

Improving the prediction of fertilizer phosphorus availability to plants with simple, but non-standardized extraction techniques

(Supplementary Material)

Olivier Duboc^{1,2*}, Alicia Hernandez-Mora^{2,3}, Walter W. Wenzel¹, Jakob Santner^{2*}

¹ University of Natural Resources and Life Sciences, Institute of Soil Research, Konrad-Lorenz-Strasse 24, 3430 Tulln, Austria.

² University of Natural Resources and Life Sciences, Institute of Agronomy, Konrad-Lorenz-Strasse 24, 3430 Tulln, Austria.

³ Agrana Research & Innovation Center GmbH (ARIC), Josef-Reither-Strasse 21-23, 3430 Tulln, Austria

* Corresponding authors: olivier.duboc@boku.ac.at, jakob.santner@boku.ac.at

Number of Tables: 5

Number of Figures: 5

MATERIALS AND METHODS

List of the fertilizers

Table S1: Description of the fertilizers used in this study (n=79). HTC= Hydrothermal Carbonization

Sample ID	Description	Sourced from / Processed by	P total (<i>aqua regia</i> ; g P 100g dry matter ⁻¹)*	Used in pot experiment	Used in Duboc et al. (2017) (ID given if applicable)
BGSL-1	Biogas slurry from food and agricultural wastes. The slurry was freeze-dried before use.	Biogas Bruck/Leitha GmbH & Co KG (Bruck /Leitha, Austria)	1.73	X	BGSL
BGSL-1-BC 400-1	BGSL-1 pyrolyzed at 400 °C in an experimental lab reactor with nitrogen as flush gas	Austrian Institute of Technology (AIT) (Tulln, Austria)	3.37		BGSL-BC
BGSL-1-BC 400-2	Same as above	AIT (Tulln, Austria)	2.79	X	
BGSL-1-BC 500	Same as above, T = 500°C	AIT (Tulln, Austria)	2.85		
BGSL-2	Biogas slurry, same origin as BGSL-1, but material was not freeze-dried before treatment	Biogas Bruck/Leitha GmbH & Co KG (Bruck /Leitha, Austria)	1.37		
BGSL-2-HC	BGSL-2 treated by HTC, 225 min at 200°C	Institute for Chemical and Energy Engineering (IVET), BOKU, Vienna	1.89		
BGSL-3	Same as BGSL-2 (subsample of the same sampling date)	See BGSL-2	2.10		
BGSL-3-HC	BGSL-3 treated by HTC, 225 min at 200°C	See BGSL-2-HC1	2.16		
BGSL-4	Same as BGSL-2 and -3 (subsample of the same sampling date)	See BGSL-2	1.82		
BGSL-4-HC	BGSL-4 treated by HTC, t = 390 min; T = 175°C	See BGSL-2-HC1	1.77		
CatM-1	Cattle Manure	Beckmann & Brehm	0.82		

		GmbH (Beckeln, Germany)			
CatM-1-BC 500	CatM-1 pyrolyzed at 500°C for 20 min in a PYREKA (Pyreg GmbH, Dörth/Germany)	AIT (Tulln, Austria)	2.91	X	
CatM-1-BC 700	CatM-1 pyrolyzed at 700°C as above	AIT (Tulln, Austria)	1.86		
CatM-1-HC	CatM-1 treated by HTC: 60 min ramp + 60 min at 200°C + cooling. Lab reactor model 4740, Parr Instrument GmbH (Frankfurt/Main, Germany). 24 g+ 24mL H ₂ O	IVET, BOKU, Vienna	0.95		
ChM-1	Chicken manure (ChM)	Egg producing farm	1.97	X	CM
ChM-1-BC 400-1	ChM-1 pyrolyzed at 400 °C (see BGSL-1)	AIT (Tulln, Austria)	4.14		CM-BC
ChM-1-BC 400-2	Same as above	AIT (Tulln, Austria)	3.30		
ChM-1-BC 400-So	Same as above but with addition of Na ₂ CO ₃ .	AIT (Tulln, Austria)	4.02		
ChM-1-BC 500	ChM-1 pyrolyzed at 500 °C (see BGSL-1)	AIT (Tulln, Austria)	3.62	X	
ChM-1-BC 500-So	Same as above but with addition of Na ₂ CO ₃ .	AIT (Tulln, Austria)	3.62		
ChM-1-HC	ChM-1 treated by HTC, 225 min at 180°C	IVET, BOKU, Vienna	2.52	X	
ChM-2	Chicken manure	Egg producing farm	1.53		
ChM-2-HC-1	ChM-2 treated by HTC, 120 min at 180°C	IVET, BOKU, Vienna	2.03		
ChM-2-HC-2	ChM-2 treated in 2 steps by HTC. <u>Step 1</u> : 120 min at 220°C; <u>Step 2</u> : 120 min at 220°C	IVET, BOKU, Vienna	3.05		
ChM-3	Chicken manure	Egg producing farm	1.25		
ChM-4	Chicken manure	Egg producing farm	1.19		
ChM-5	Chicken manure	Italpollina Deutschland (Aschau im Chiemgau, Germany).	1.41	X	
ChM-5-BC 500	ChM-5 pyrolyzed at 500°C (see CatM-1-BC 500)	AIT (Tulln, Austria)	4.02	X	

