

This project has received funding from the European Union's Horizon 2020 research and innovation program under the Marie Sklodowska-Curie grant agreement No. 859885.



# <u>C-PLANET</u> NTE 1 – ESR11 – MICROTEACHING 3

Amir Bashirgonbadi Sept. 9, 2020





#### **AMIR BASHIRGONBADI**

- Graduated as MSc materials engineer@ KU Leuven
- Then, I served as a Sales Engineer in a polymer compounding company, in Iran
- PhD: ESR 11, started in May









— Where are they used?

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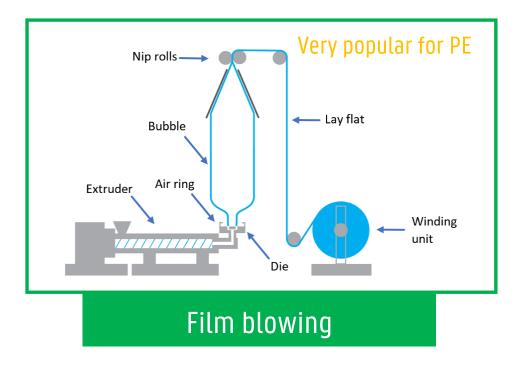


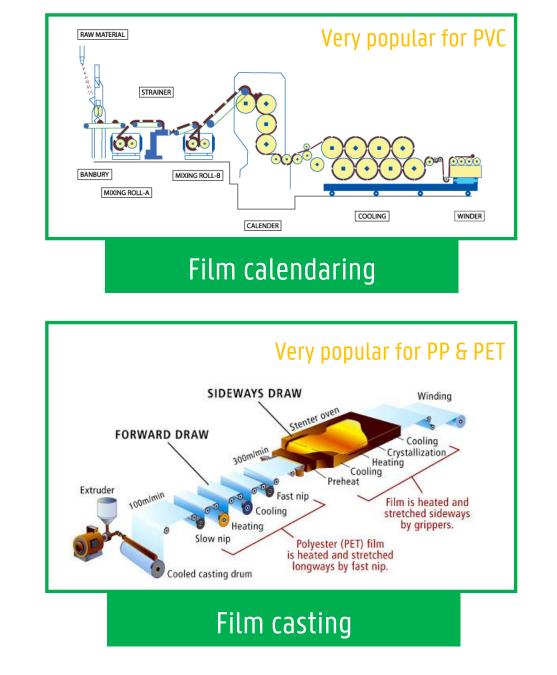


# And millions of more applications!

# **HOW ARE THEY PRODUCED?**

Very different techniques!For example these three:

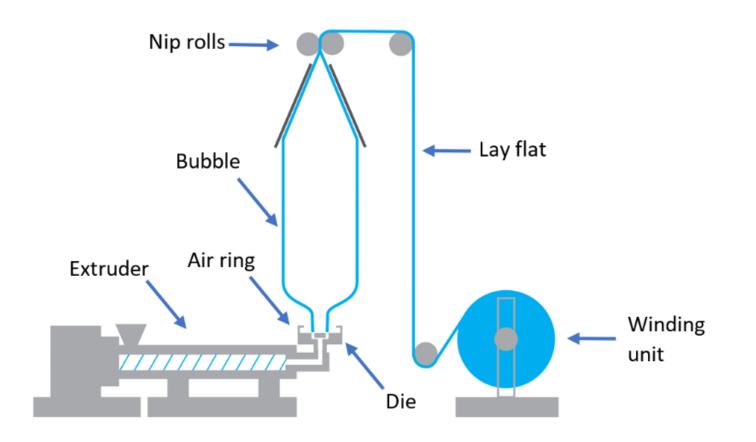






# FILM BLOWING PROCESS PARTS

— Or: Tubular film extrusion







# **RESEARCH QUESTION**

How can we quantify (and enhance) the Recycling Quality of the contaminated polyethylenes in film blowing applications?

 Contaminations? For the moment, cross-polymer contaminations: other PEs, PP, PET, PS, and PA

 $RQ = \alpha \times (Blowability) + \beta \times (Properties)$ 

<u>Objective</u>: to be able to make a choice of film-blowable contaminated PEs

- 1. A technique to define and measure blowability needs to be developed
- 2. Alpha and Beta coefficients should be assigned
- 3. RQ should be predictable for certain (distribution of) molecules/blends



# **IS IT EASY TO MAKE FILMS FROM RECYCLED PLASTICS?**

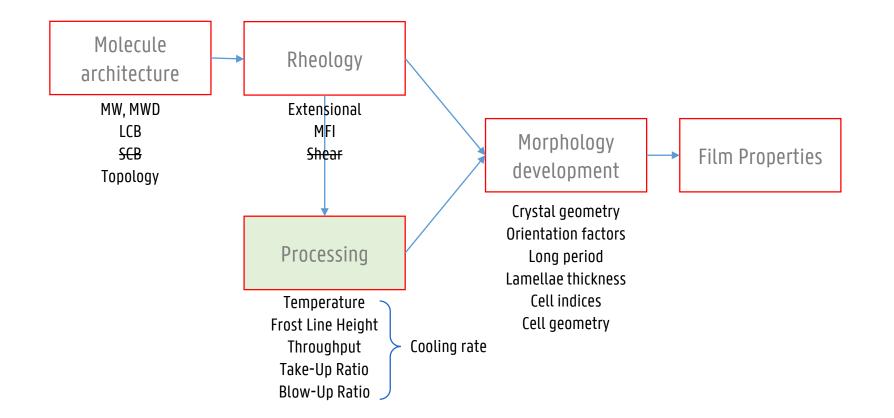
#### Challenges:

- Flow behavior
- Phase morphology
- Mechanical properties
- Aesthetics and smell
- Food-contact limitations





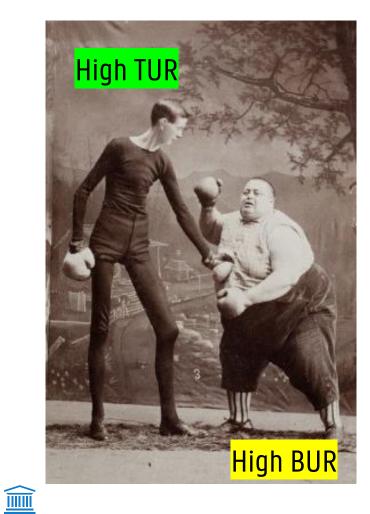
#### AN OVERVIEW OF THE FILM BLOWING PROCESS





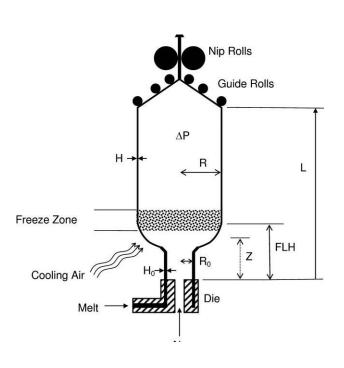
# **PROCESSING PARAMETERS: BUR, TUR, AND FLH**

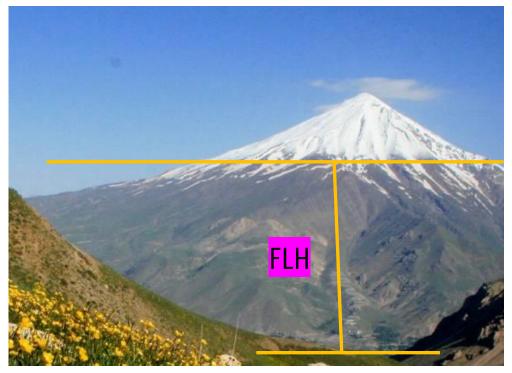
BUR: Blow up ratio, TUR: Take up ratio, FLH: Frost line height



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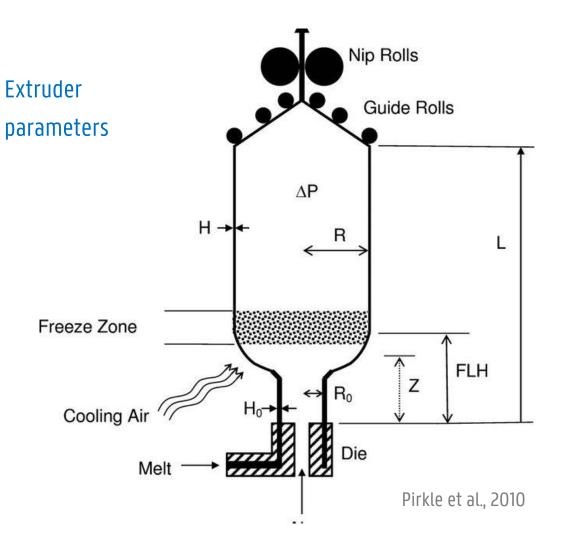
Mount Damavand, 5610m high, back in my hometown

