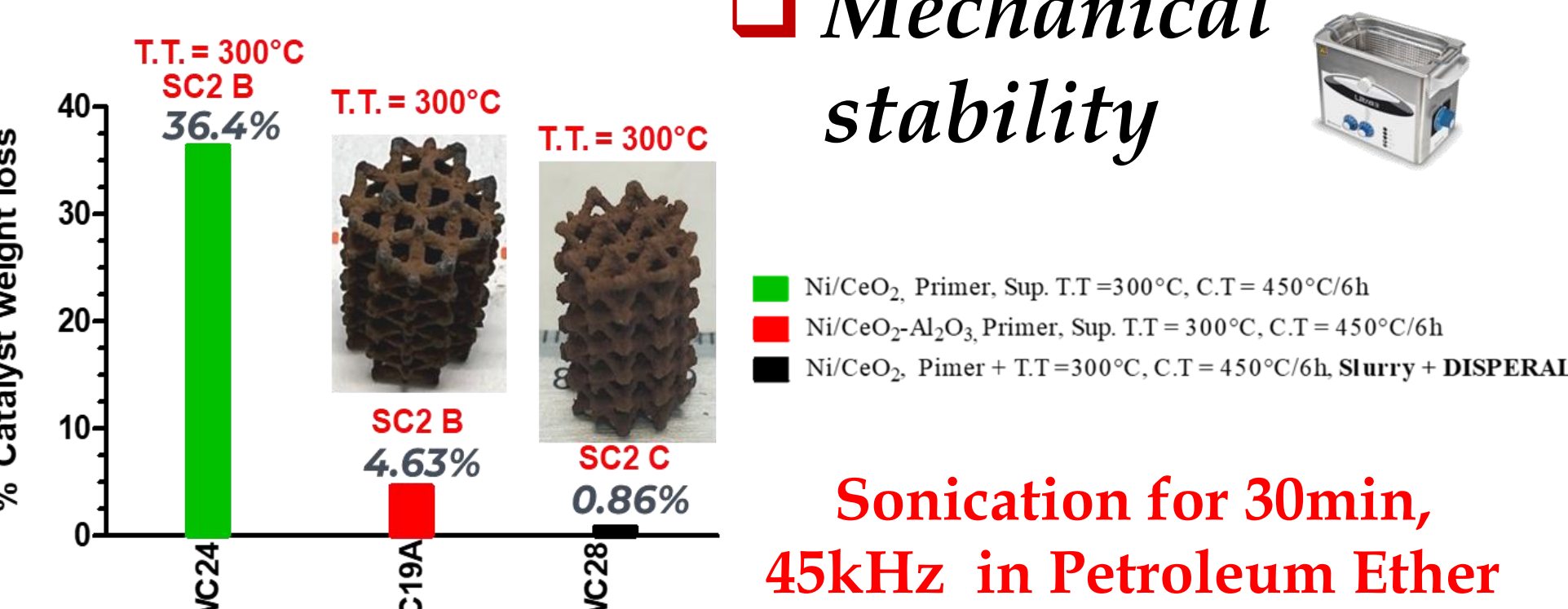
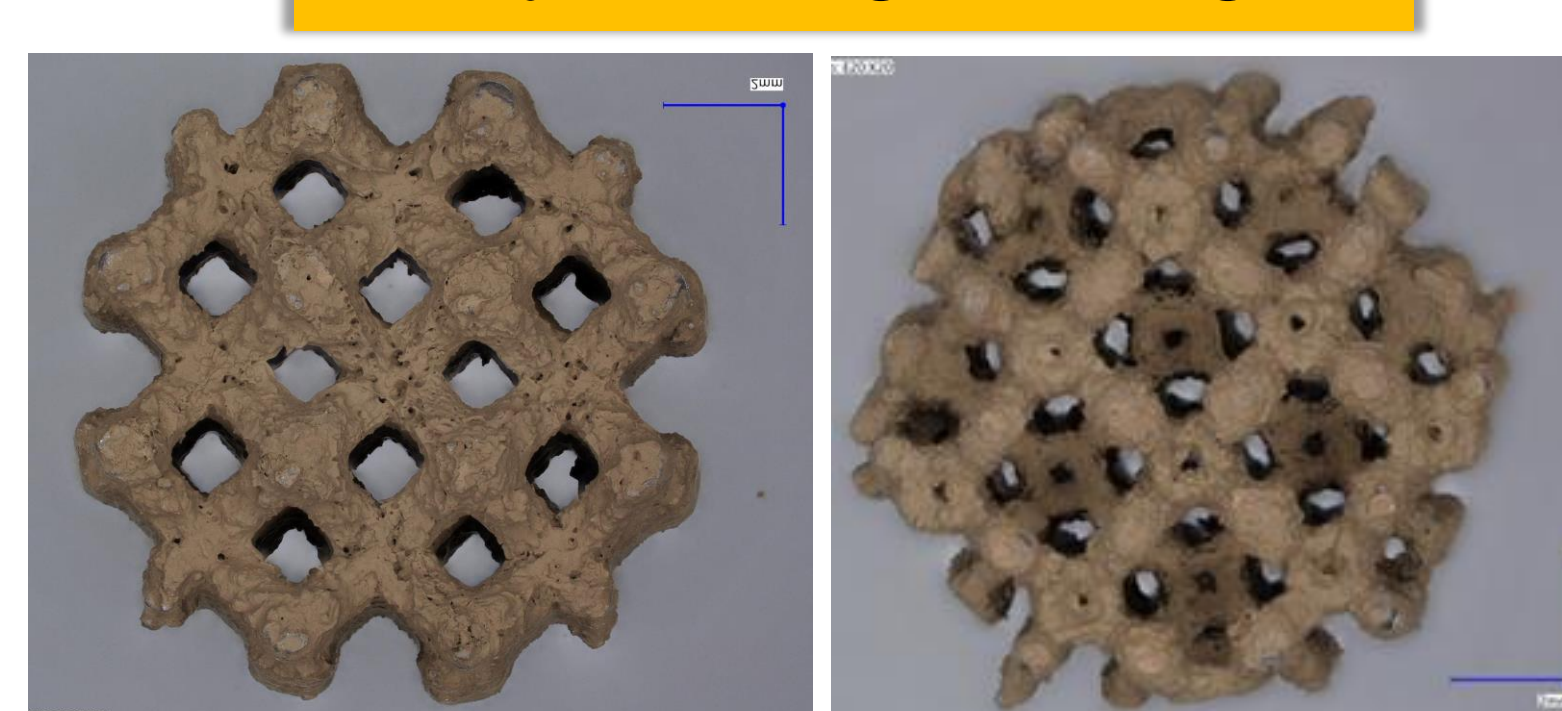