ChM-5-BC 700	ChM-5 pyrolyzed at 700°C as above	AIT (Tulln, Austria)	4.29		
ChM-5-HC	ChM-5 treated by HTC (see CatM-1-HC-1)	IVET, BOKU, Vienna	1.72		
MBM-1	Meat and bone meal (MBM)	Steirische Tierkörperverwertungs GmbH & Co KG (Gabersdorf, Austria)	4.72	X	MBM
MBM-1-BC 400-1	MBM-1 pyrolyzed at 400°C (see BGSL-1)	AIT (Tulln, Austria)	10.69		MBM-BC
MBM-1-BC 400-2	Same as above	AIT (Tulln, Austria)	10.24		
MBM-1-BC 500	Same as above but at 500°C	AIT (Tulln, Austria)	10.85	X	
MBM-1-HC	MBM-1 treated by HTC, 225 min at 180°C	IVET, BOKU, Vienna	8.84		
MBM-2	Meat and bone meal	Steirische Tierkörperverwertungs GmbH & Co KG (Gabersdorf, Austria)	4.84	X	
MBM-2-BC 500	MBM-2 pyrolyzed at 500°C (see CatM-1-BC 500)	AIT (Tulln, Austria)	10.76	X	
MBM-2-BC 700	MBM-2 pyrolyzed at 700°C (see above)	AIT (Tulln, Austria)	12.52		
MSS-1-BC	MSS pyrolyzed at 400°C (see BGSL-1)	AIT (Tulln, Austria)	9.26		MSS-BC-1
MSS-2-BC	Pyrolyzed MSS	WPA beratende Ingenieure (Vienna, Austria)	6.85	X	MSS-BC-2
MSS-3-BC	Pyrolyzed MSS	AIT (Tulln, Austria)	9.14		MSS-BC-3
MSS-4	Municipal sewage sludge	Municipal wastewater treatment plant (Tulln, Austria)	2.13	X	
MSS-4-BC 500	MSS-4 pyrolyzed at 500°C (see CatM-1-BC 500)	AIT (Tulln, Austria)	6.59	X	
MSS-4-BC 700	MSS-4 pyrolyzed at 700°C (see above)	AIT (Tulln, Austria)	5.50	X	
MSS-4-HC	MSS-4 treated by HTC (see CatM-1-HC-1)	IVET, BOKU, Vienna	2.31		
MSS-5	Municipal sewage sludge	Municipal wastewater treatment plant (Traismauer, Austria)	4.01	X	
MSS-5-HC-1	MSS-5 treated by HTC with addition of MgCl ₂ and adjusted at pH 10.5, T = 240°C	IVET, BOKU, Vienna	4.45	X	

