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CO₂ GAS FERMENTATION OPPORTUNITIES AND TECHNICAL CHALLENGES

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CO₂ GAS FERMENTATION

OPPORTUNITIES AND TECHNICAL CHALLENGES

JEAN-LUC DUBOIS
SCIENTIFIC DIRECTOR
ARKEMA

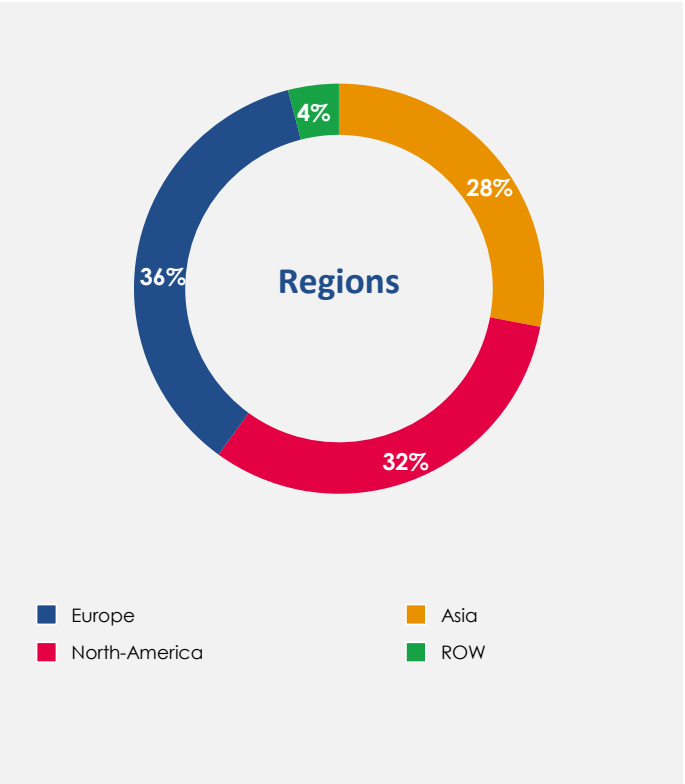
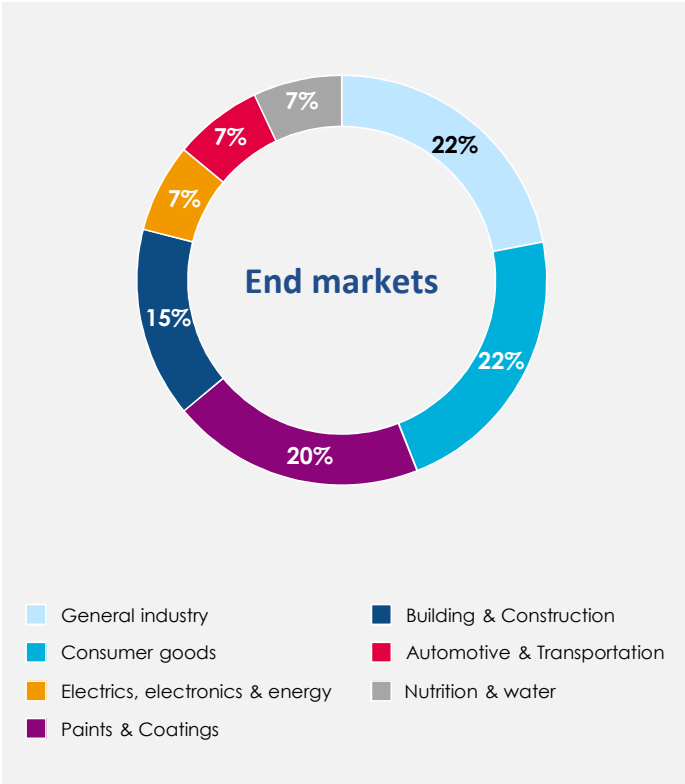
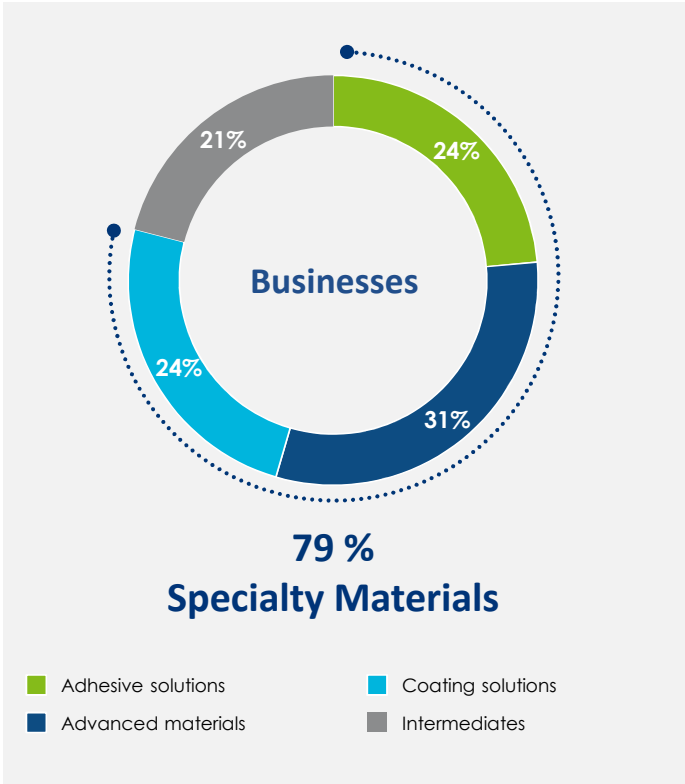


9th Conference on CO₂-based Fuels and Chemicals
Online Event



ARKEMA TODAY

2019 SALES SPLIT: €8.7bn



20,500
talents

11,200
in Europe

4,075
in North America

4,320 in Asia

905 in the rest of
the world



Over
10,000
customers

Collaborations
with the leading
global brands

WOMEN AND MEN AT THE HEART OF OUR DEVELOPMENT

~2,000
new hires
every year



Presence in
55 countries

144 plants
15 R&D
centers

INNOVATIVE SOLUTIONS WITH A SIGNIFICANT CONTRIBUTION TO THE UNITED NATIONS'S SUSTAINABLE DEVELOPMENT GOALS (SDG)