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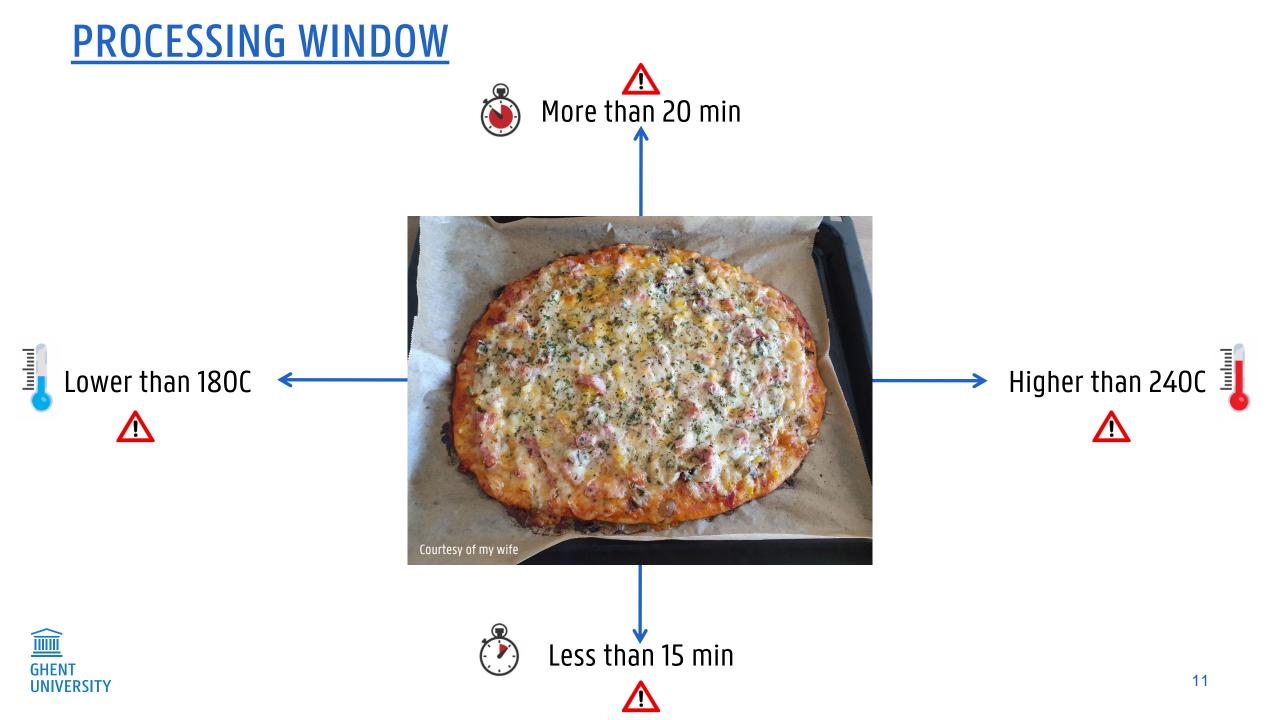
# FILM BLOWING PROCESS VARIABLES

#### Main parameters in this process are as follows:

- 1. Melt temperature, which is controlled by the extruder heating elements.
- 2. Throughput, which is controlled by the rotation speed of the extruder screw.
- 3. Blow up ratio, which is the ratio of the radius of the inflated bubble to the diameter of the die
- 4. **Take up ratio**, which is the ratio of the vertical speed of the material coming out of the die to the linear speed of the nip roller
- 5. Frost line height, which is the height from the die surface where the polymer is frozen and is not deformable anymore, and is controlled by the cooling unit.