MSS-5- HC-2	MSS-5 treated by HTC with addition of K-citrate and adjusted at pH 3.5, T = 240°C	IVET, BOKU, Vienna	4.83	X	
MSS-6- AshDec- Mg	MSS treated by pyrolysis and gasification with addition of MgCl ₂	Activil corp. (Moscow, Russia) ^a	7.30		MSS-G-1
MSS-7- AshDec- Mg	MSS treated by pyrolysis and gasification with addition of MgCl ₂	Activil corp. (Moscow, Russia) ^a	9.77	X	MSS-G-2
MSS-8- AshDec- Mg	MSS treated by AshDec process with addition of MgCl ₂	Bundesanstalt für Materialforschung (BAM) (Berlin, Germany) ^a	10.18	X	
MSS- AshDec- K/Na-1	MSS treated by AshDec process with addition of K ₂ SO ₄ and Na ₂ SO ₄	BAM (Berlin, Germany) ^b	7.57		
MSS- AshDec- K/Na-2	MSS treated by AshDec process with addition of K ₂ SO ₄ and Na ₂ SO ₄	BAM (Berlin, Germany) ^b	7.65	X	
MSS- AshDec- Na-1	MSS treated by AshDec process with addition of Na ₂ SO ₄	BAM (Berlin, Germany) ^b	7.65		
MSS- AshDec- Na-2	MSS treated by AshDec process with addition of Na ₂ SO ₄	BAM (Berlin, Germany) ^b	7.95	X	
MSS- AshDec- Na Low	MSS treated by AshDec process with addition of Na ₂ SO ₄ at suboptimal Na/P molar ratio	BAM (Berlin, Germany) ^b	7.44	X	
MSSA-1	Municipal sewage sludge ash	Undisclosed origin ^c	7.55	X	
MSSA-1- Slag-1a	MSSA-1 (25 %) fused with Linz- Donawitz steel slag (75 %) for 30 min, quenched.	Undisclosed origin ^c	2.29		
MSSA-1- Slag-1b	As above, but not quenched	Undisclosed origin ^c	2.37	X	
MSSA-1- Slag-2a	MSSA-1 (26 %) fused with Linz- Donawitz steel slag (67 %) and CaO (7 %) for 30 min, quenched.	Undisclosed origin ^c	2.31		
MSSA-1- Slag-2b	As above, but not quenched	Undisclosed origin ^c	2.39	X	

MSSA-1-Slag-3a	MSSA-1 (12.5 %) fused with Linz-Donawitz steel slag (72 %) and CaO (15.5 %) for 30 min, quenched.	Undisclosed origin ^c	1.83		
MSSA-1-Slag-3b	As above, but not quenched	Undisclosed origin ^c	1.87	X	
MSSA-2-Slag	Fused municipal sewage sludge ash with Linz-Donawitz steel slag	FEhS - Building Materials Institute (Duisburg, Germany) ^c	2.38	X	
Prec-P-RoC-1	P-RoC process: Precipitated Ca-phosphate from liquid fraction of centrifuged MSS	Karlsruhe Institute of Technology (KIT) (Karlsruhe, Germany)	3.72	X	
Prec-P-RoC-2	P-RoC process: Precipitated Ca-phosphate from percolation water of a dry fermentation plant	KIT (Karlsruhe, Germany)	1.59	X	
Prec-Struvite-1	“Berliner Pflanze”: Struvite from municipal WWTP	Berliner Wasserbetriebe (Berlin, Germany)	12.18	X	Struvite
Prec-Struvite-2	“CrystalGreen” Struvite	Ostara Nutrient Recovery Technologies Inc. (Vancouver, Canada)	12.72	X	
Ref-Di Calcium P	CaHPO ₄	Sigma Aldrich; CAS: 7757-93-9	22.16	X	
Ref-Mono Calcium P	Ca(H ₂ PO ₄) ₂	Alfa Aesar; CAS: 301524-28-7	24.37	X	
Ref-Rock P-1	Rock phosphate	Undisclosed origin	13.57	X	RP
Ref-Rock P-2	Rock phosphate	Eppawala, Sri Lanka	14.86	X	
Ref-SSP	Commercial Single Superphosphate (“DC Superphosphate”)	Timac Agro Düngemittelproduktions- und HandelsgmbH, (Zwentendorf, Austria)	8.98	X	SSP
Ref-ThermoP	Thermophos: Fused Ca-Mg-Phosphate, by melting phosphate rock and serpentine rock	Nelisfert (New Zealand)	7.96	X	
Ref-ThomasP	Thomas slag	FEhS - Building Materials Institute (Duisburg, Germany)	3.98	X	

Ref-TSP	Commercial Triple Superphosphate	Raiffeisen-Lagerhaus (Austria)	21.57	X	
---------	----------------------------------	--------------------------------	-------	---	--

* Dry matter basis after drying at 50°C for 24 h, except the Ref- and Prec- products which were analyzed and used without additional drying.

