Highly Effective Propane Dehydrogenation Using Ga-Rh Supported Catalytically Active Liquid Metal Solutions

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GENERAL

All reactions requiring protective atmosphere were carried out using standard Schlenck techniques. All reagents were commercial and used as received. The content of Rh and Ga, and their ratio, was determined by inductively coupled plasma – atom emission spectroscopy (ICP-AES) using a Ciros CCD (Spectro Analytical Instruments GmbH). The solid samples were digested with concentrated HCI:HNO₃:HF in a 3:1:1 ratio in volume, using microwave heating up to 220 °C for 40 min (<u>CAUTION</u>: HF solutions and vapors are extremely toxic, all manipulation has to be carried in a very efficient fume hood, wearing protective clothes, gloves, goggles). The instrument was calibrated for Rh (343.489 nm) and Ga (417.206 nm) with standard solutions of the relevant elements prior to the measurements.

MATERIALS SYNTHESIS

Preparation of (Et₃N)GaH₃

This compound was synthesized using the described procedure [1] using triethylammonium chloride (Sigma-Aldrich) instead of trimethylammonium chloride. The compound was not isolated and used as ethereal solution. The Ga content of this solution was determined as follow: 1 mL of ethereal solution was quenched in 10 mL of HCl (~2M) and the resulting mixture shortly boiled to evaporate the diethyl ether. The homogeneous solution was then diluted to 500 mL and the Ga content determined by ICP-AES. Given the low stability of gallane complexes, the obtained (Et₃N)GaH₃ solution was used immediately after its preparation.

Preparation of Ga decorated Al₂O₃

100 g of Al_2O_3 (Sigma-Aldrich; grade: Brockmann I, activated, standard; particle size: 0.05-0.15 mm; BET surface area: 155 m²/g; pH: 7.0 ± 0.5) were heated under vacuum (1 mbar) at 300 °C overnight in a Schlenck flask. After cooling, the Al_2O_3 was suspended in 200 mL dry diethyl ether, under argon. The required amount of an ethereal solution of Et₃NGaH₃ was added to this suspension in order to obtain the desired theoretical Ga loading (ca. 6-7 % w/w of Ga) with respect to the support. The ether was removed under vacuum at ca. -30 °C. After complete removal of diethyl ether, the flask was quickly (ca. 10 °C /min) heated up to 300 °C and held at this temperature until no gaseous products were observed any longer. Once the gallane decomposition terminated, the resulting grey solid was held at this temperature under vacuum (1 mbar) overnight and then cooled and stored under argon.

Preparation of Rh/Ga decorated material

Typically, 5 g of Ga decorated Al_2O_3 were suspended in 50 mL of distilled water under vigorous stirring. This suspension was heated at 50 °C and a stock solution of $RhCl_3 \cdot 3H_2O$ (with a nominal Rh concentration of 1 mg/ml) in distilled water was added. Given the Ga load (%w/w) of the material, the added amount of stock solution was adjusted to obtain the desired final Ga/Rh ratio, accounting for the loss of Ga due to the redox reaction between the latter and the Rh³⁺ cation (see Supplementary Figure 1). The resulting suspension was held under stirring for 15 min. Then, the solution was filtered and the material was thoroughly washed with distilled water (500 ml). The resulting solid was dried in an oven at 130 °C, overnight. The obtained materials, their Ga and Rh loading, as well as the respective Ga/Rh ratio are listed in Supplementary Table 1.

$$Rh^{3+} + Ga^{0} \longrightarrow Rh^{0} + Ga^{3+}$$

$$Ga/Rh = \frac{[(m_{Ga}/69.723) - (m_{Rh}/101.9055)]}{(m_{Rh}/101.9055)}$$

Figure S1: Galvanic displacement for the adjustment of the Rh-content in the SCALMS catalyst. The final Ga/Rh ratio is obtained by the mass of Ga on the support (m_{Ga}) and the mass of added Rh (m_{Rh}), once accounted for the galvanic displacement reaction.

