#### 9<sup>th</sup> High Temperature Solid Looping Cycles Network - Day 2: CLEANKER



9:10-9:25	Cleanker project overview - Maurizio Spinelli <sup>a</sup> , Martina Fantini <sup>b</sup> , Stefano Consonni <sup>c</sup> - <sup>a</sup> LEAP, <sup>b</sup> Eucore <sup>c</sup> PoliMI
9:25-10:10	Sorbent properties and lab scale tests for cement applications
	J. Carlos Abanades <sup>a</sup> , Borja Arias <sup>a</sup> , Monica Alonso <sup>a</sup> , Jose Ramon Fernandez <sup>a</sup> , Sandra Turrado <sup>a</sup> , Nico Mader <sup>b</sup> , Joerg Maier <sup>b</sup> - <sup>a</sup> CSIC-INCAR, <sup>b</sup> University of Stuttgart -
10:10-10:25	Cleanker pilot plant design - Jörg Hammerich, IKN GmbH -
10:25-10:55	<b>Cleanker pilot test results</b> - Francesco Magli <sup>a</sup> , Edoardo De Lena <sup>b</sup> , Riccardo Cremona <sup>c</sup> , Maurizio Spinelli <sup>b</sup> , Monica Alonso <sup>d</sup> , Nico Mader <sup>e</sup> , Marco Lindeman Lino <sup>f</sup> , Manuele Gatti <sup>c</sup> , Matteo C. Romano <sup>c</sup> <sup>a</sup> Buzzi Unicem SpA, <sup>b</sup> LEAP, <sup>c</sup> Politecnico di Milano, <sup>d</sup> CSIC-INCAR, <sup>e</sup> University of Stuttgart, <sup>f</sup> VDZ Technology gGmbH,
Coffee break	
11:15-11:35	Simulation and validation of reactor models of Cleanker Vernasca pilot
	Kari Myöhänen, Jouni Ritvanen - LUT University
11:35-12:05	Cleanker process analysis and retrofitting
	Edoardo De Lena <sup>a</sup> , Maurizio Spinelli <sup>a</sup> , Riccardo Cremona <sup>b</sup> , Matteo C. Romano <sup>b</sup> , Guido Pellegrino <sup>c</sup> , Ancelin Coulon <sup>d</sup> , Anna Kounina <sup>d</sup> - <sup>a</sup> LEAP, <sup>b</sup> Politecnico di Milano, <sup>c</sup> Italcementi-HeidelbergCement, <sup>d</sup> Quantis
12:05-12:25	Scale-up and economics for a full-size plant
	Jörg Hammerich <sup>a</sup> , Marco Lindeman Lino <sup>b</sup> , Kari Myöhänen <sup>c</sup> - <sup>a</sup> IKN GmbH, <sup>b</sup> VDZ Technology gGmbH, <sup>c</sup> LUT University
12:25-12:50	<b>CO<sub>2</sub> utilization, transport and storage study</b> Alla Shogenova <sup>a</sup> , Kazbulat Shogenov <sup>a</sup> , Mai Uibu <sup>a</sup> , Rein Kuusik <sup>a</sup> , Mustafa Cem Usta <sup>a</sup> , Daniela Gastaldi <sup>b</sup> , Fulvio Canonico <sup>b</sup> , Guido Pellegrino <sup>c</sup> - <sup>a</sup> Tallinn University of Technology, <sup>b</sup> Buzzi Unicem, <sup>c</sup> Italcementi-HeidelbergCement
12:50-13:10	Cleanker strategic conclusions - Matteo Romano <sup>a</sup> , Maurizio Spinelli <sup>b</sup> - <sup>a</sup> Politecnico di Milano, <sup>b</sup> LEAP
Lunch (13:30-14:15)	
14:15 – 19:00 Cleanker pilot plant visit	

#### 14:15 – 19:00 Cleanker pilot plant visit

- •14:15: Departure from Piacenza
- •15:15: Arrival at Vernasca cement plant
- •15:15-15:45: Introduction and preparation to the visit
- •15:45-16:30: Visit to the pilot plant and to the cement plant
- •16:30-17:00: End of the technical visit and coffee break
- •17:00-17:45: Presentation and final discussion (meeting room)
- •18:00: Departure from Vernasca (back to Piacenza)





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CLEAN clinKER by calcium looping or low-CO<sub>2</sub> cement