6 RESEARCH INNOVATIVE PLATFORMS



New energies

Materials to develop solar power, wind power, and electric batteries



Biosourced materials

Solutions to replace fossil resources as raw materials



Water treatment

Materials for water filtration applications



Home efficiency and insulation

Solutions to reduce energy consumption of buildings



Lightweight materials

Materials for composites and 3D Printing



Consumer electronics

Solutions to bring electronics within everyone's reach

46*% PRODUCTS PORTFOLIO CONTRIBUTING TO UN SDG

*44% products portfolio assessed

SUSTAINABLE DEVELOPMENT GOALS



MANAGE OUR ACTIVITIES AS A RESPONSIBLE MANUFACTURER



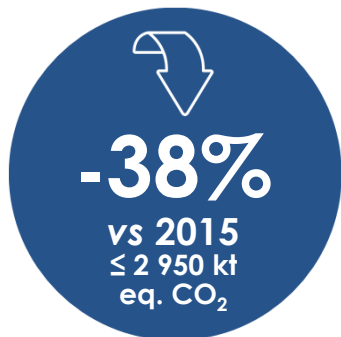
CLIMATE



Climate plan : Commitment to Paris agreement and Science-based target trajectory **well below 2°C**

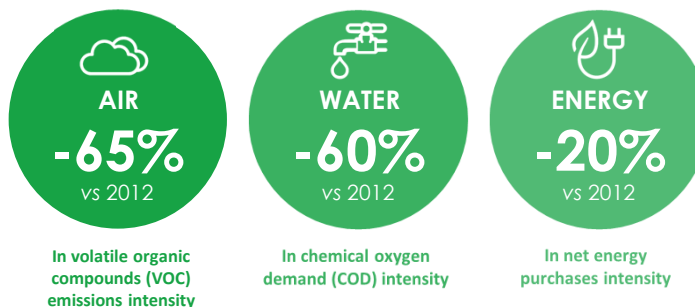


Greenhouse gas emissions (GHG) new target for 2030



ENVIRONMENT

New targets for 2030



Performance 2019 (vs 2012)



SECURITY

To be among the best in the industry

SAFETY AT WORK⁽¹⁾
Reduce injury frequency rate



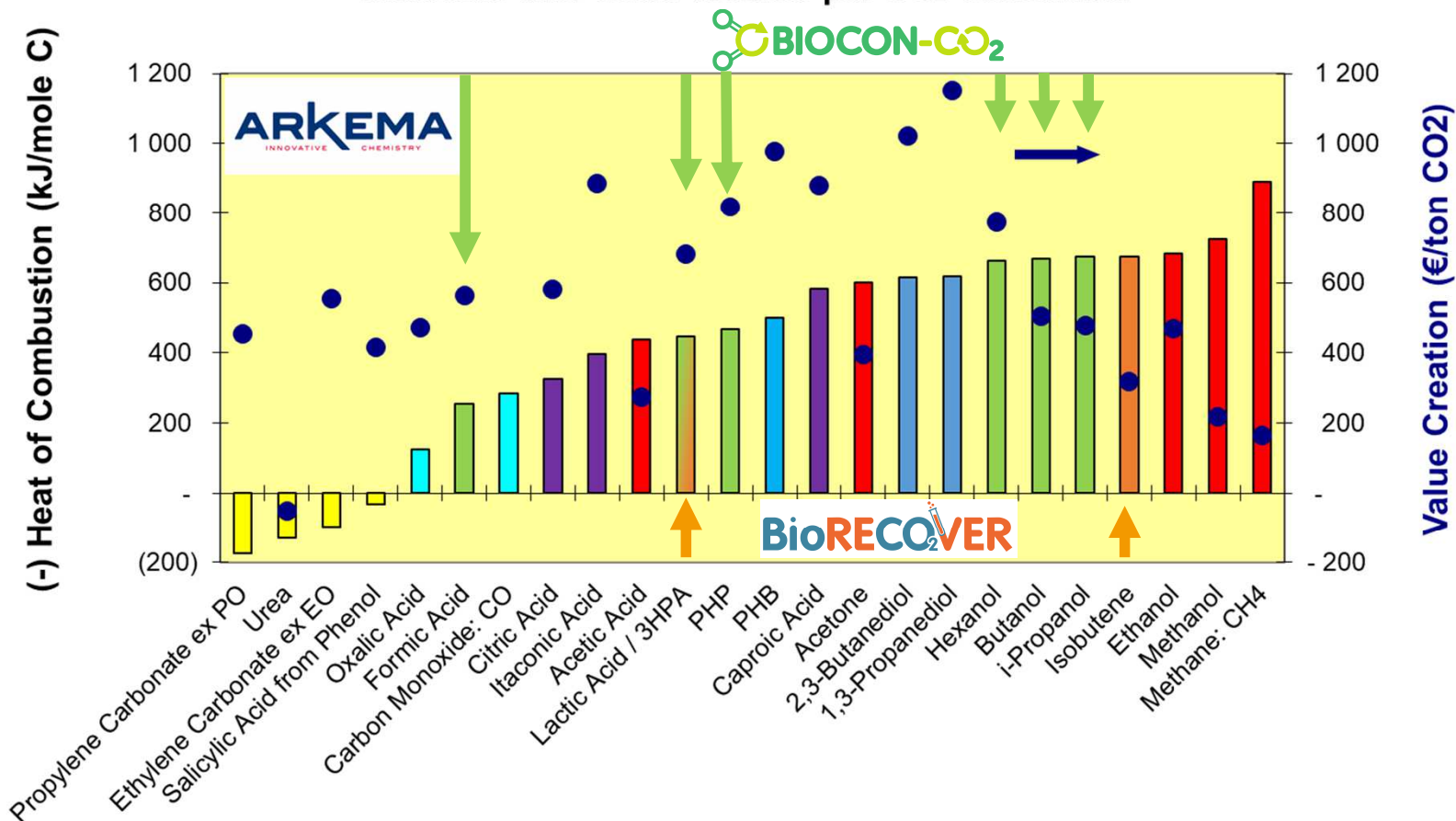
SAFETY EVENTS⁽¹⁾
Reduce safety events frequency rate



⁽¹⁾ Number of accident or event per million worked hour

TARGET PRODUCT SELECTION: VALUE CREATION AND ENERGY CONSUMPTION

Heat of Combustion as image of energy consumed to produce the molecule and Value created per CO₂ consumed



HEAT MANAGEMENT

❖ Determination of the adiabatic temperature rise

$$\text{❖ } \Delta_r H^\circ \left[\frac{\text{kJ}}{\text{mol}} \right] = \sum \Delta_f H^\circ_{\text{products}} - \sum \Delta_f H^\circ_{\text{reagents}}$$