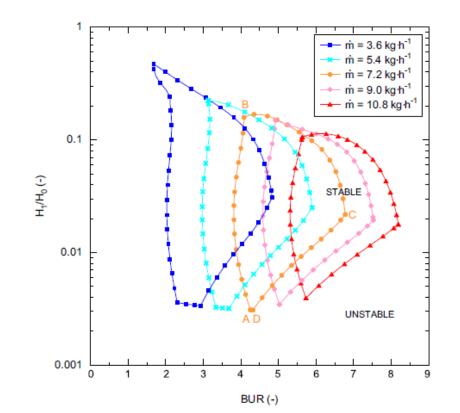


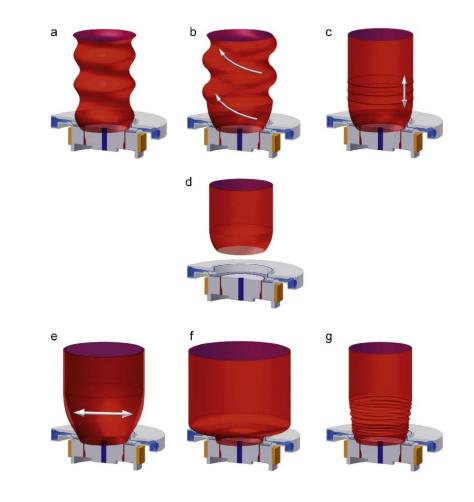




# **BUBBLE STABILITY – DIRECT METHODS**

- Current definitions:
  - Bubble instabilities
  - Processing window

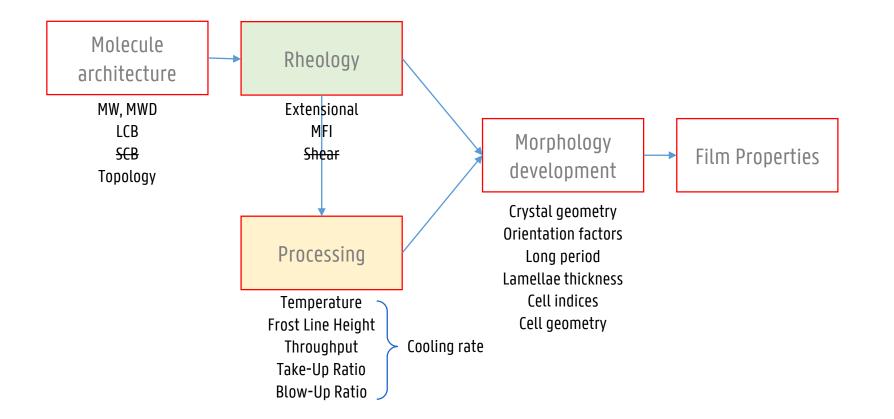




Roman Kolařík PhD Thesis, 2012



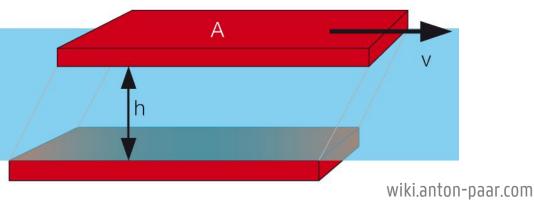
#### **FILM BLOWING PROCESS**





# SHEAR VISCOSITY OR EXTENSIONAL VISCOSITY?

Shear deformation

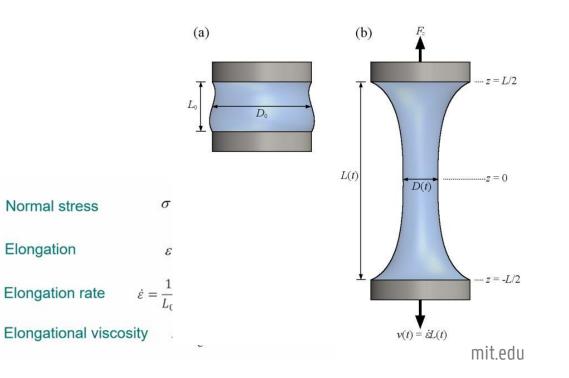


- Extensional deformation
  - This is what we see in

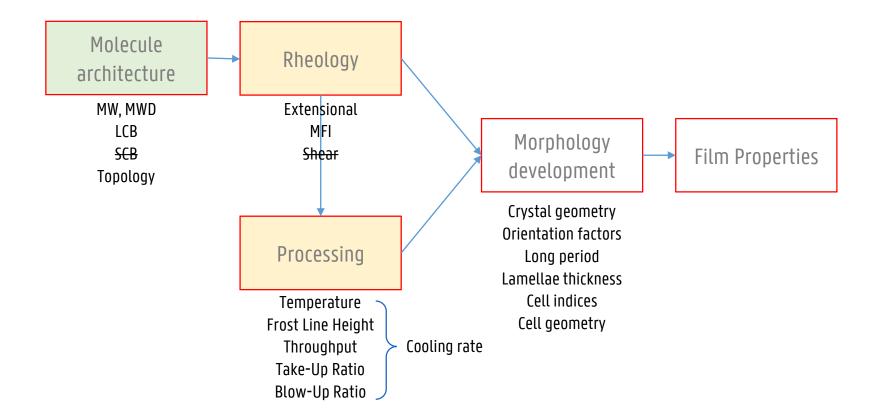
#### processes like film blowing



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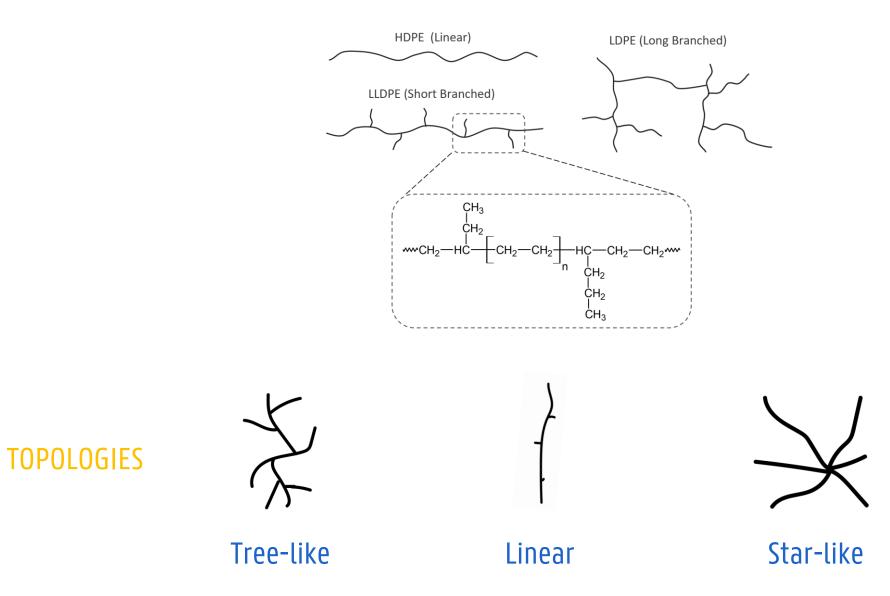


#### **FILM BLOWING PROCESS**



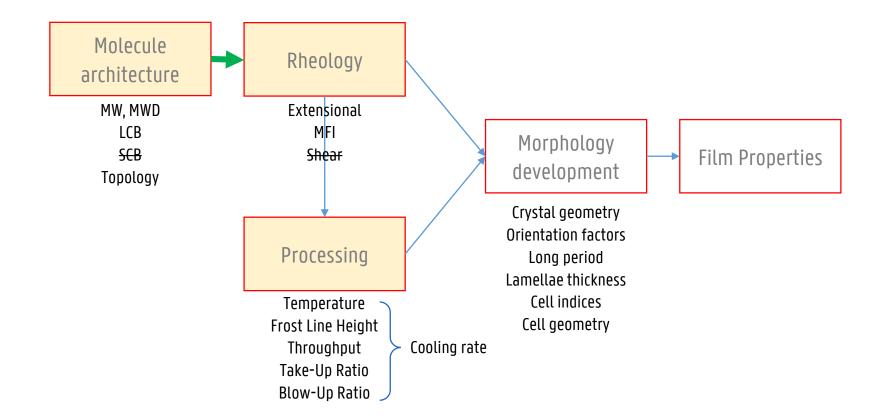


#### **DIFFERENT POLYETHYLENES**



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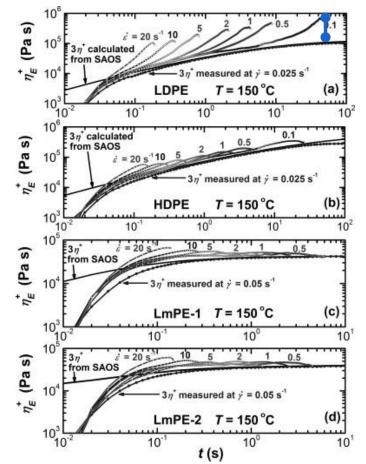
#### **FILM BLOWING PROCESS**





### **SHEAR VS EXTENSIONAL VISCOSITY**

Branched PEs exhibit strain hardening, while linear PEs stick to their linear viscoelastic behavior



GHENT UNIVERSITY Strain hardening factor

# **EXAMPLE OF RHEOLOGY VS MOLECULAR ARCHITECTURE**

#### Four Behaviors:

- 1: Strain rate 1 Strain hardening no difference
  - 2: Strain rate  $\uparrow$  Strain hardening  $\downarrow$   $\succ$

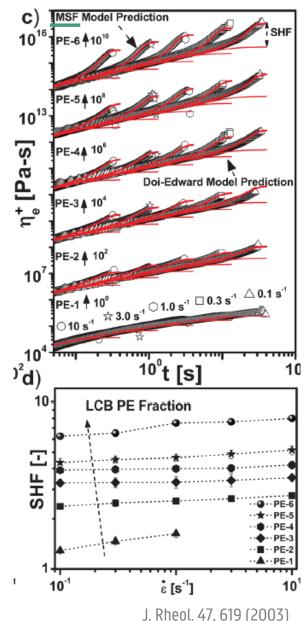
3. Strain rate 个 - Strain hardening ↑ 若

4: Strain rate 个 - No strain hardening

Typical for metallocene catalyzed PE

#### SHF indicates Network Strength

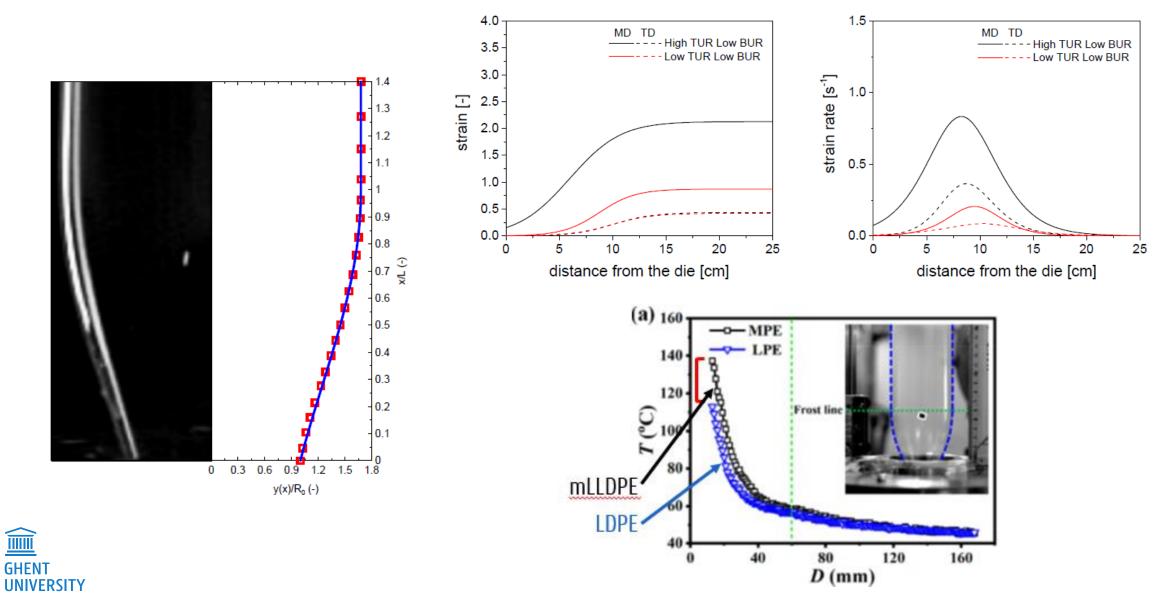
A high network strength implies that the applied stress cannot disrupt the network to soften the material. Molecular stress function