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# **CLEANKER Project Overview**

<u>M. Spinelli<sup>a</sup></u>, M. Fantini<sup>b</sup>, S. Consonni<sup>c</sup>

<sup>a</sup>LEAP (Laboratorio Energia e Ambiente Piacenza), <sup>b</sup>Eucore, <sup>c</sup>Politecnico di Milano,

#### 9<sup>th</sup> High Temperature Solid Looping Cycles Network (HTSLCN) Meeting Piacenza, Palazzo Farnese Day 2 - 15/03/2023





The ultimate objective of CLEANKER is **advancing the integrated Calcium-looping process for CO<sub>2</sub> capture in cement plants.** Main targets:

- install and operate a new demo system <u>at TRL 7</u> based on the <u>integrated CaL process</u>, connected to the Vernasca 1.300.000 ton/y cement plant, operated by BUZZI in Italy.
- demonstrate the <u>technical-economic feasibility</u> of the integrated CaL process in retrofitted large scale cement plants through process modelling and scale-up study.
- demonstrate the CO<sub>2</sub> mineralization of the captured CO<sub>2</sub> (inorganic materials, small-scale pilot reactor)





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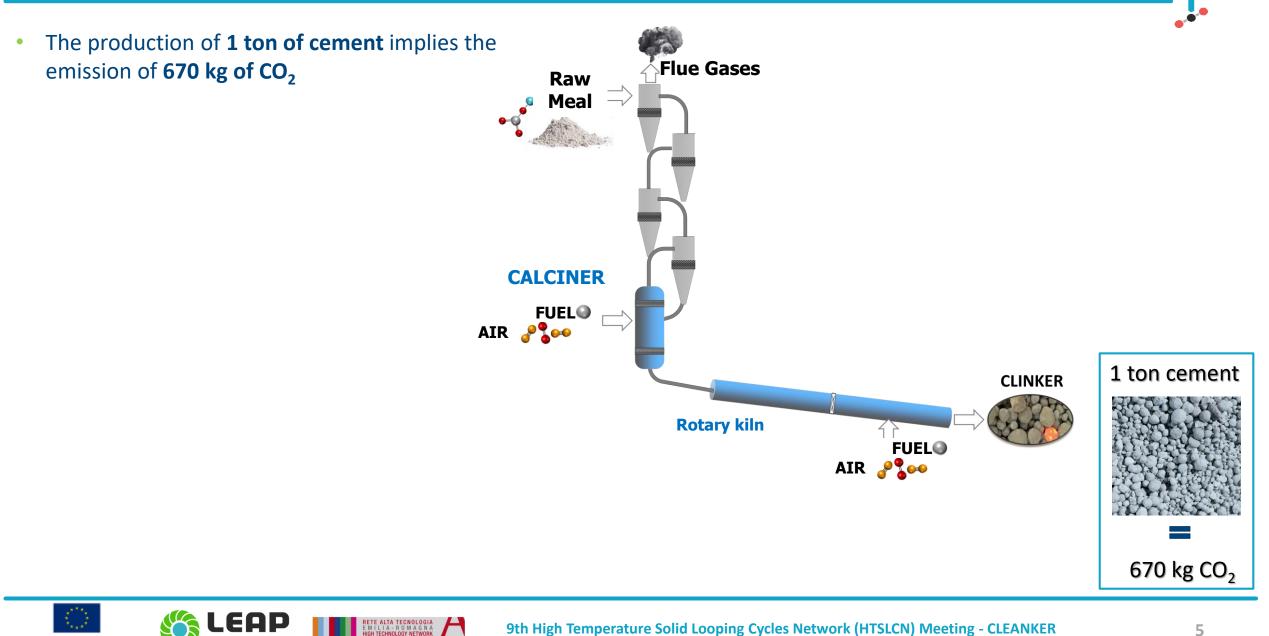
# CO<sub>2</sub> emissions in cement making