^a Thermo-chemical treatment described in Adam et al.(2009)

^b Process described in Herzel et al. (2021)

^c process as in Bartsch et al. (2013) and Rex et al. (2014)

RESULTS AND DISCUSSION

Solubility of struvite in 0.5 mol L⁻¹ NaHCO₃ solution. Comparison of experimental data with calculations from Visual MINTEQ 3.1

Table S2: Input concentrations for calculation of struvite dissolution equilibrium in 0.5 mol L⁻¹ NaHCO₃ with Visual MINTEQ 3.1 (<https://vminteq.lwr.kth.se>). Comparison of 1 : 200 and 1 : 1000 fertilizer : solution ratio (*w* : *v*).

	Ion	Concentration (mg L ⁻¹)	
		1 : 200	1 : 1000
Input	Mg ²⁺	495	99.1
	NH ₄ ⁺	367	73.4
	PO ₄ ³⁻	1936	387.3
	Na ⁺	11500	11500
	CO ₃ ²⁻	30000	30000

Table S3: Output of calculation of struvite dissolution equilibrium in 0.5 mol L⁻¹ NaHCO₃ with Visual MINTEQ 3.1 (<https://vminteq.lwr.kth.se>). Comparison of 1 : 200 and 1 : 1000 fertilizer : solution ratio (*w* : *v*) with MgCO₃ allowed to precipitate (X) or not (-). By default, struvite was allowed to precipitate in both scenarios. Starting concentrations as in Table S2. pH was set to 8.3 since it is buffered by the HCO₃⁻ ions of the extraction solution.

MgCO ₃	% of total P dissolved	
	1 : 200	1 : 1000
-	16.4	100
X	100	100

Table S4 Results of an extraction experiment using 1 : 200 and 1 : 1000 fertilizer : solution ratio (*w* : *v*; 150 and 30 mg struvite in 30 mL extraction solution respectively) at 0.5, 4 and 21 h. Results expressed as mean ± *u* where *u* (coverage factor = 1) encompasses the respective uncertainties of total P and extracted P. pH remained between 8.25 and 8.35 during the extraction.

Time (h)	% of total P dissolved	
	1 : 200	1 : 1000
0.5	26.6±2.3	93.8±6.4
4	24.6±1.8	98.9±6.5
21	26.0±2.4	101.4±7.6