catalyst	Ga % _{w/w}	Rh % _{w/w}	Ga/Rh	
Rh	0	0.19	0	
GaRh25	5.65	0.33	25	
GaRh34	5.90	0.26	34	
GaRh82	5.90	0.11	82	
GaRh89	6.06	0.10	89	
GaRh125	5.94	0.07	125	
Ga	6.40	0	-	
All the values were determined with ICP-AES (see above) and are accurate within an error of $\pm 3\%$				

Table S1. Compositions of the different catalysts used in this study

Preparation of Rh/Al₂O₃ catalyst

A 100 mL flask was charged with 5.01 of Al_2O_3 and ca. 20 mL of distilled water. 12.5 mL of a solution $Rh(NO_3)_3$ (with a nominal Rh concentration of 1 mg/L) were added. The water was evaporated under vacuum (1 mbar) at 50 °C. The resulting off-white powder was calcined for 12 h at 450 °C. The obtained off-white material was transferred to the reduction reactor and reduced with a stream of pure H₂ (60 mL/min), at 300 °C for 3 h. The resulting grey powder was analyzed by means of ICP-AES, giving a Rh content of $0.19\%_{w/w}$.

PVD preparation of bimetallic model samples on TEM grids

Rh (wire, 1 mm diameter, MatecK, 99.9 %) and Ga (in a pyrolytic boron nitride crucible, Alfa Aesar, 99.99999 %) were evaporated using a Focus EFM 3T evaporator. A quartz crystal microbalance was used to assure constant deposition rates. The base pressure of the used UHV system lies within the lower 10⁻¹⁰ mbar range. During deposition pressures in the low (Rh) and high (Ga) 10⁻⁹ mbar range are observed.

SEM IMAGING

Scanning Electron Microscopy (SEM) analysis was carried out with a Zeiss Evo 40 instrument using voltages between 15 and 25 kV and beam currents between 50 and 2000 pA. The EDX intensity maps shown as superposition in Supplementary Figure 2d) show the AlOx particle imaged in Supplementary Figure 2a) at similar magnification. The particles were deposited directly on a conductive sticky carbon pad (Plano GmbH).



Figure S2: a-c) SEM imaging of the Ga₁₂₅Rh SCALMS and d) EDX intensity maps of 2a.



Figure S3: SEM imaging of the Ga₂₅Rh SCALMS before (a and c) and after (b and d) the catalytic reaction

CATALYTIC REACTION SET-UP

The catalysts were used as prepared according to the above procedure. They were not reduced prior to catalytic testing. The catalytic tests were carried out in a continuous flow laboratory rig at atmospheric pressure. The flowsheet of the rig is depicted in Figure S4. A defined catalyst mass of 1.2 g was placed into the fixed-bed reactor. The reactor was heated to the set point at 10°C/min and after a stabilization time of 15 min , the reaction was started by supplying 8.9 mL_N min⁻¹ propane (Linde, purity 2.5) as feed gas diluted with 89 mL_N min⁻¹ helium (Linde, purity 4.6), respectively. This resulted in a gas hourly space velocity (GHSV) of 4900 ml_{gas} ml_{Cat. bed}⁻¹ h⁻¹ and in a residence time τ of 0.7 s (at standard conditions). The gases were dosed by mass flow controllers (MFC, Bronckhorst). All reactor tubes and pipes were held at 100 °C by using heating tapes and fiberglass tape insolation. The Quartz fixed-bed reactor was heated by a tubular split furnace. All other parts which were in contact with the reactants were made of stainless steel 1.4571.



Figure S4: Flowsheet of the continuous-flow experimental laboratory rig applied within this work for the dehydrogenation of propane.