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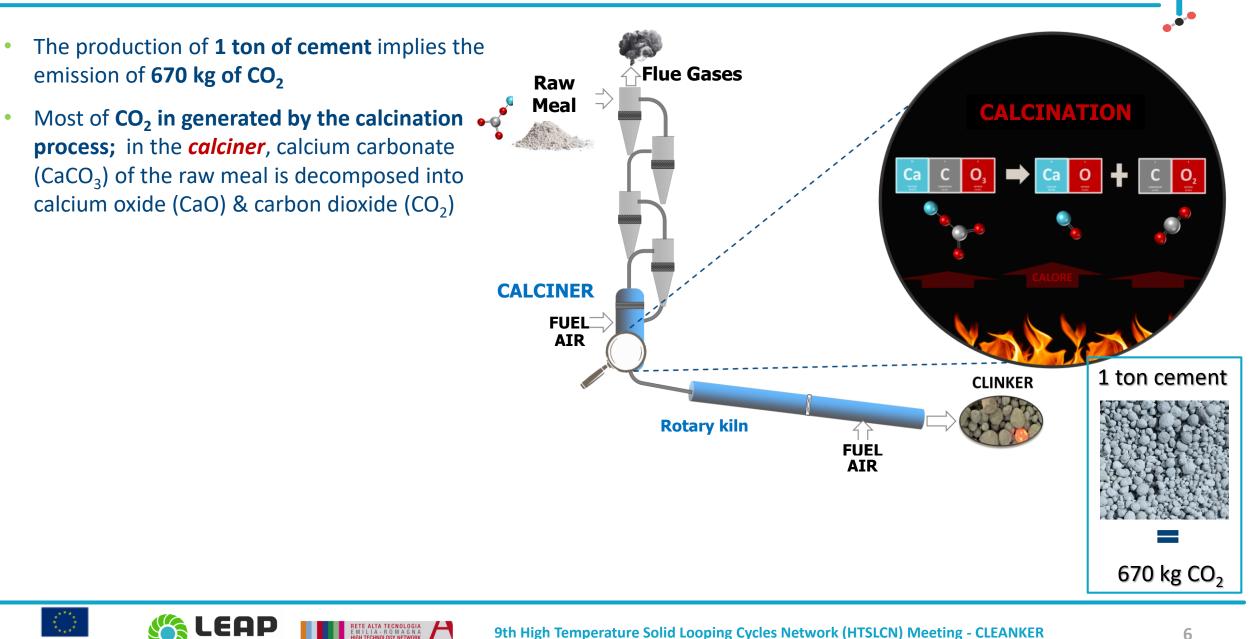
Framework Programme of the European Union



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# CO<sub>2</sub> emissions in cement making





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# CO<sub>2</sub> emissions in cement making

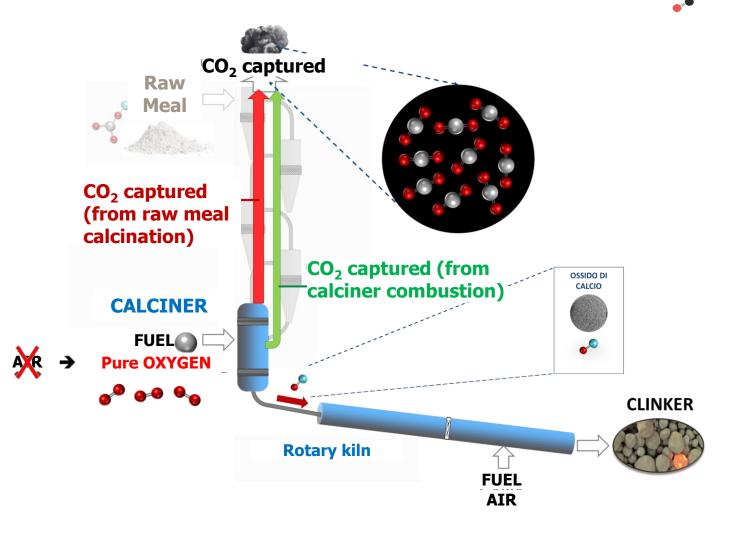
- Flue Gases Raw Meal COMBUSTION 0, CALCINER **FUEL** AIR **CLINKER** 1 ton cement **Rotary kiln FUEL** AIR 🦓 🎖 👀 670 kg CO<sub>2</sub>
- The production of **1 ton of cement** implies the emission of **670 kg of CO<sub>2</sub>**
- Most of CO<sub>2</sub> in generated by the calcination process; in the *calciner*, calcium carbonate (CaCO<sub>3</sub>) of the raw meal is decomposed into calcium oxide (CaO) & carbon dioxide (CO<sub>2</sub>)
- Calcination is an endothermic reaction, requiring heat → first combustion → additional CO<sub>2</sub> emissions
- The final product (CLINKER) is produced in the *rotary kiln* by heating the hot meal up to 1450°C → second combustion → additional CO<sub>2</sub> emissions
- Eliminating all the combustion steps (e.g. by exploiting renewable energy) would not be sufficient to completely decarbonize cement making process!