Plant biomass and P content

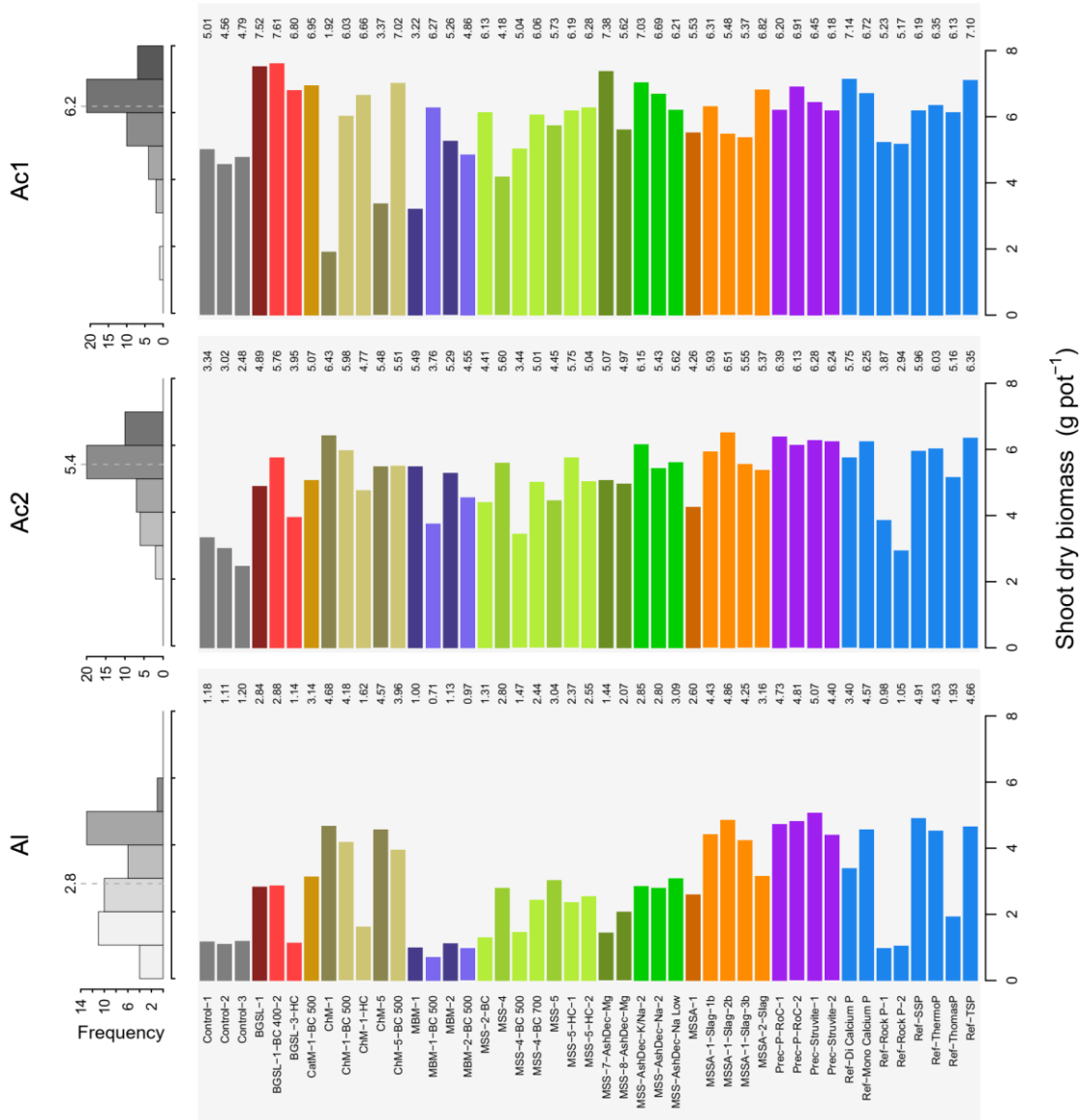


Figure S1: Shoot dry biomass harvested from each pot. In the histograms, the dotted line and the value above it is the median.