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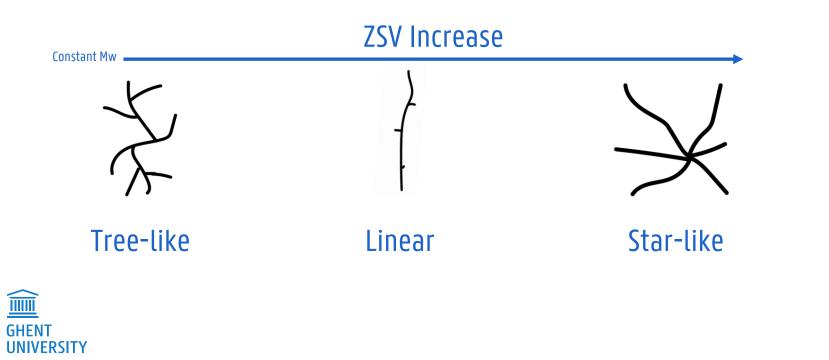


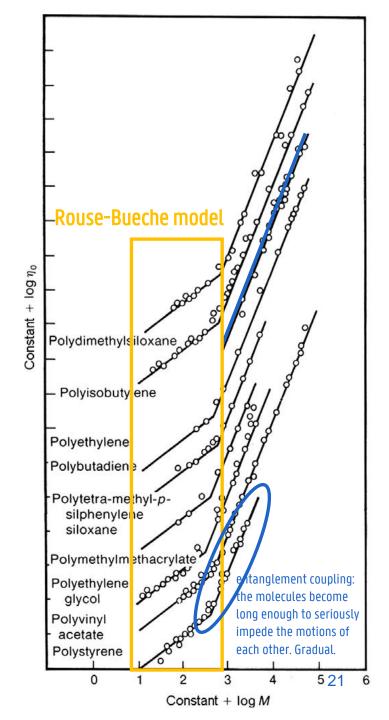
#### **DIFFERENT STRAINS AND STRAIN RATES AT DIFFERENT TEMP.**



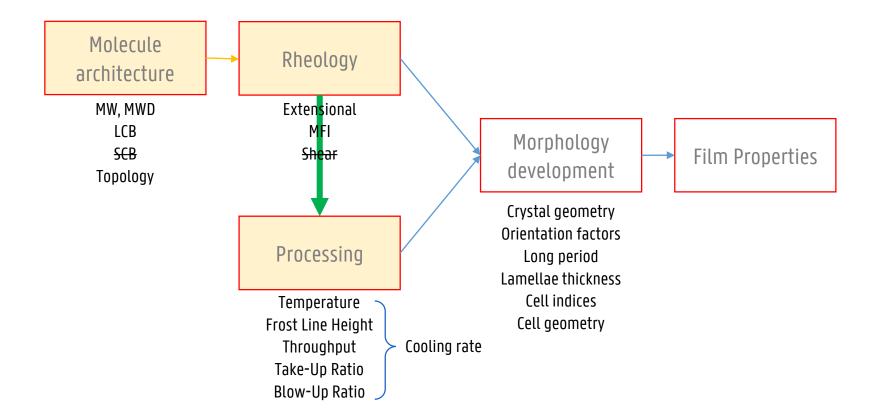
# **MOLECULAR TOPOLOGY AND MW VS ZSV**

- For linear PE (at 190C):  $\eta_0^L = 10^{-14.25} M_w^{3.6}$
- Star-like topology will have higher ZSV
- Tree-like topology will have lower ZSV





#### **FILM BLOWING PROCESS**



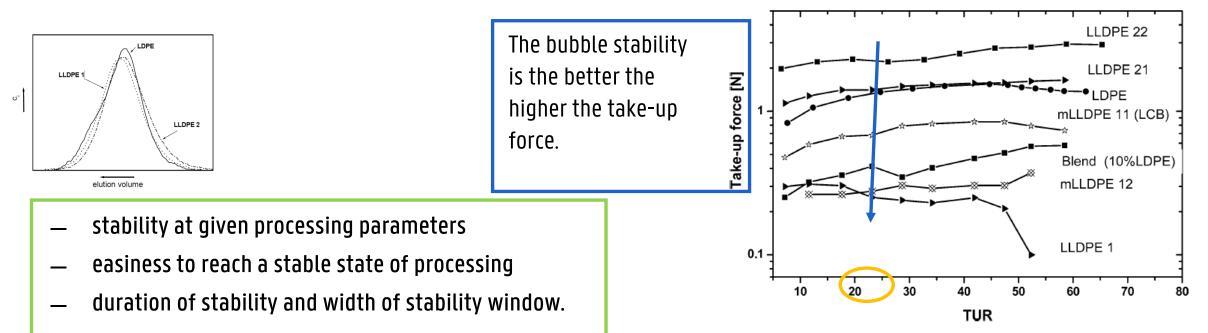


### **BUBBLE STABILITY - INDIRECT METHOD 2**

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Take-up force as a function of take-up ratio for various polyethylenes

	LLDPE 22	LLDPE 21	LDPE	mLLDPE 11	LLDPE/LDPE 90/10	mLLDPE 12	LLDPE 1
F[N] at TUR = 25 $3\eta_0$ [Pa s] at 150 °C $\mu$ [Pa s] at $\dot{\varepsilon}_0 = 0.5 \text{ s}^{-1}\varepsilon_{\text{H}} = 3$ and $T = 150 °C$	2.2 32×10 <sup>4</sup> ~50×10 <sup>4a</sup>	1.5 $11 \times 10^4$ $\sim 10 \times 10^{4a}$	1.4 $3.5 \times 10^4$ $10 \times 10^4$	0.7 $4.3 \times 10^4$ $7 \times 10^4$	$ \begin{array}{c} 0.4 \\ 1.6 \times 10^4 \\ 2.1 \times 10^4 \end{array} $	$0.3 \\ 3 \times 10^4 \\ 3 \times 10^4$	$0.2 \\ 1.5 \times 10^4 \\ 1.5 \times 10^4$
µ.[Pa s] at 150 °C Bubble stability	n.m. + +	n.m. + +	20×10 <sup>4</sup> +	8×10 <sup>4</sup> +	3.5×10 <sup>4</sup> +-	3×10 <sup>4</sup>	$1.5 \times 10^{4}$

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### **BUBBLE STABILITY - DIRECT METHOD**

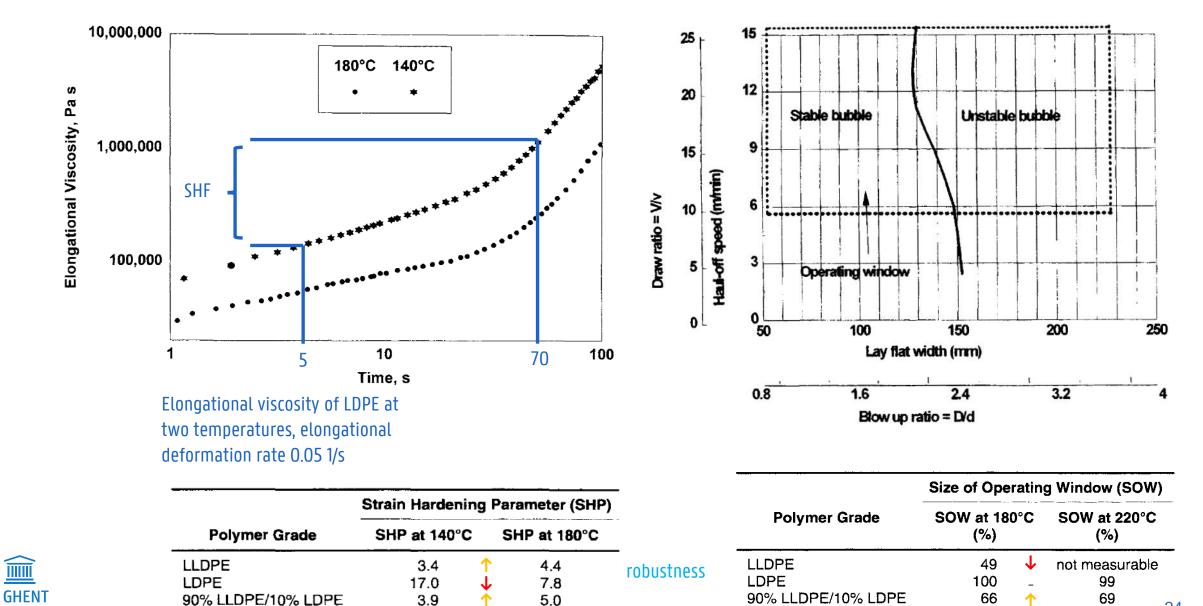
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80% LLDPE/20% LDPE