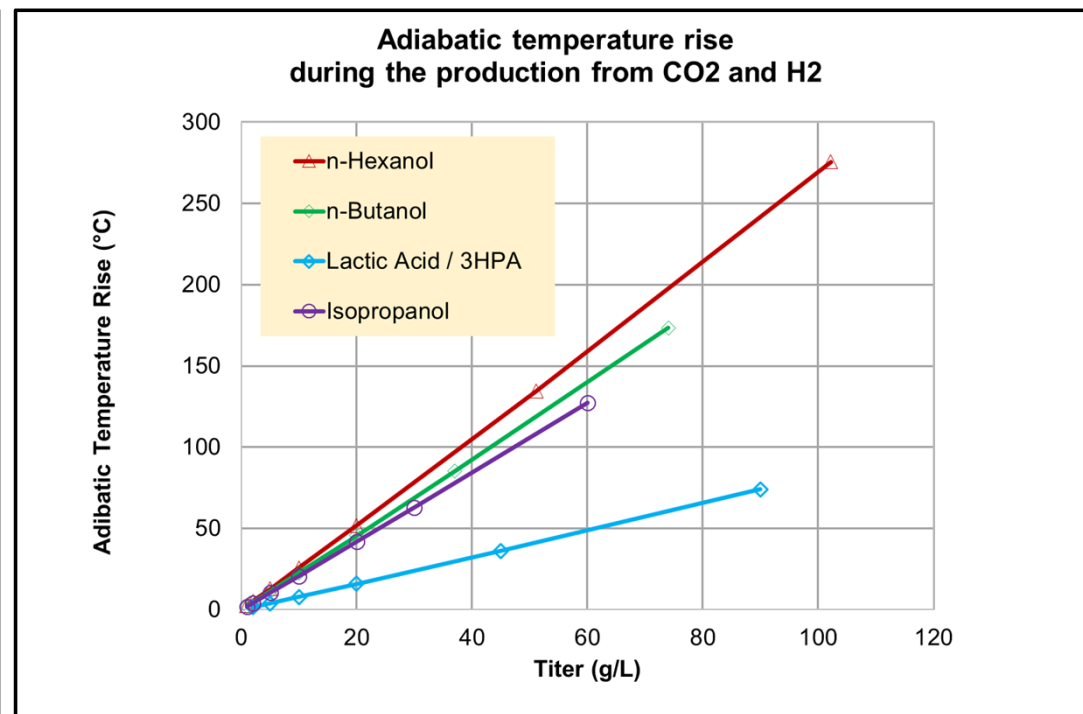
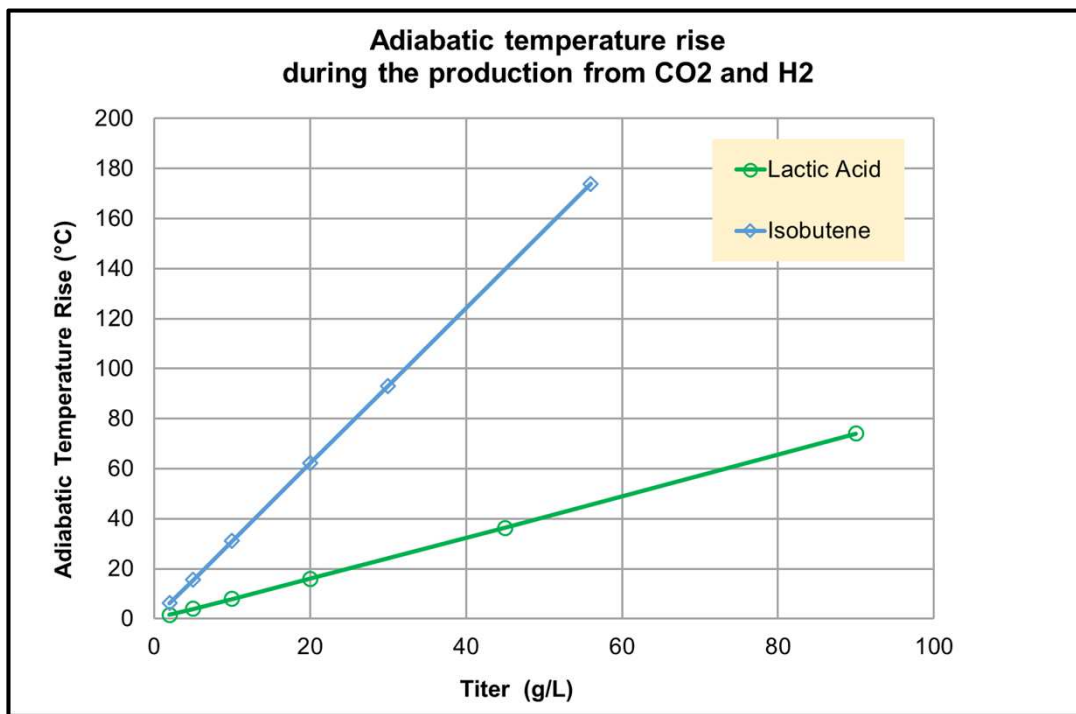
$$\text{❖ } \Delta T_{\text{liquid product}} = \frac{-\Delta_r H^\circ \left[\frac{\text{kJ}}{\text{mol}} \right] * \text{product titer} \left[\frac{\text{mol}}{\text{L}} \right]}{\text{product titer} \left[\frac{\text{kg}}{\text{L}} \right] * \left(\frac{c_{p,\text{mol,product}}}{M_{\text{product}}} \right) + \left(1 - \text{product titer} \left[\frac{\text{kg}}{\text{L}} \right] \right) * c_{p,\text{mass,water}}}$$

$$\text{❖ } \Delta T_{\text{isobutene}} = \frac{-\Delta_r H^\circ \left[\frac{\text{kJ}}{\text{mol}} \right] * \text{product titer} \left[\frac{\text{mol}}{\text{L}} \right]}{c_{p,\text{vol,water}}}$$

❖ Example: CO₂ to n-Butanol

- Hypothesis: (no metabolic leakage)
- $4 \text{ CO}_2 + 12 \text{ H}_2 \rightarrow \text{C}_4\text{H}_9\text{OH} + 7 \text{ H}_2\text{O}$
- Heat of reaction calculated from enthalpy of formation → exothermic

HEAT MANAGEMENT



- ✦ Probably impossible to reach more than 10-20 g/L without external cooling
- ✦ Low Titrers = High Capital Cost
- ✦ 100 kt/year of lactic acid = energy loss of 93 900 MWh/year = equivalent of the energy consumed by more than 14 000 Europeans in their households.

PROCESS SOLUTIONS

❖ Option 1: Internal heat exchanger.