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#### **Integrated Calcium-looping process**

- The first step required for implementing the integrated CaL is to switch the <u>calciner</u> from air combustion to pure oxyfuel combustion
- $\rightarrow$  In this way,  $CO_2$  is produced at high concentrations and is ready for the following purification, transport and storage steps





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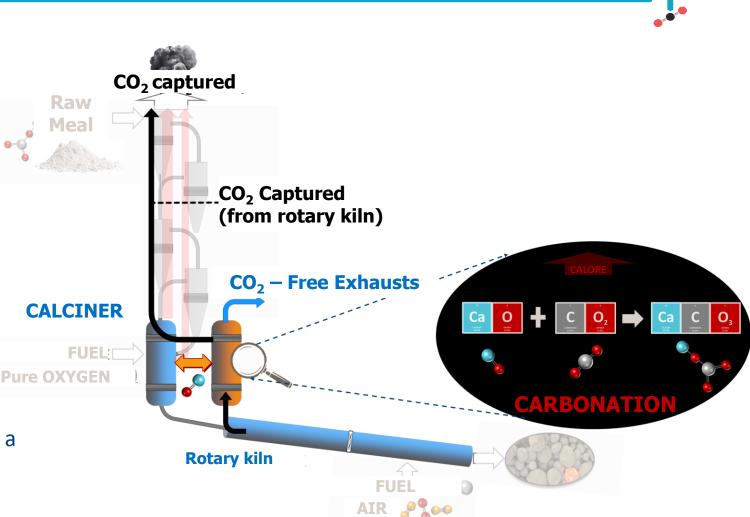
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### **Integrated Calcium-looping process**

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- $\rightarrow$  In this way,  $CO_2$  is produced at high concentrations and is ready for the following purification, transport and storage steps
- The second step requires to use a fraction of calcium oxide (CaO) as CO<sub>2</sub> sorbent:
- → In the **carbonator**, the CaO based material «captures»  $CO_2$  from the effluents produced in the rotary kiln, forming  $CaCO_3$
- CaCO<sub>3</sub> is then recycled back to the calciner, where a second calcination generates:
  - 1) a concentrated flow of CO<sub>2</sub> captured
  - 2) a flow of **regenerated sorbent** (CaO) ready for the next CO<sub>2</sub> capture cycle (Calcium Looping)



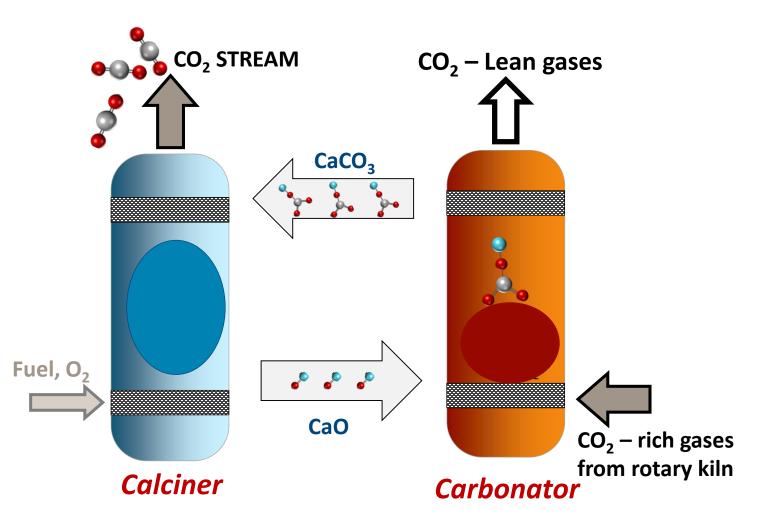
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Calcium operates as a  $CO_2$  carrier by concentrating  $CO_2$  from the rotary kiln effluents to a  $CO_2$ -rich gaseous strem released from the oxyfuel calciner.