24

88



6.5

5.0

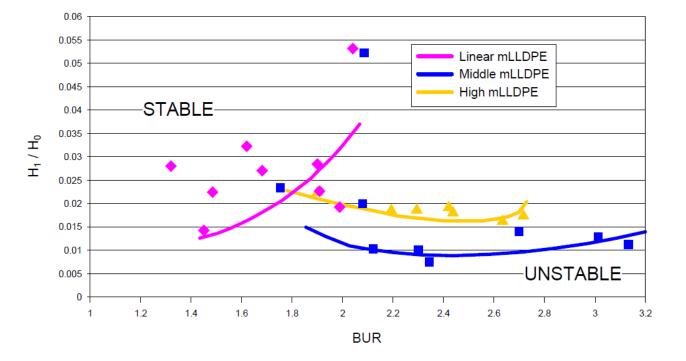
80% LLDPE/20% LDPE

85

#### **BUBBLE STABILITY CRITERIA – IDENTICAL PARAMETERS**



Scattered measurements?

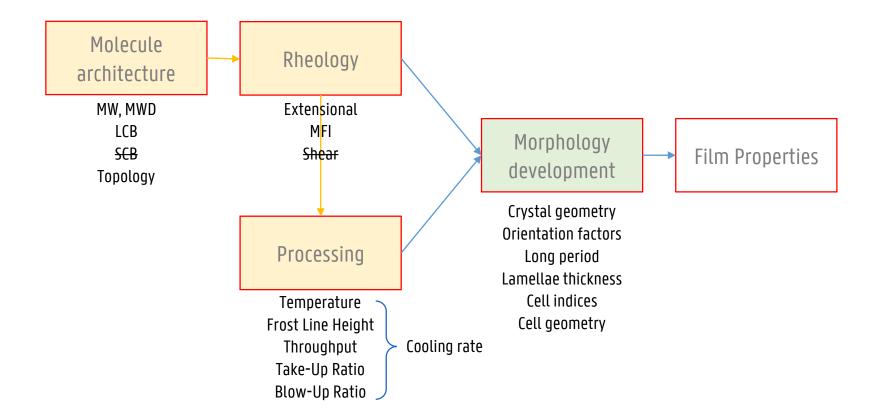


FLH 180mm and temperature 190°C

Roman Kolařík PhD Thesis, 2012

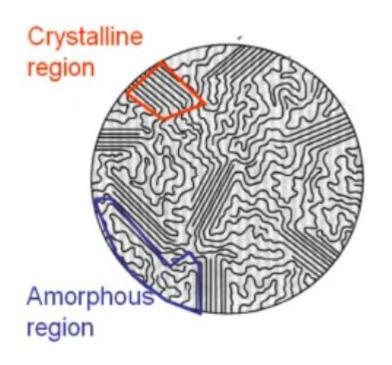


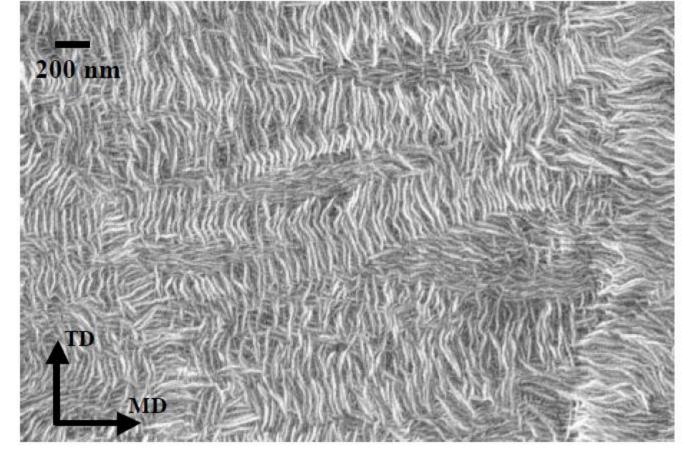
#### **FILM BLOWING PROCESS**





#### **ORIENTATION OF LAMELLA STRUCTURES - SEM**







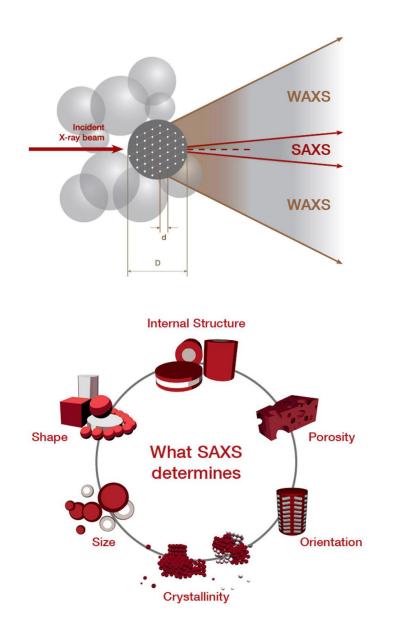


# **MORPHOLOGY CHARACTERIZATION**

- WAXS:
  - Orientation of crystals
  - Crystalline content
  - Lamellar thickness
  - Average crystal size
- SAXS:

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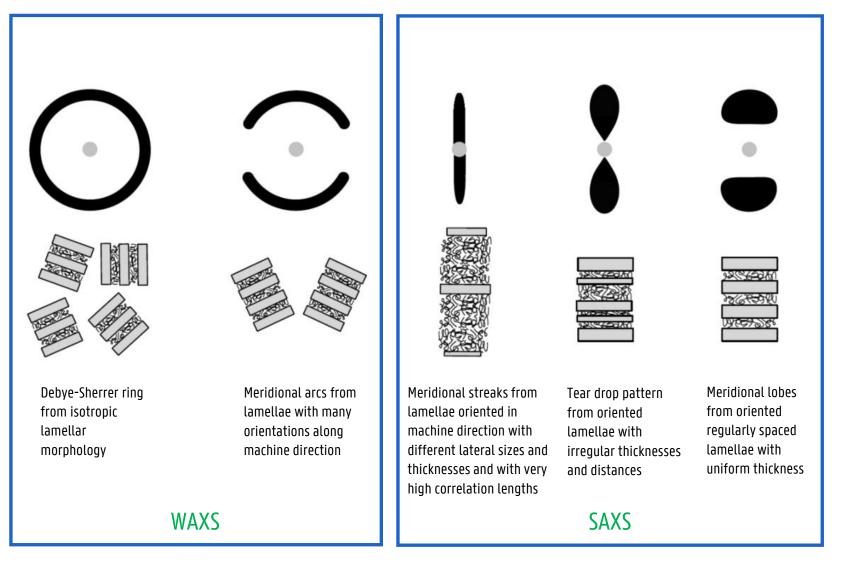
- Linear crystallinity
- Orientation of lamellas
- Lamellar thickness
- Long period



SALS, Raman Spectroscopy, Birefringence.

### **XRD RESULTS**

How to interpret the results?