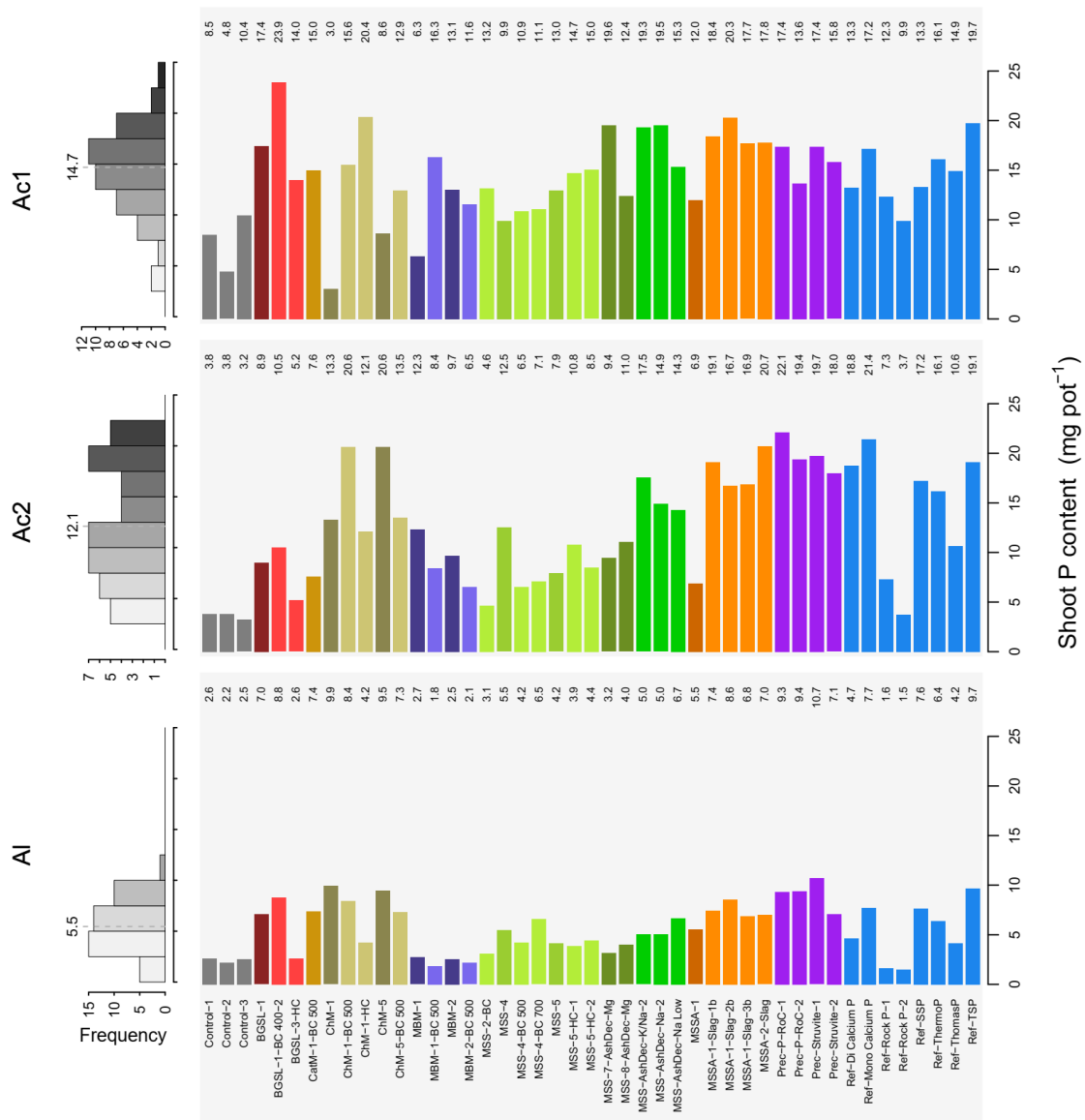


Figure S2: Shoot P content in each pot. In the histograms, the dotted line and the value above it is the median.