- High heat exchange area
- Occupy a lot of volume in a pressurized vessel → cost

❖ Option 2: External heat exchanger, on a liquid loop

- Same heat exchange area, but at reduced pressure
- Recirculation loop → Pumps needed and large volume to circulate at low titer.
- Impurities can accumulate

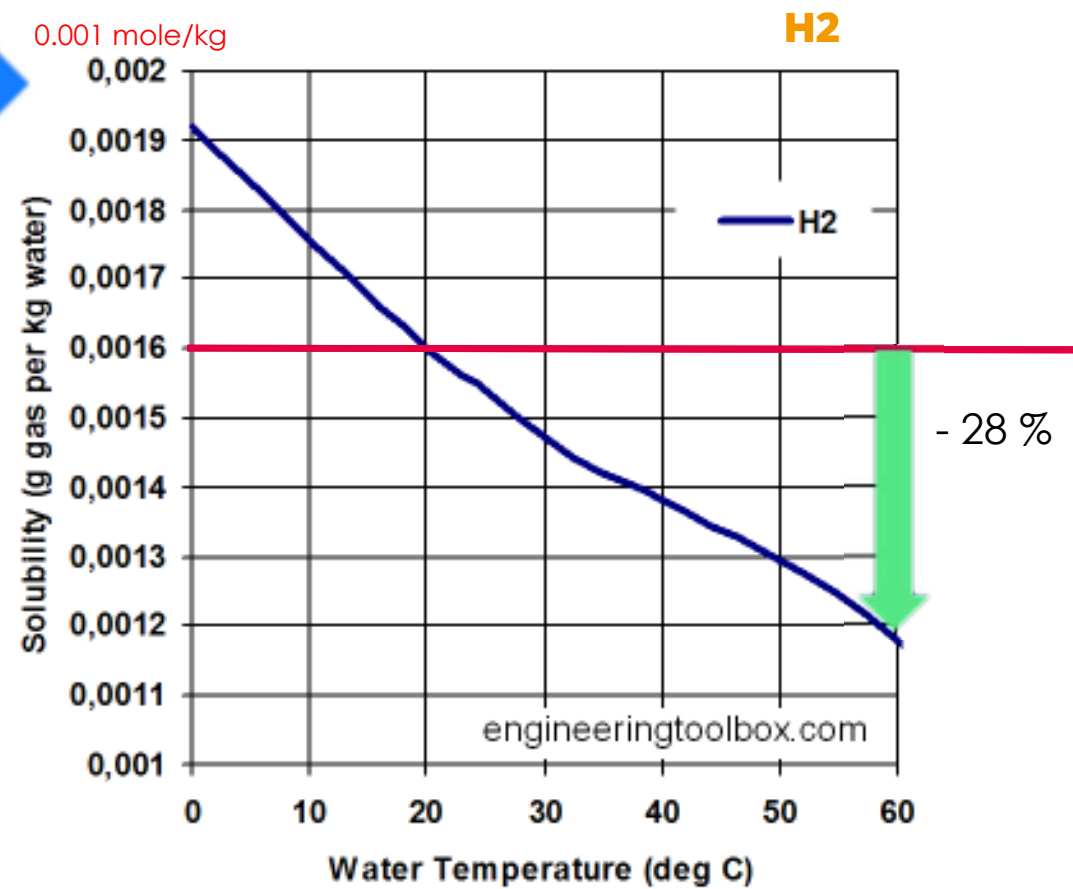
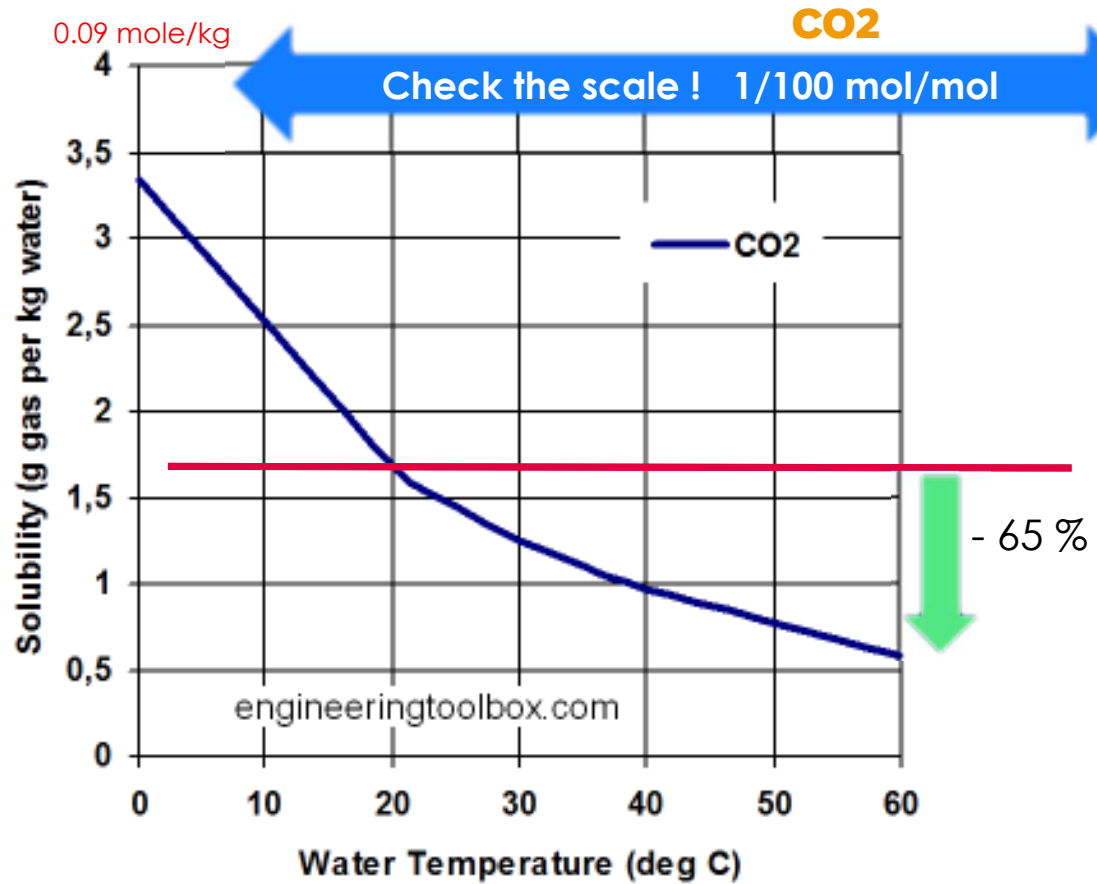
❖ Option 3: Continuous feed of fresh water, in line with adiabatic temperature rise to keep reactor temperature constant.