ANALYTIC TECHNIQUES

The product stream was analyzed by online GC using a Bruker 456 GC equipped with a GC-Gaspro column (30 m x 0.320 mm) and a flame ionization detector (FID). Mole fractions x are calculated from peak areas and calibration factors determined for every substance. The conversion of propane ($X_{propane}$), Productivity and the selectivity to propene ($S_{Propylene}$) are calculated as follows:

$$X_{n-propane} = \frac{x_{propane,0} - x_{propane}}{x_{propane,0}} \cdot 100\%$$

$$Productivity = \frac{\dot{g}_{propane,0} \cdot S_{propylene} \cdot X_{propane}}{(2)}$$

$$g_{Rh}$$

$$S_{propylene} = \frac{x_{propylene}}{x_{propylene} + x_{methane} + x_{ethane} + x_{ethene}} \cdot 100\%$$
(3)

The productivities values were calculated accounting for the mass of Rh in the catalytic reactor.

CATALYTIC TESTS

Blind activity test with empty bed



Figure S5: Selectivity and conversion of different of the empty quartz reactor in propane dehydrogenation at 550 °C and 1.2 bar. He flow 89 mL_N min⁻¹, C₃H₈ flow 8.9 mL_N min⁻¹, GHSV 4900 h⁻¹.

Dehydrogenation of helium diluted propane feed with RhGa- SCALMS at 450°C



Figure S6: Conversion (left) and Rh based productivity (right) of different Ga/Rh-SCALMS in propane dehydrogenation at 450 °C and 1.2 bar. Molar ratios of Ga:Rh are 0 (open circles), 25 (downward-pointing triangles), 89 (upward-pointing triangles) and 125 (diamonds). Reaction conditions: 1.2 g catalyst (Rh/Al₂O₃: 0.19 wt.% Rh; Rh₁-Ga₂₅: 0.33 %Rh, 5.65 %Ga; Rh₁-Ga₈₉: 0.10 %Rh, 6.06 %Ga; Rh₁-Ga₁₂₅: 0.07 % Rh, 5.94 % Ga), He flow 89 mL_N min⁻¹, C₃H₈ flow 8.9 mL_N min⁻¹, GHSV 4900 h⁻¹.



Dehydrogenation of helium diluted propane feed with RhGa- SCALMS at 480°C

productivity (right) of different Ga/Rh-SCALMS in propane dehydrogenation at 480 °C and 1.2 bar. Molar ratios of Ga:Rh are 0 (open circles), 34 (downward-pointing triangles) and 125 (diamonds). Reaction conditions: 1.2 g catalyst (Rh/Al₂O₃: 0.19 wt.% Rh; Rh₁-Ga₃₄: 0.33 %Rh, 5.65 %Ga; Rh₁-Ga₁₂₅: 0.07 % Rh, 5.94 % Ga), He flow 89 mL_N min⁻¹, C₃H₈ flow 8.9 mL_N min⁻¹, GHSV 4900 h⁻¹.

Dehydrogenation of helium diluted propane feed with RhGa- SCALMS at 500°C



productivity (right) of different Ga/Rh-SCALMS in propane dehydrogenation at 500 °C and 1.2 bar. Molar ratios of Ga:Rh are 0 (open circles), 25 (downward-pointing triangles), 88 (upward-pointing triangles) and 125 (diamonds). Reaction conditions: 1.2 g catalyst (Rh/Al₂O₃: 0.19 wt.% Rh; Rh₁-Ga₂₅: 0.33 %Rh, 5.65 %Ga; Rh₁-Ga₈₉: 0.10 %Rh, 6.06 %Ga; Rh₁-Ga₁₂₅: 0.07 % Rh, 5.94 % Ga), He flow 89 mL_N min⁻¹, C₃H₈ flow 8.9 mL_N min⁻¹, GHSV 4900 h⁻¹.

<u>Propene selectivity of RhGa- SCALMS catalysts at various temperatures during</u> <u>propane dehydrogenation</u>

With the exception of pure Rh/Al₂O₃ catalyst, all catalysts showed nearly constant selectivity for propene over the entire duration of experiment. The observed selectivity values for the all catalysts across the temperature range is summarized in the table S2 below.