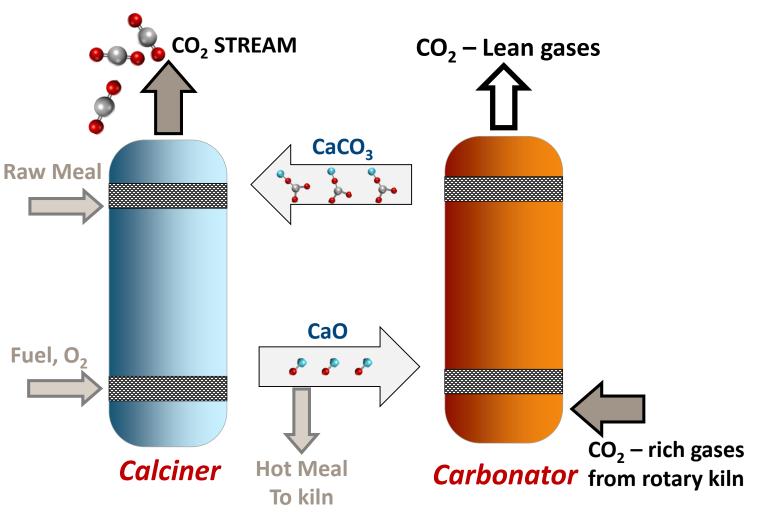
CLEAN clinkFF by calcium

Calcium operates as a  $CO_2$  carrier by concentrating  $CO_2$  from the rotary kiln effluents to a  $CO_2$ -rich gaseous strem released from the oxyfuel calciner.

Integrated CaL advantages:

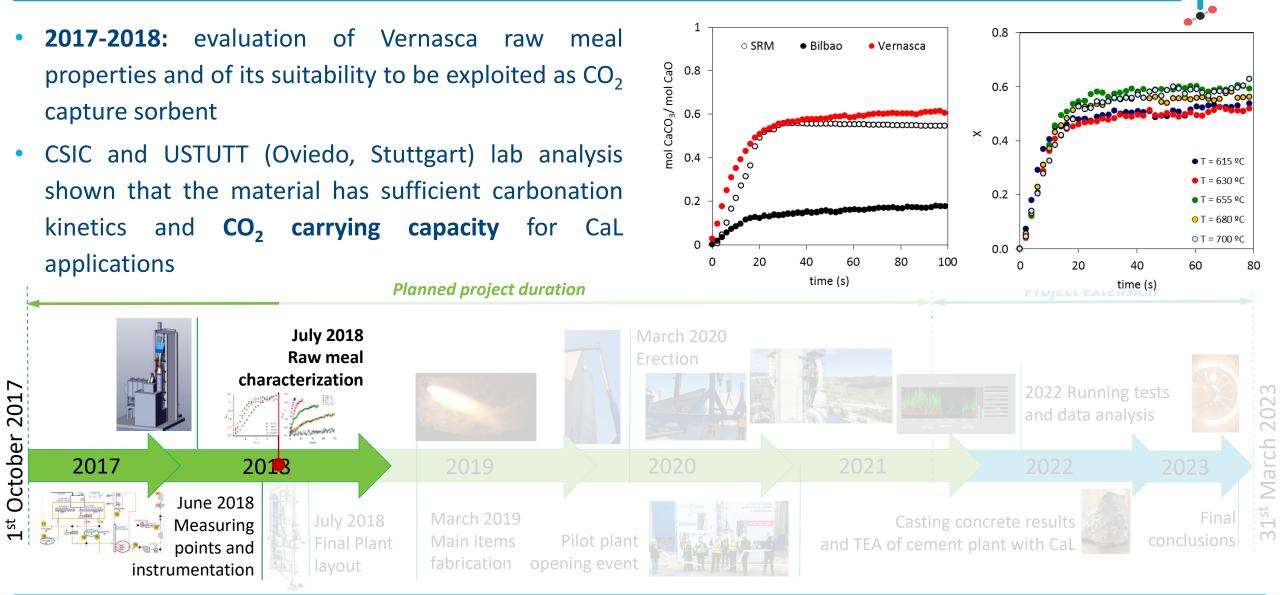
- No special equipment required
- Cement raw meal is the CO<sub>2</sub> sorbent
- No variation to rotary kiln and cooler

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# **CLEANKER – Timeline: sorbent characterization**







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#### **CLEANKER timeline: pilot construction**

- 2017-2018: pilot plant design
  - 693 technical sheets
  - 15 revisions to achieve an optimized process scheme