- Titer might be limited → High extraction cost

❖ Option 4: Don't use hydrogen... Or any other good idea.

GAS SOLUBILITY IN WATER VS TEMPERATURE (solubility decreases with temperature)

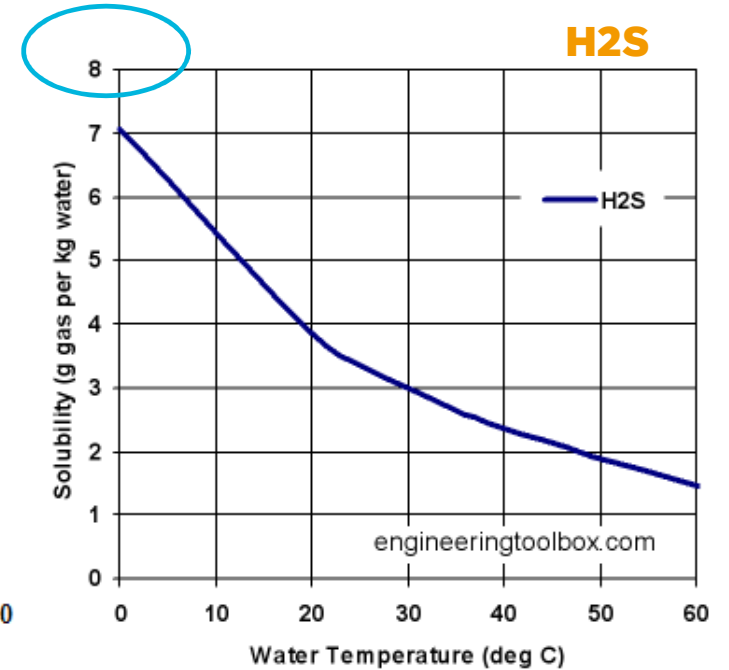
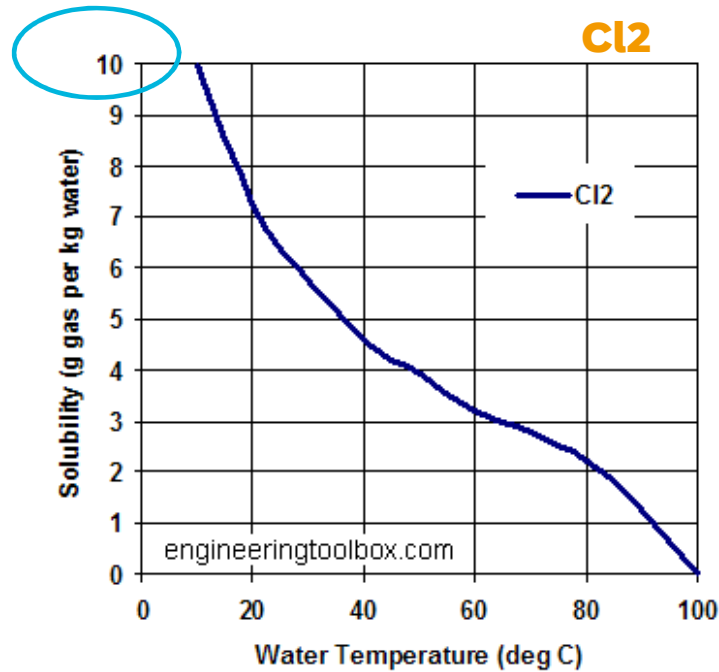
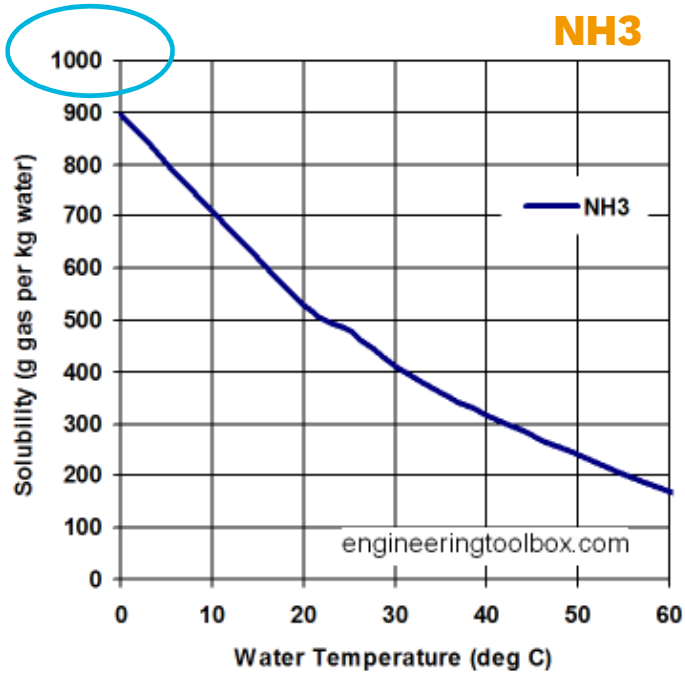
(source: Engineeringtoolbox.com)