<i>Temperature / °C</i>	Ga:Rh ratio / -	Selectivity, S _{propene} / %
450°C	Ga/Rh : 25	92 ± 2
	Ga/Rh : 89	91 ± 4
	Ga/Rh : 125	95 ± 2
	Rh/Alox : 0	79 ± 12
480°C	Ga/Rh : 34	91 ± 5
	Ga/Rh : 125	93 ± 3
	Rh/Alox	88 ± 4
500°C	Ga/Rh : 25	89 ± 4
	Ga/Rh : 89	92 ± 3
	Ga/Rh : 125	90 ± 6
	Rh/Alox	81 ± 6
550°C	Ga/Rh : 34	88 ± 5
	Ga/Rh : 82	89 ± 4
	Ga/Rh : 125	87 ± 7
	Rh/Alox	71 ± 20

Table S2: Selectivities of RhGa- SCALMS catalysts at various temperatures during propane dehydrogenation over 15 h TOS

Dehydrogenation of propane by Ga/Al₂O₃ catalyst – Base line tests



Selectivity(right) of Ga-Al₂O₃ in propane dehydrogenation at 450 °C (open square), 480°C (bottom

half-filled square) 500°C (top half-filled square) and 550°C (filled square) at 1.2 bar. Reaction conditions: 1.2 g catalyst (Ga/Al₂O₃: 6.4 wt.% Ga), He flow 89 mL_N min⁻¹, C₃H₈ flow 8.9 mL_N min⁻¹, GHSV 4900 h⁻¹.

RAMAN SPECTROSCOPY

Raman spectroscopy of SCALMS after catalytic application was conducted using an AvaRaman-PRB-532 (Avantes) probe and an AvaRaman-532HERO-EVO (Avantes) system. The system consists of a 532 nm (green) solid state laser (Cobolt) and an AvaSpec-HERO (Avantes) spectrometer with a grating set of 1200 lines mm^{-1} (HSC1200-0.75). The spectrometer was equipped with a 50 μ m slit and the detected wavelength range was 534-696 nm. The spectra were collected in 20 repetitions at 15 mW laser power with an exposure time of 5 s.



Figure S10: Raman spectra of spent SCALMS after propane dehydrogenation at 550 °C, as well as the spectra of a spent Rh/Al₂O₃ catalyst after dehydrogenation at 450 °C.

Table S3: Characteristic values of the D and G band in the Raman spectra of spent Ga-Rh SCALMSafter propane dehydrogenation at 550 °C and a Rh/Al2O3 reference sample after dehydrogenation at 450 °C.

catalyst	PDH temperature	I_G/I_D	/I _D D band / cm ⁻¹		G band / cm ⁻¹	
			FWHM	Position	FWHM	Position
Ga/Rh = 125	550	1.188	203.5	1338	67.2	1601
Ga/Rh = 82	550	1.146	214.6	1340	72.3	1599
Ga/Rh = 34	550	1.148	203.8	1338	68.7	1599
Ga/Rh = 0	450	1.346	136.5	1337	46.1	1607

XPS MEASUREMENT AND ANALYSIS

Different catalyst samples of alumina-supported Ga/Rh catalysts with a Ga loading of 6.0 wt.% and Ga:Rh ratios of 16:1, 25:1, 58:1, 88:1 and 125:1 were examined using X-ray photoelectron spectroscopy (XPS). In addition, bimetallic Ga-Rh model systems with Ga:Rh ratios of 49:1, 82:1 and 166:1 (2.0, 1.2 and 0.6 at.% Rh) were studied. All spectra were collected in ultra-high vacuum using a non-monochromatized Al K_a x-ray source, at normal electron emission. A detailed description of the XPS setup can be found elsewhere[2].