• 2019: construction of pilot plant components

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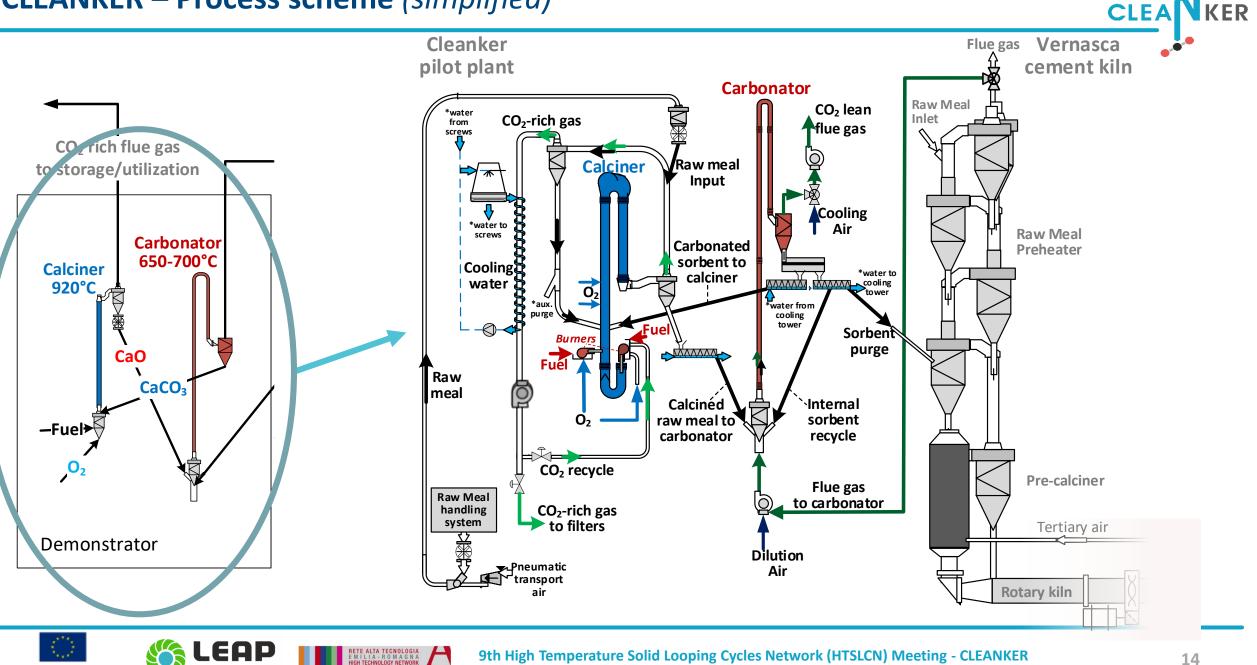
#### **CLEANKER – Process scheme** (simplified)

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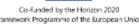
#### **CLEANKER timeline: pilot erection**

- 2020: pilot plant erection in the Vernasca hosting site, owned by Buzzi Unicem
- Installation of a total 110 tons of components and machineries (+ 40 ton of refractory material), 38 big-size ducts, 78 expansion joints and 189 strumental devices

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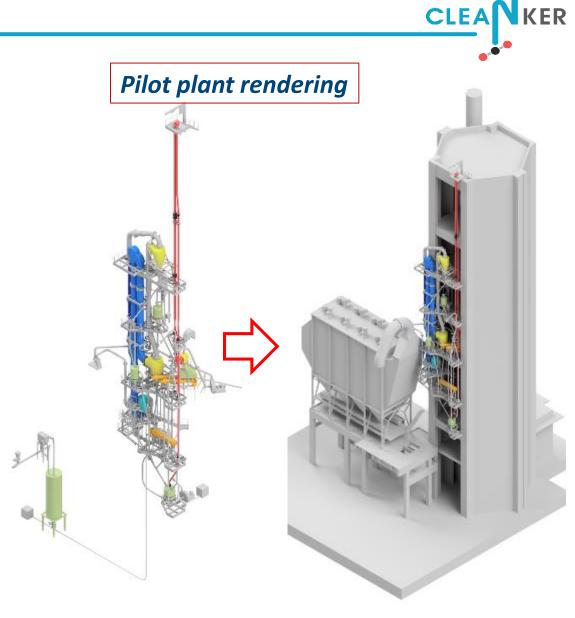
### **CLEANKER – Pilot plant**