→ Decreased solubility to be compensated by an increased pressure

IMPACT OF GAS IMPURITIES

Impurities have a higher solubility and can accumulate in a liquid loop



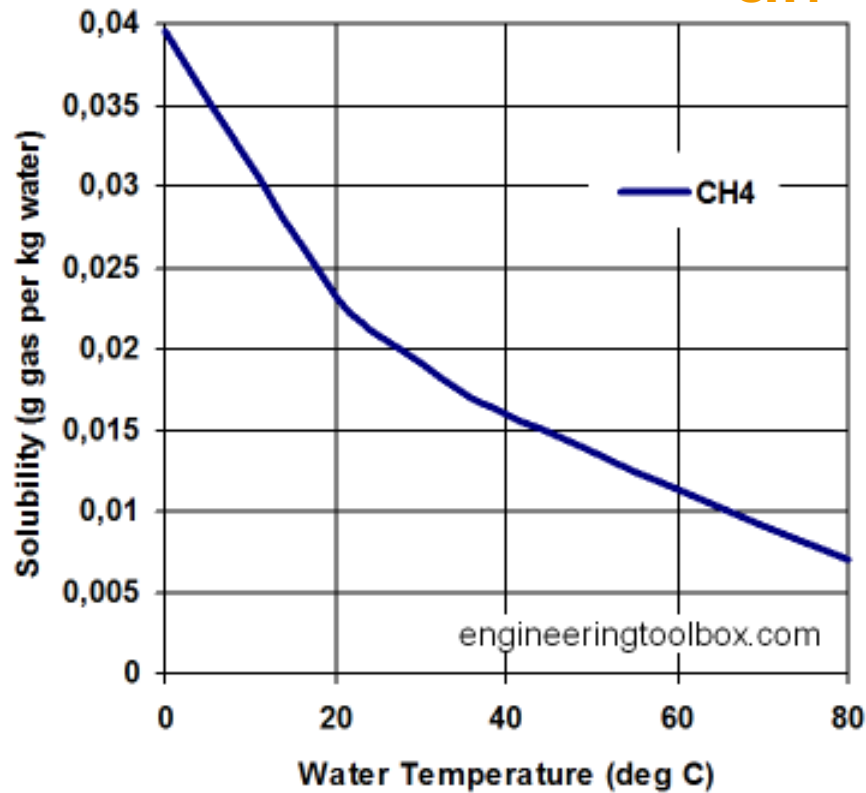
- ❖ To be checked for any other impurities
- ❖ Significant solubilities of some impurities that could accumulate

ALTERNATIVE CARBON SOURCES – Gas solubilities similar to H₂

(H₂ at 0°C: 0.001 mol/kg, CO₂ at 0°C: 0.09 mol/kg)

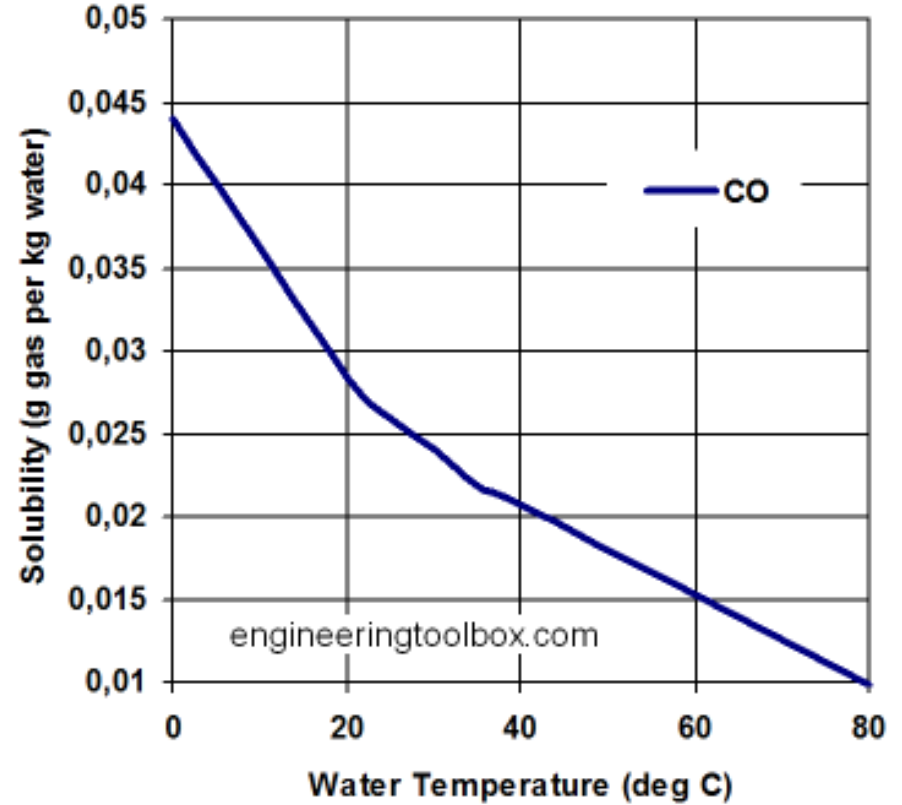
0.0025 mole/kg

CH₄



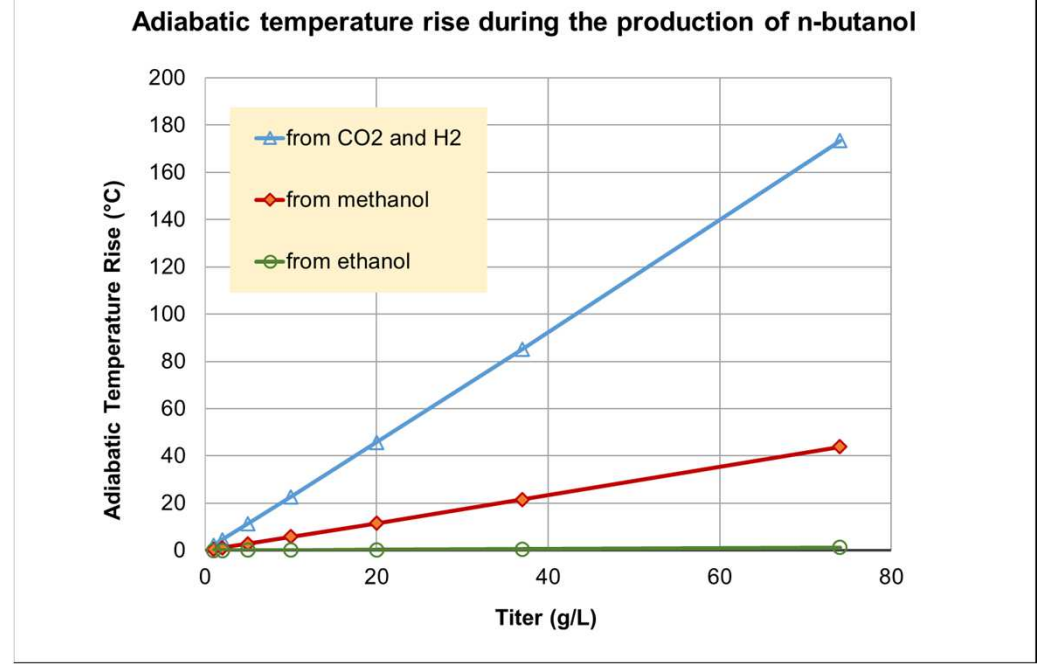
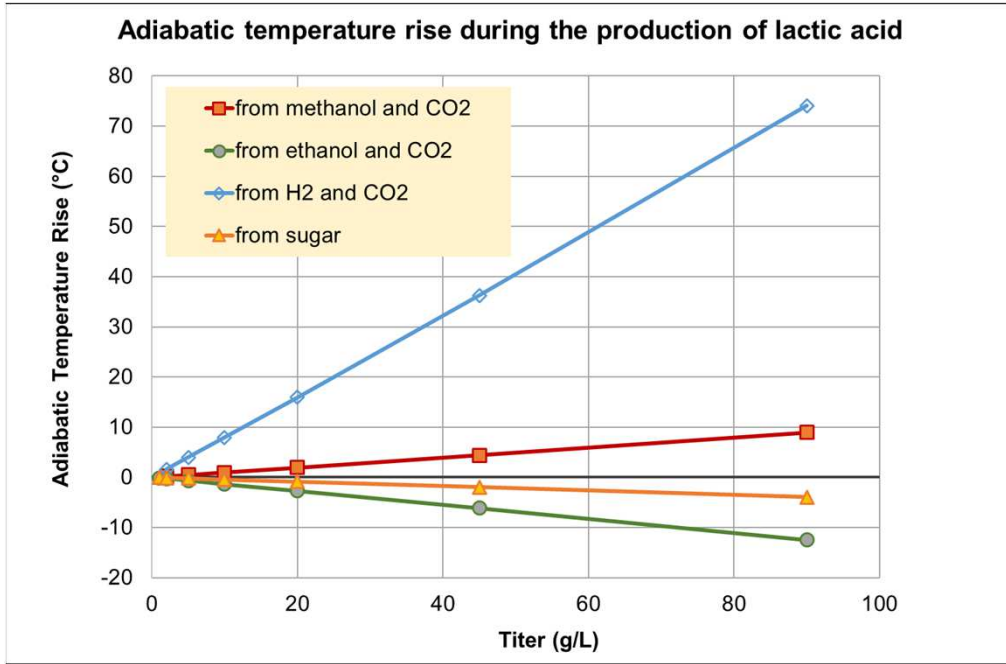
0.0018 mole/kg