Influence of cell geometry and size, strut diameter and porosity

CATALYTIC ACTIVATION OF POCS... homogeneous layers, well anchored, no pore-clogging phenomena ...!!



Catalyst loading: 0.1-0.25 g/cm³

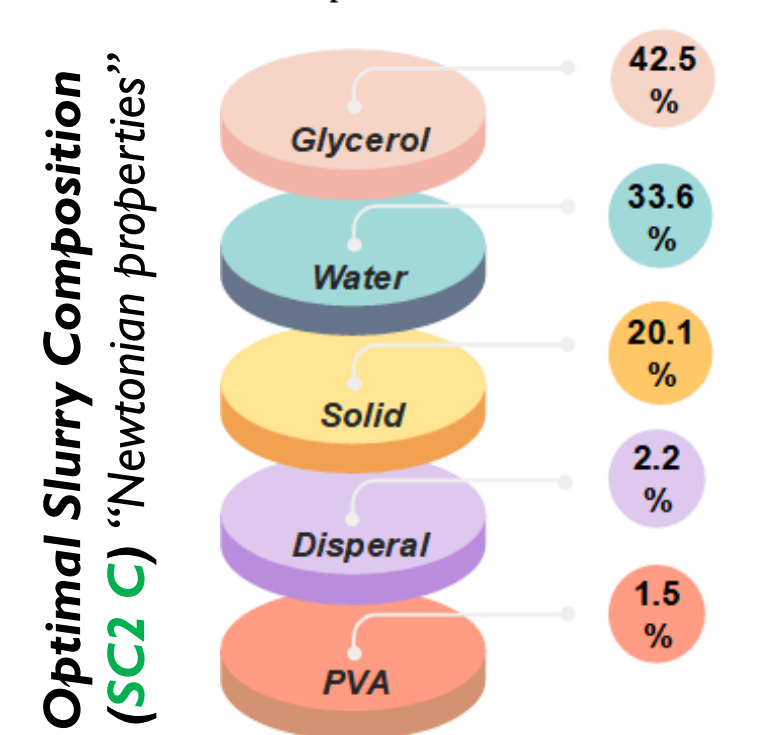


Mechanical stability

Sonication for 30min, 45kHz in Petroleum Ether

Composition of the different slurry prepared.

Slurry	Catalyst formulation	Powder catalyst (%)	Glycerol (%)	PVA (%)	Water (%)	Disperal P2® (%)
SC1	Ni/CeO ₂	24.03	45.65	1.49	28.83	-
SC2A	Ni/CeO ₂	22.40	42.50	1.50	33.60	-
SC3	Ni/CeO ₂	25.36	48.18	1.46	25.00	-
SC2B	Ni/CeO ₂ -Al ₂ O ₃	22.40	42.50	1.50	33.60	-
SC2C	Ni/CeO ₂	20.14	42.50	1.50	33.60	2.26



CONCLUSION

- AM is able to manufacture complex parts allowing more freedom of design optimization for catalytic reactors compared with traditional manufacturing techniques;
- The combined dip/spin coating method can be used to obtain POCS catalysts with homogeneous and stable catalytic layers (thickness $\approx 15\mu\text{m}$);
- The presence of anchoring points, the thermal or anodization pre-treatment (or both) of supports or the primer (DISPERAL P2) utilization (both in the slurry and coated on the supports) play a crucial role in achieving high mechanical stability;
- No pore-clogging phenomena were observed irrespective of the geometry used;
- The structured catalytic systems obtained by combining AM with the washcoating technique are characterized by higher porosity (88 -90%), higher SSA (50-115 cm²/cm³) and lower pressure drops with respect to the conventional packed bed reactor.

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