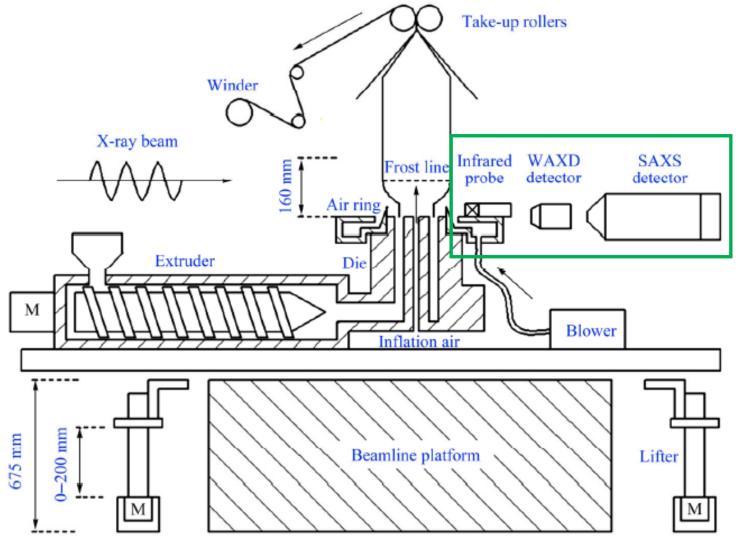




Troisi et al., 2016

### **ONLINE INVESTIGATION OF THE MORPHOLOGY**

Film blowing setup, with adjustable height, exposes the bubble to the X-ray radiation at different points





### **STRUCTURE DEVELOPMENT – ONLINE XS**

1997, On-Line Birefringence Measurement in Film Blowing of a Linear Low Density Polyethylene





Chinese Journal of Polymer Science Vol. 35, No. 12, (2017), 1508–1516

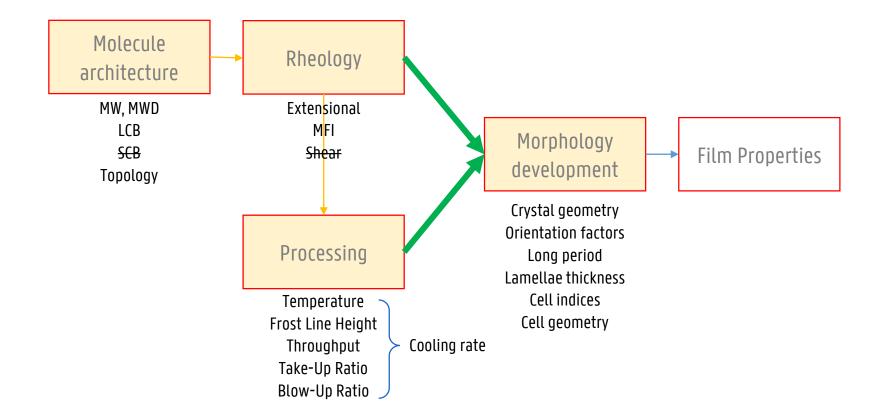




Dutch Belgian Beamline BM26B at the European Synchrotron Radiation Facility (ESRF, Grenoble, FR)

E.M. Troisi, M. van Drongelen, H.J.M. Caelers, G. Portale, G.W.M. Peters Eindhoven University of Technology European Polymer Journal 74 (2016) 190–208

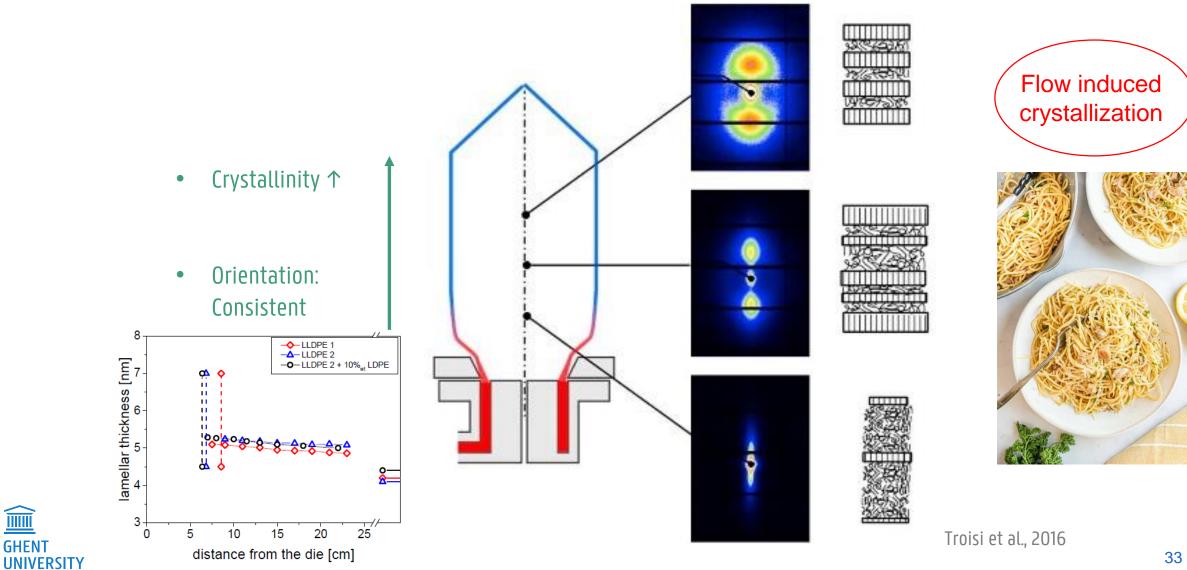
#### **FILM BLOWING PROCESS**





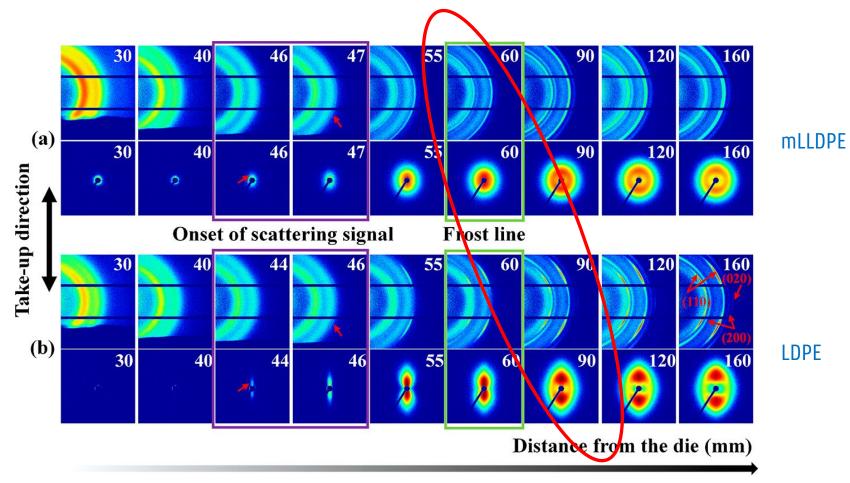
#### **MORPHOLOGY DEVELOPMENT ALONG BUBBLE**

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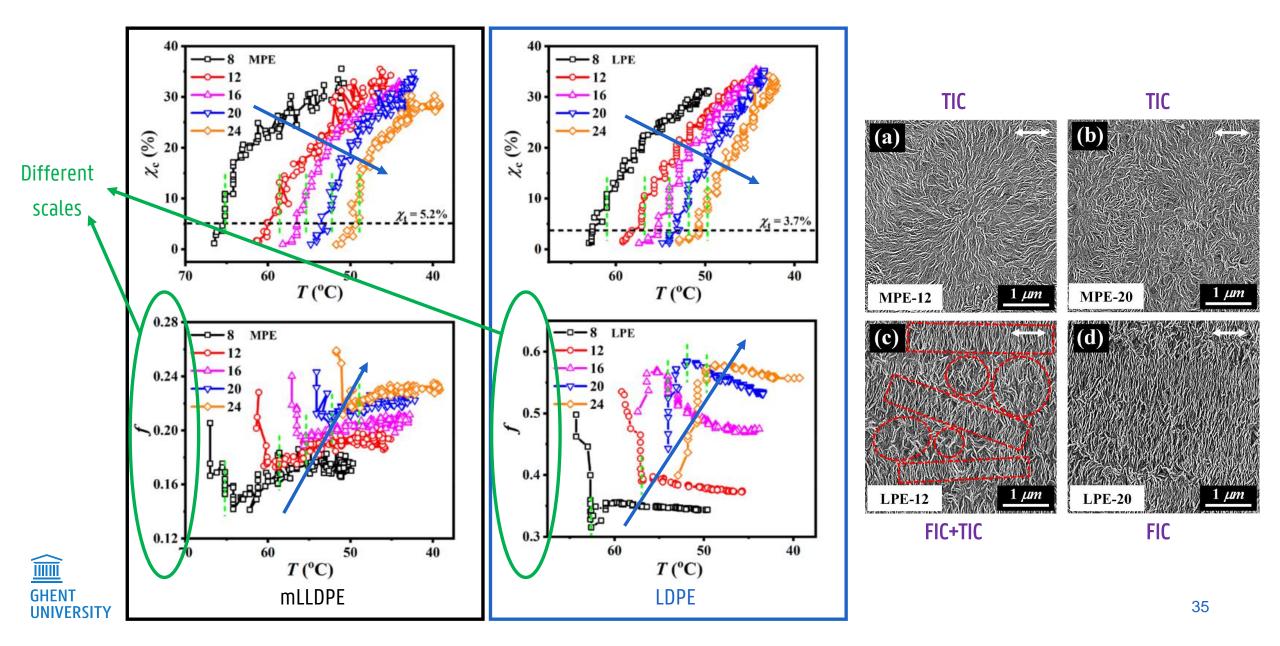
# **POLYMER EFFECT ON MORPHOLOGY**