CO



ADIABATIC TEMPERATURE RISE:

H₂ makes the process difficult, other reducing agents to be considered



	Reaction	$\Delta_r H^\circ$ (kJ/mol)
From H ₂ and CO ₂	$3 \text{ CO}_2 + 6 \text{ H}_2 \rightarrow \text{C}_3\text{H}_6\text{O}_3 + 3 \text{ H}_2\text{O}$	-298
From methanol and CO ₂	$2 \text{ CH}_4\text{O} + \text{CO}_2 \rightarrow \text{C}_3\text{H}_6\text{O}_3 + \text{H}_2\text{O}$	-36
From ethanol and CO ₂	$\text{C}_2\text{H}_6\text{O} + \text{CO}_2 \rightarrow \text{C}_3\text{H}_6\text{O}_3$	50
From sugar	$\text{C}_6\text{H}_{12}\text{O}_6 \rightarrow 2 \text{ C}_3\text{H}_6\text{O}_3$	32

	Reaction	$\Delta_r H^\circ$ (kJ/mol)
From H ₂ and CO ₂	$4 \text{ CO}_2 + 12 \text{ H}_2 \rightarrow 1 \text{ C}_4\text{H}_9\text{OH} + 7 \text{ H}_2\text{O}$	-701
From methanol and CO ₂	$4 \text{ CH}_4\text{O} \rightarrow 1 \text{ C}_4\text{H}_9\text{OH} + 3 \text{ H}_2\text{O}$	-177
From ethanol and CO ₂	$2 \text{ C}_2\text{H}_6\text{O} \rightarrow 1 \text{ C}_4\text{H}_9\text{OH} + 1 \text{ H}_2\text{O}$	-5

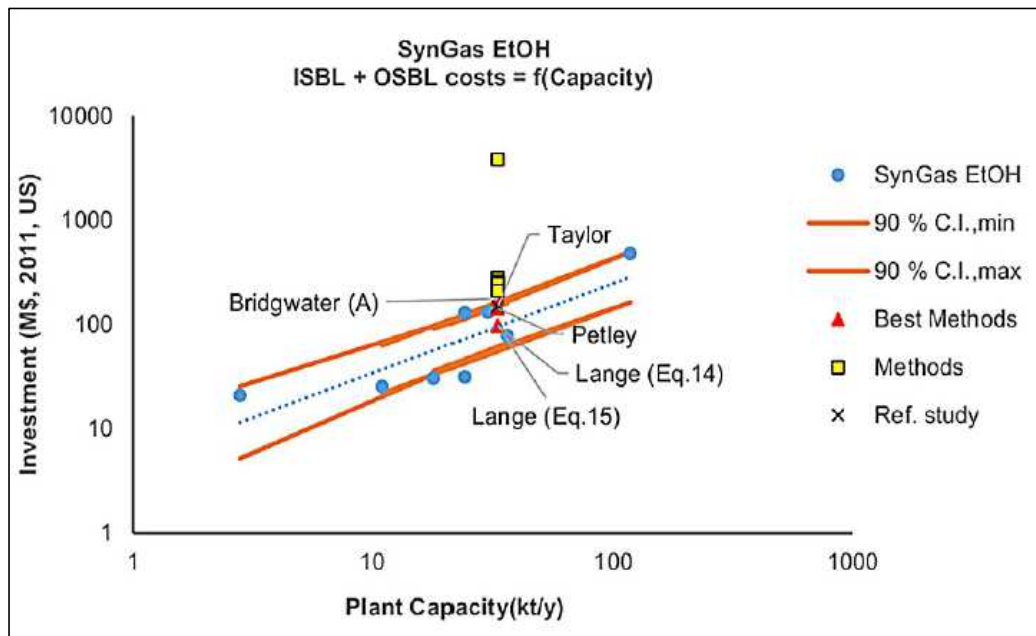
❖ Challenging to have high titer, from CO₂/H₂ and good heat management. Methanol as alternative