Shoot N/P ratio

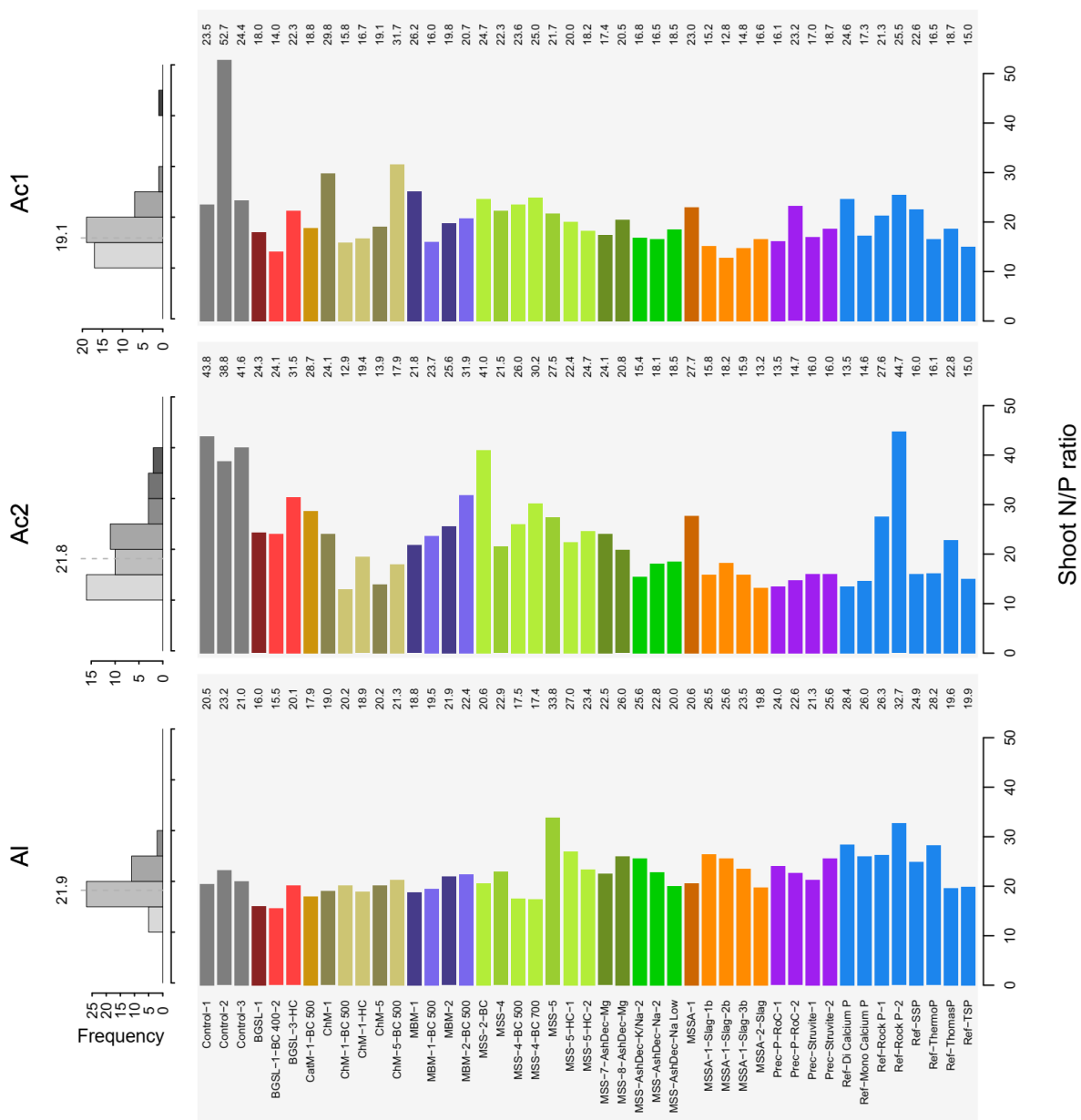


Figure S3: Shoot N/P mass ratio. In the histograms, the dotted line and the value above it is the median.

Responsiveness of the Ac1 soil to P fertilizer

Among the three soils used in this study, the Ac1 soil showed the weakest regressions between fertilizer extraction methods and plant growth or P uptake. To some extent, it appears that the soil was not responsive to P addition. Here we show that despite this appearance, there was in fact a response to P addition.

Although we cannot directly compare fertilizers against each other ($n = 1$), it is possible to compare different fertilizer groups. In Table S5 we show the difference of shoot biomass between (1) the three unfertilized controls and the three water-soluble references (“Ref-SSP”, “Ref-TSP” and “Ref-Mono Calcium P”) and (2) the three unfertilized controls and the three pots with the largest biomass. The results confirm that there was a response to P addition in that soil.

Table S5: Difference of shoot biomass (g pot^{-1}) in the Ac1 soil between the three unfertilized controls and selected groups of fertilized treatments: either (1) the three soluble references or (2) the three pots with the largest biomass.

		Mean of the controls	Mean of the alternative	<i>p</i> -value (Welch's t-test)
		g pot^{-1}		
		\pm standard deviation of means		
(1)	Unfertilized controls vs H ₂ O-soluble fertilizers “Ref-TSP”, “Ref-SSP”, “Ref-Mono Calcium P”)	4.79 \pm 0.13	6.67 \pm 0.26	0.00841
(2)	Unfertilized controls vs pots with the largest biomass	4.79 \pm 0.13	7.50 \pm 0.07	0.00035

Comparison of regressions on the neutral soil between this study and our previous study