Linear polymers tend to develop non-oriented structures, while branched polymers exhibit oriented morphologies





#### **MORPHOLOGY VS TUR**

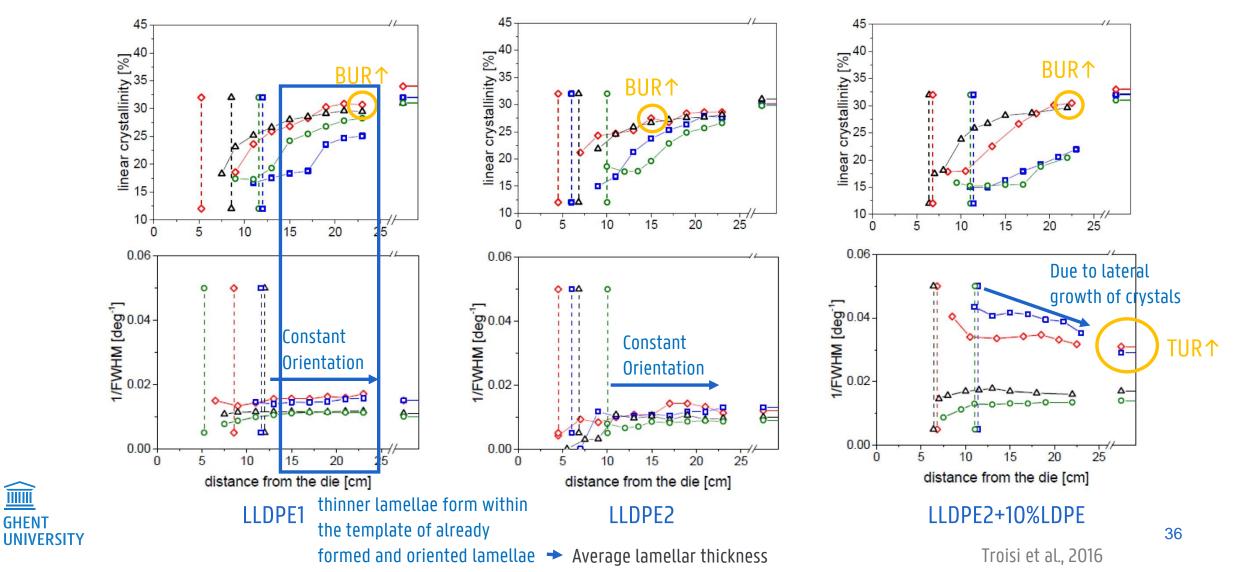


#### **ORIENTATION AND XC EVOLUTION**

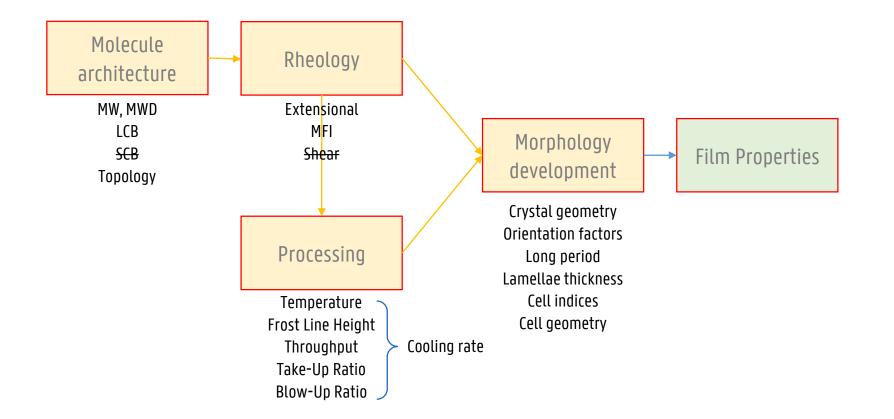
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—□— TUR↑-BUR↓ –**∆**– TUR↓-BUR↑ -O- TUR↓-BUR↓