# Vernasca cement plant Buzzi Unicem



Cement plant preheating tower











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#### **CLEANKER** calciner



- **Two burners** (Heavy-oil fuel, oxycombustion)
- Multiple Oxygen injection points
- **CO<sub>2</sub> recycle** duct (cooled)
- Rotary screw to control solid circulation
- Raw material preheating stage (riser-cyclone)
- Gas/solid cyclone separators









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#### **CLEANKER** carbonator



- Overall length 105m, variable diameter (250 mm upward-
- Stailness steel eintrained flow reactor (EFR), gooseneck shape;
- **Cyclone** to separate carbonated meal from CO<sub>2</sub>-free gases
- **Cooled screw** to sent the carbonated meal back to calciner







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## **CLEANKER timeline – Opening event**

- 9-10-2020 Opening event at Buzzi's premises in Vernasca: «La cattura della CO<sub>2</sub> nell' industria del cemento Il progetto CLEANKER»
- 8 oral presentations + pilot plant visit

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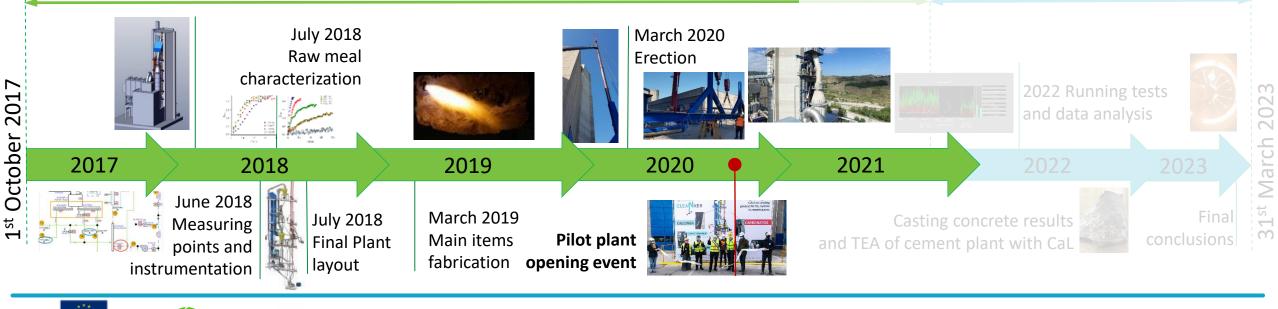
- CLEANKER stakeholders and policy makers have been involved
- Pilot plant commissioning was started right after the opening event



Project extension

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#### **CLEANKER Opening Event**







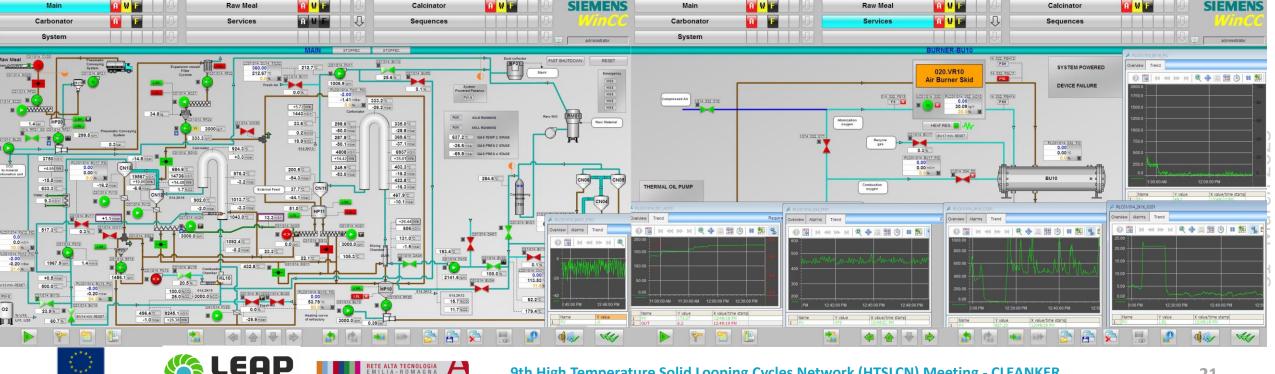


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# **CLEANKER timeline – experimental campaigns**