CAPITAL COST ESTIMATES

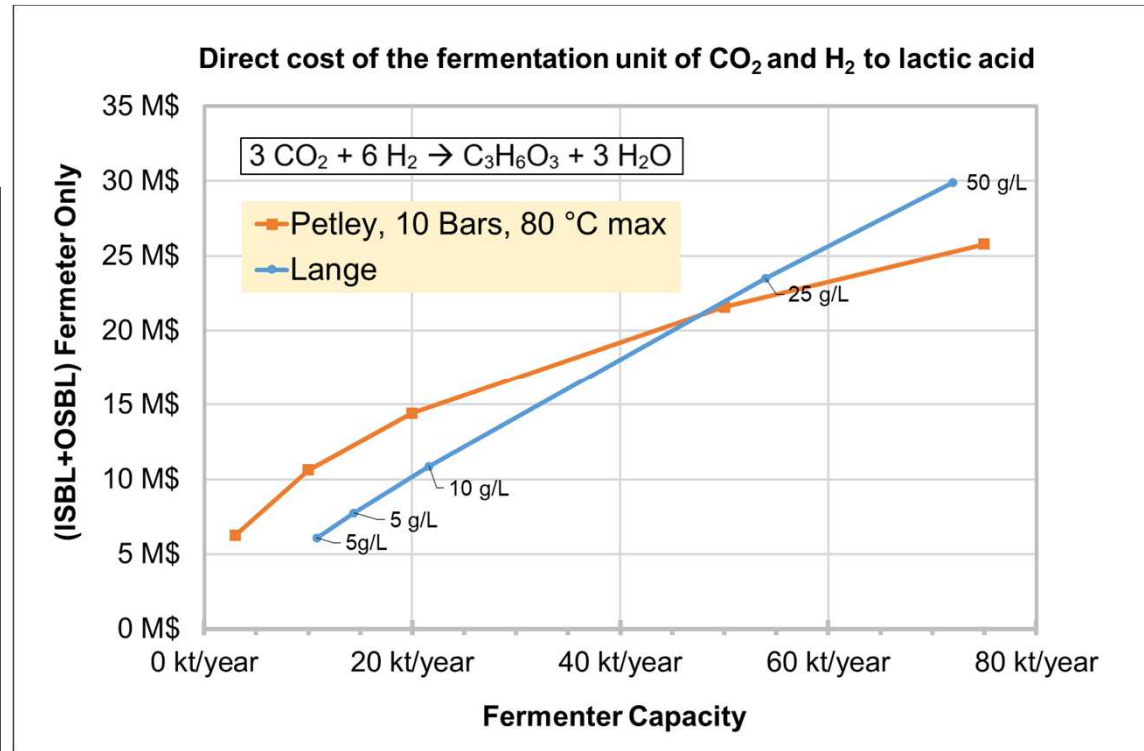
2 methods: Petley and Lange, Cost evaluation for the fermenter

❖ Petley: based on pressure and temperature

❖ Lange: based on heat loss



Early-Stage Capital Cost Estimation of Biorefinery Processes: A Comparative Study of Heuristic Techniques, M Tsagkari, JL Couturier, A Kokossis and JL Dubois, **ChemSusChem** 2016, 9, 2284 – 2297



Other main equipments: Compressor, Filtration, Separation, water treatment, off gases treatment,...

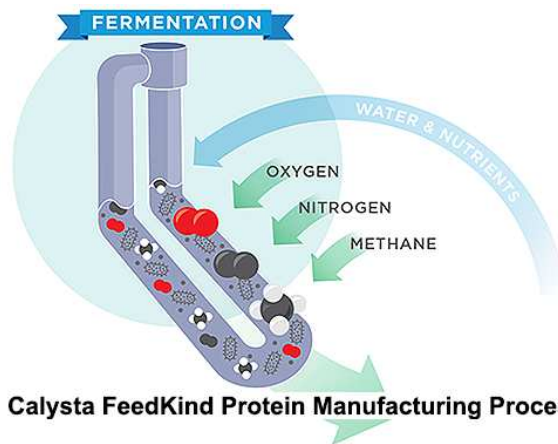
INDUSTRIAL SCALE GAS FERMENTORS: 4 DIFFERENT TECHNOLOGIES



INEOS Gas (CO/H₂) fermenter (Idled)
Ethanol



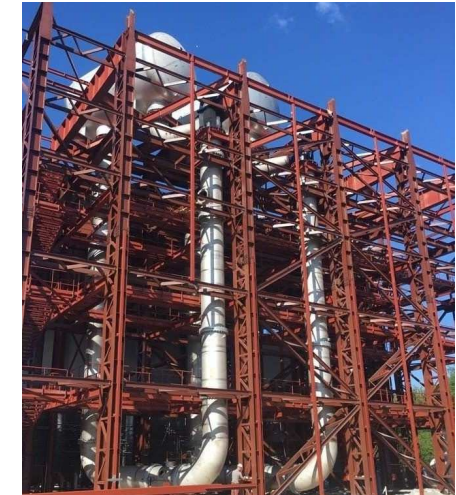
Calysta Gas (CH₄) fermenter
Proteins



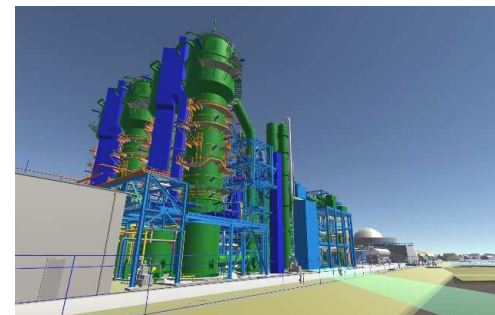
Calysta FeedKind Protein Manufacturing Process



Lanzatech/Shougang Gas (CO/H₂/CO₂) Fermenter
Ethanol



Unibio Gas (CH₄) Fermenter
Proteins



Lanzatech/Arcelor Mittal (under construction)
Ethanol

INDUSTRIAL SCALE GAS FERMENTATION PROCESSES: 3 – 6000 \$/T PRODUCT

	Ineos Bio	Calysta	Lanzatech	Unibio	Coskata
Location	USA	China	Belgium	Russia	USA
Product	Ethanol & Electricity	Proteins	Ethanol	Proteins	Ethanol
Feedstock	Biomass to Syngas	Methane	CO	Methane	CO
Capacity product	24 kt/y 8 MW	20 kt/y	63 kt/y	6 kt/y	118 t/y (pilot/demo)
CAPEX	130 M\$ (2011)	80 M\$ (2020)	180 M\$ (2020)	35 M\$ (2016)	25 M\$ (2008)
Technology	Stirred tank / Bubble column	Loop reactor	Jet Loop reactor	U-loop	

HEAT MANAGEMENT

❖ **Challenges in heat management: a lot of heat is produced at low temperature.**

❖ **What to do with the heat produced?**

- Use for downstream/upstream process steps?
- Use in district heating?
- Use in green houses?

❖ **Challenges for the process:**

- Higher temperatures would be preferable: better value for the heat.
- May require extremophiles, enzymatic process
- But gas solubility is decreasing at higher temperature...
- And microorganisms survival might be compromised.

❖ **Heat losses have to be seen in light of the production capacity**

- Not detectable at lab scale
- May represent the energy consumption of several 10 000 European citizens at 100 000 tons/year.

THANK YOU FOR YOUR ATTENTION

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 BioRECOVER

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