	Mw (kg/mol)	PDI
LLDPE1	94	3.9
LLDPE2	108	2.4
LDPE	217	5.9

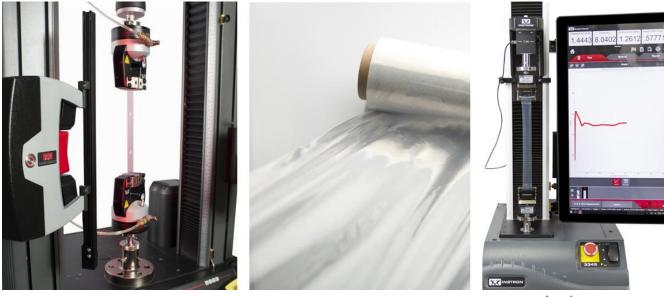


#### **FILM BLOWING PROCESS**





#### **FILMS MECHANICAL PROPERTIES**



instron.us

Static loading condition Tensile testing

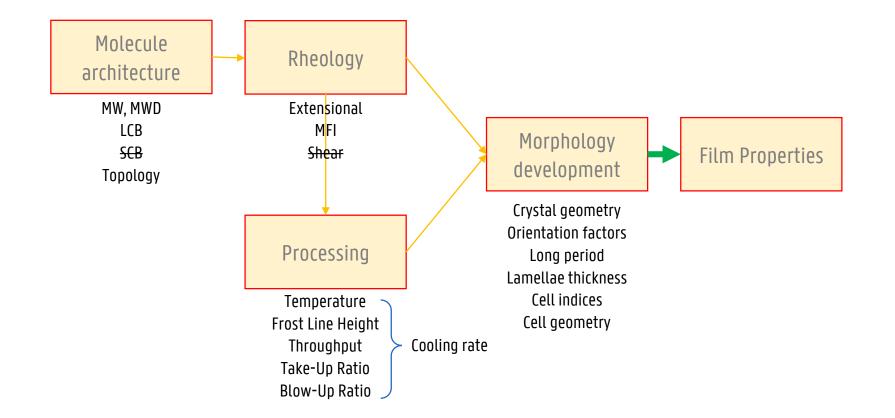


labthink.com

Dynamic loading condition Dart drop testing

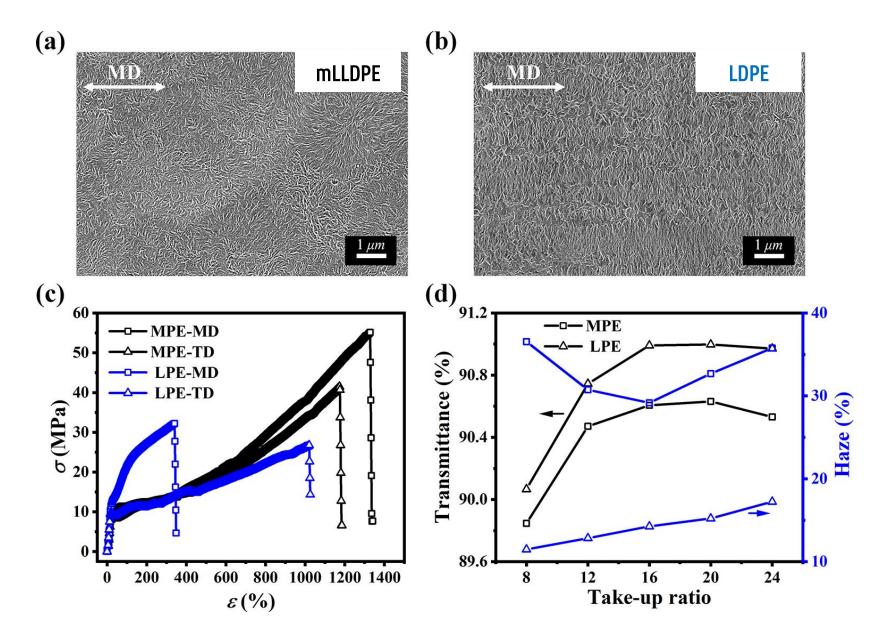


#### **FILM BLOWING PROCESS**





#### **ANISOTROPIC PROPERTIES, POLYMER EFFECT**

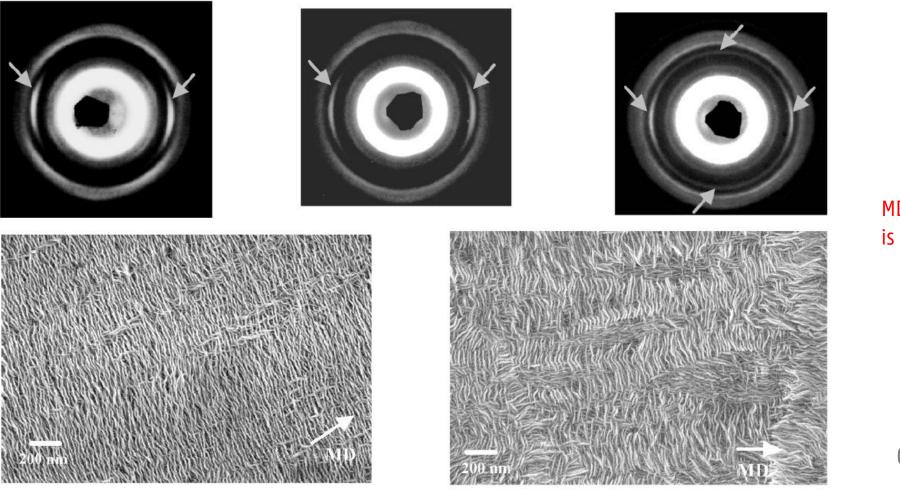


#### **Branched PE:**

Lower mechanical properties, higher anisotropy, higher optical properties, and better processability



#### **FLH VS CRYSTALLINE STRUCTURE**



MD Orientation is decreased

Godshall, 2003



- FLH ↑
- Dart impact ↑

TD tear  $\downarrow$ 

MD tear ↑

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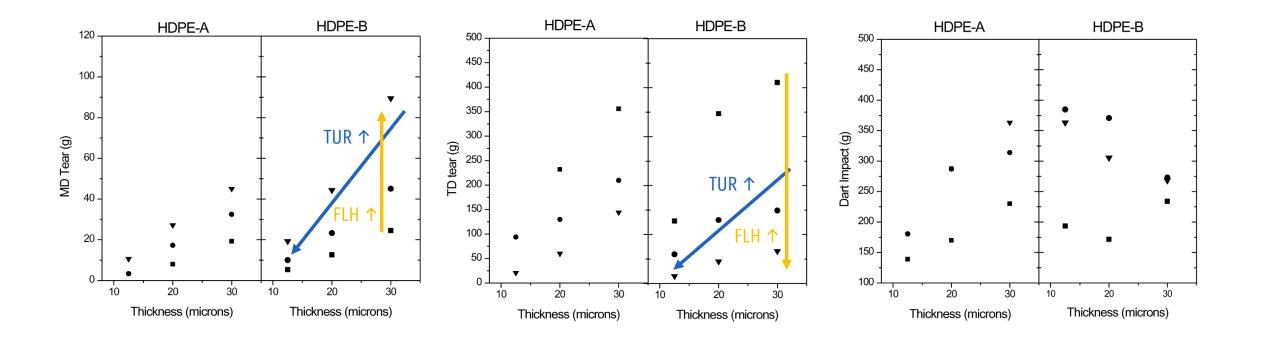




# **MECHANICAL PROPERTIES VS TUR**

#### In linear PE:

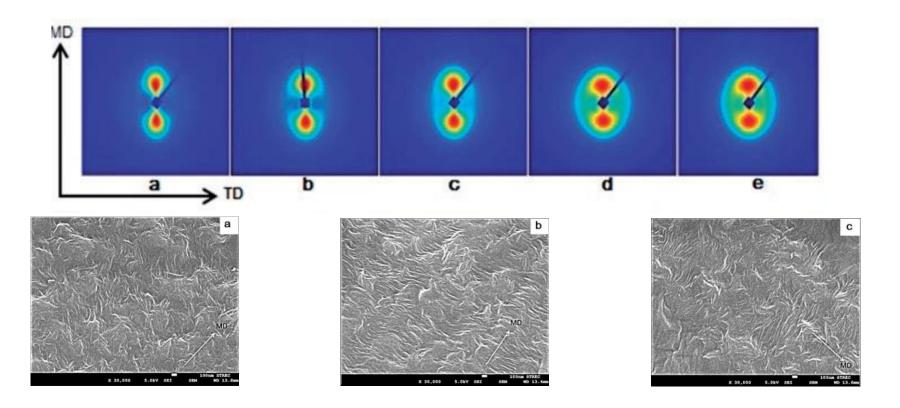
As the FLH increases, MD Tear increases, and TD Tear substantially degrades, dart drop resistance is mixed!





# **BUR VS CRYSTALLINE STRUCTURE**

Not very different mechanical properties but different barrierity as a result of BUR changes for linear PE





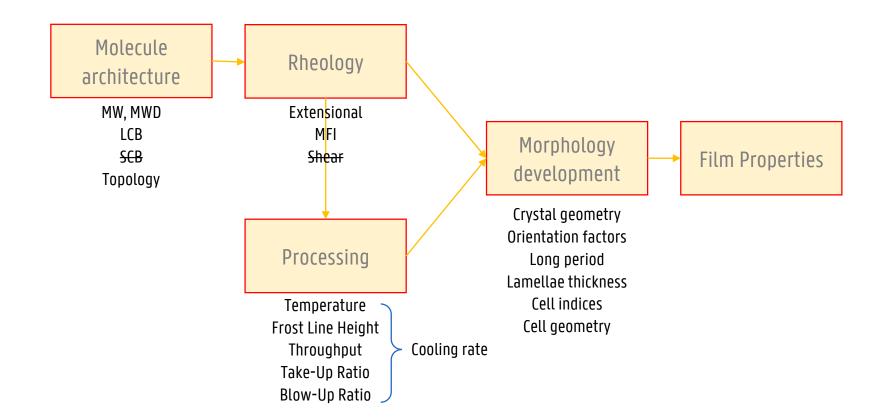
BUR ↑

- WVTR ↑
- 0TR ↑

**Constant thickness** 

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# ESR 11 EXPERIMENTS PLANNING - MATERIAL

- A choice of film blowing grade PEs are made available.
  - 3 LDPEs: Different in MW and LCB content
  - 3 LLDPEs: Different in comonomer type and content but at the same MW
  - 2 HDPEs: Different in PDI but at the same MW

Grade	MW	LCB content	Info
LDPE 1	A	D	Topology and MWD are known
LDPE 2	A	С	Topology and MWD are known
LDPE 3	В	C	Topology and MWD are known

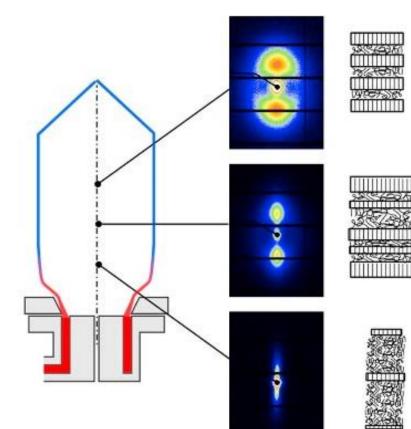
Grade	MW	Comonomer	Comonomer	Info
		type	content	
LLDPE 1	Н	I	K	MWD is known.
LLDPE 2	Н	1	L	MWD is known.
LLDPE 3	Н	J	L	MWD is known.

Grade	MW	PDI	Info
HDPE 1	E	F	MWD is known.
HDPE 2	E	G	MWD is known.



# **ESR 11 EXPERIMENTS PLANNING - TECHNIQUES**

- Characterization of material MFI and Melt density at different temperatures
- Extensional viscometry at different temperatures and strain rates to examine the rheology at different stages through processing (before FLH)
- Film blowing trials at different processing parameters to draw processing windows for different material systems
- Mechanical testing at both static and dynamic loadings, tensile tests, puncture resistance, dart drop test, Elmendorf test, sealability tests, and other tests?
- In- and off-process SAXS and WAXS studies and SEM characterizations of morphology
- Rheotens Viscometry
- Color, Haze, and gloss measurements
- Surface roughness characterizations and AFM
- Other tests?





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#### Thanks for your attention.

#### Questions?

This project has received funding from the European Union's Horizon 2020 research and innovation program under the Marie Sklodowska-Curie grant agreement No. 859885.