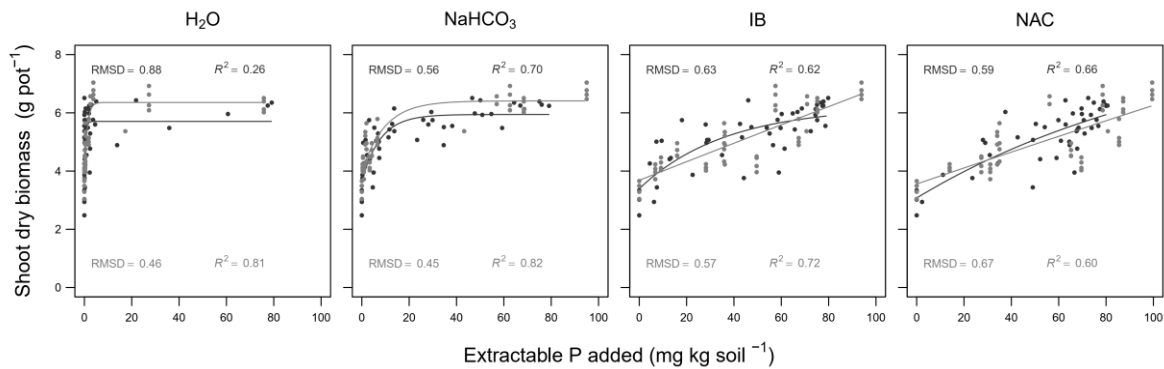


Figure S4: Comparison of the regressions of shoot biomass vs. extractable P in this study (dark color) and our previous study (Duboc et al., 2017) (light color) for the slightly acidic (Ac2) soil. In the previous study, soil was fertilized with 100 mg P kg⁻¹ while in this study we used 80 mg P kg⁻¹. To make the results comparable, the independent variable is the amount of extractable P added to the soil (mg P kg⁻¹), and not the amount of extractable P in % of total P as in the main part of the publication.

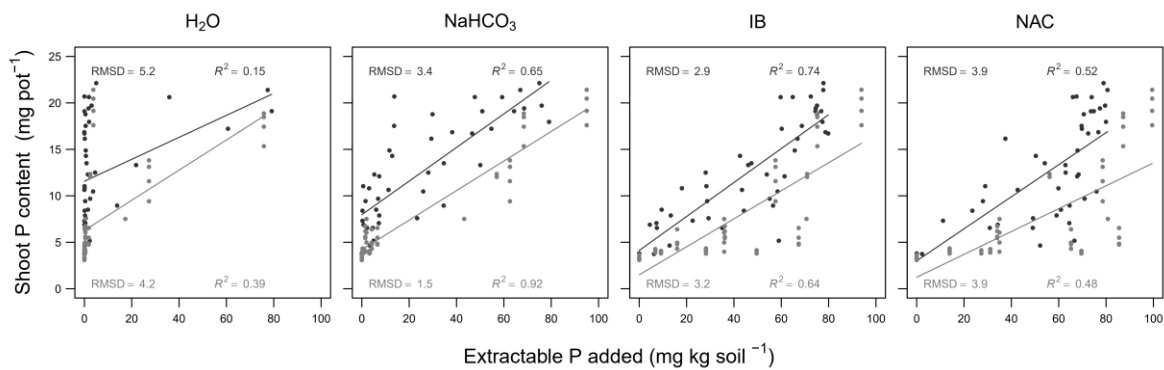


Figure S5: Comparison of the regressions of shoot P content vs. extractable P in this study (dark color) and our previous study (Duboc et al., 2017) (light color) for the slightly acidic (Ac2) soil. In the previous study, soil was fertilized with 100 mg P kg⁻¹ while in this study 80 mg P kg⁻¹ was used. To make the results comparable, the independent variable is the amount of extractable P added to the soil (mg P kg⁻¹), and not the amount of extractable P in % of total P as in the main part of the publication.

References

- Adam, C., Peplinski, B., Michaelis, M., Kley, G., Simon, F.-G., 2009. Thermochemical treatment of sewage sludge ashes for phosphorus recovery. *Waste Management* 29, 1122–1128. <https://doi.org/10.1016/j.wasman.2008.09.011>
- Bartsch, S., Breuer, J., Drissen, P., Pischke, J., Rex, M., 2013. Optimierte Ressourceneffizienz in der Konverterstahlerzeugung; Phosphoranreicherung und Aufschluss phosphorhaltiger mineralischer Reststoffe in flüssigen LD-Schlacken. Schlussbericht FKZ 033R004A-E.
- Duboc, O., Santner, J., Golestani Fard, A., Tacconi, J., Zehetner, F., Wenzel, W.W., 2017. Predicting phosphorus availability from chemically diverse conventional and recycling fertilizers. *Sci. Total Environ.* 599–600, 1160–1170. <https://doi.org/10.1016/j.scitotenv.2017.05.054>
- Herzel, H., Aydin, Z., Adam, C., 2021. Crystalline phase analysis and phosphorus availability after thermochemical treatment of sewage sludge ash with sodium and potassium sulfates for fertilizer production. *J. Mater. Cycles Waste Manag.* <https://doi.org/10.1007/s10163-021-01288-3>
- Rex, M., Drissen, P., Bartsch, S., Breuer, J., Pischke, J., 2014. Aufschluss von Phosphor aus Klärschlamm- und Tiermehlaschen in flüssiger Konverterschlacke. Presentation at the workhop Abwasser-Phosphor-Dünger, 29 Jan 2014, Berlin, Germany.