- Experimental campaigns have been managed and executed by BUZZI operators, with the support of LEAP, PoliMI, VdZ and Stuttgart
- 9 experimental campaigns: 5 short tests of 3 days each and 4 long tests of 1 week each) to evaluate the performances of the system as a function of main CaL parameters (e.g. solid/gas ratio, EFR reactors operating conditions)
- The pilot plant was operated for more than 100 hours in representative integrated Cal operating condition





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# **CLEANKER timeline – exploitation activities**

- CLEANKER consortium is evaluating all the technical aspects for the potential integration of CaL concept within different kind of cement plants
- **scale-up** studies for both retrofit & greenfield applications
- **business plan and TEAs** have been produced for the commercial exploitation of CLEANKER technology as a retrofit option for BUZZI and ITC (Heidelberg) cement plants Planned project duration

July 2018

Raw meal

July 2018

layout

**Final Plant** 

2019

March 2019

Main items

fabrication

Pilot plant

opening event

characterization

2018

June 2018

Measuring

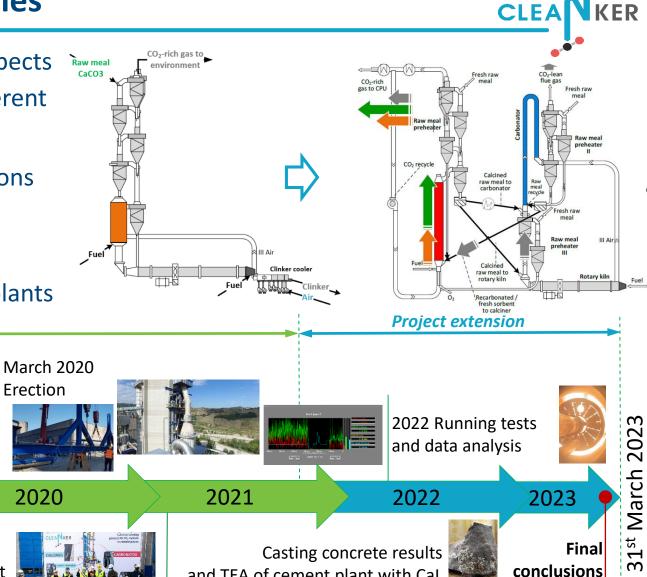
points and

instrumentation

October 2017

2017

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and TEA of cement plant with CaL

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#### **CLEANKER in SUPERQUARK**



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26 Agosto 2020, RAI1, SUperQuark, Piero Angela https://www.youtube.com/watch?v=oQcrWfRbFJg







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The raw meal used for making cement can be efficiently exploited as CO<sub>2</sub> sorbent, not only in controlled lab tests but also in operational environment

→ All the uncertainties related to sorbent properties and to the formation of side species have been overcome

#### **Results**

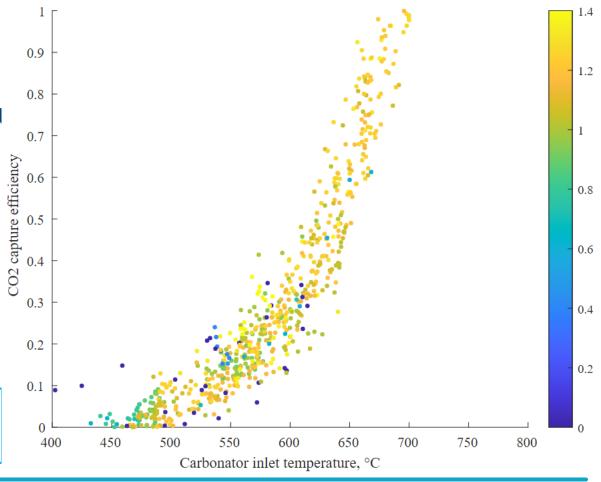
#### **Carbonator:**

- Good CO<sub>2</sub> capture performances in a wide range of inlet T (550-700°C), confirmed by gas and solid analyses
- Linear trend between the increase in the Ca to CO<sub>2</sub> ratio and the CO<sub>2</sub> capture rate

#### Calciner:

- Pilot operation continuously improved during tests
  - $\rightarrow$  stable operation of oxyfuel calcination achieved
- Promising CO<sub>2</sub> concentrations at calciner outlet (>70%);

Residual difficulties in keeping **high sorbent circulation rates** for significant periods, due to small pilot ducts



# Thanks for your attention!

For any question:



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