The preparation of all catalyst samples for the XPS measurements was done at room temperature and in air. The powder samples were attached to the W foil using a H₂O-based Ag/SiO₂ dispersion (plano-em) as conductive glue. For each catalyst batch, two samples were examined at room temperature, one as-synthesized before the reaction and one after the reaction (marked with an asterisk). All spectra were collected after introduction to UHV without further treatment. Since the samples showed some charging (up to 7 eV), the binding energy scales are referenced to the binding energy of the Al 2p level at 74.6 eV; this value was reported for Al₂O₃ in literature[3]. We observe signals shifted to lower binding energy in Ga 2p (- 2 eV), Ga 3d (- 2 eV) and Rh 3d signals (-2.1, and 2.5 eV respectively). These generally appear more pronounced in spectra collected after catalytic testing indicating the formation of metallic Ga and Rh species under reaction condition. Based on the observed shifts we assign the observed signals to Ga/Ga₂O₃ and Rh/RhO_x[4,5,6]

The spectra of the bimetallic Ga-Rh model system were collected with the same setup and excitation energy. These samples were prepared at room temperature and in air by combining macroscopic amounts of Ga (99.99999 %; Merck, former Sigma-Aldrich) and corresponding amounts of Rh (99.9 %, Goodfellow) in a W crucible (Lesker) attached to the sample stage of the XPS system. Temperature control of the W crucibles was achieved using resistive heating in combination with a K-type thermocouple spot-welded to the base of the crucible. The *in vacuo*-cleaning and preparation of the model surfaces included heating to temperatures as high as 580°C to facilitate homogeneous alloy formation and to decompose the passivating Ga oxide film formed in air; carbonaceous impurities were removed by sputtering with 1 keV Ar⁺. The binding energy scale for these samples is referenced to the Fermi-energy using a detailed region scan of the valence region of Rh (111). To account for fields introduced by resistive heating,

the binding energy of the Ga 3d core level binding energy is fixed to 18.8 eV, the value observed without heating. The quantification of the XPS signals of the bimetallic model systems is conducted by referencing to a Rh (111) single crystal and pure Ga. No temperature-, or composition-dependent shifts are observed in the Rh 3d core level signals. Spectra are shown in Supplementary Figure S11.







Figure S12: Survey XP spectra of AlOx-supported SCALMS samples. Asterics indicate spent catalysts.



Figure S13: Ga $2p_{3/2}$, O 1s and C 1s spectra collected from the Ga₈₂Rh alloy droplet. The data was scaled to normalized Ga 3d intensity for display.

TEM Analysis

(Scanning) transmission electron microscopy (method)

The model samples compatible for TEM studies were prepared as described above. After deposition the samples are transferred via ambient condition and inserted into the TEM. Typically, a 3-5 nm thick oxide layer is present at the surface of the nanoparticles. Storage in ambient condition for up to a week does not seem to result in an increase of the oxide layer thickness.

(Scanning) transmission electron microscopy (S/TEM) studies were performed on a Titan³ Themis microscope operating at either 200 kV or 300 kV. The TEM is equipped with C_s-correctors both at the illumination and imaging side, along with a Super-X energy dispersive X-ray (EDX) detector and a GIF Quantum ERS (spectrometer). The Super-X detector comprises four silicon drift detectors (SDD) symmetrically placed around the optical axis, close to the sample area, with a detection solid angle of about 0.9 sr. All four signals are combined into one spectrum to improve the collection efficiency in spectrum imaging (SI) acquisition. In the STEM imaging and SI experiments, the probe-forming semiangle was set to a value of 15.7 mrad. A probe current of 200-500 pA and dwell time 30-50 µs was used. High-angle annual dark-field (HAADF), ADF, annual bright-field (ABF) and BF STEM images were simultaneously acquired along with the EDX signals. For high-resolution TEM (HRTEM) imaging, the image corrector was set to negative C_s imaging (NCSI) condition [7], with the first pass band of the phase contrast transfer function (PCTF) reaching out to a resolution of 1Å. All electron diffraction data are elastic filtered, which were recorded by the GIF camera with energy select slit of 10 eV placed over the zero-loss (i.e., elastically scattered) electrons. Energy filtering removes most of the inelastically scattered electrons and thus greatly enhances the contrast of diffracted spots and rings, especially close to the central transmitted beam, e.g., the first broad diffraction ring of solid amorphous or liquid phase, which would be otherwise very difficult to locate, quantify and interpret.

Identification of the nanocrystal phase

The nano-crystallites phase is assigned based on both the chemical composition (from EDX maps) and diffraction patterns. The local Rh concentration evaluated from summed EDX signals of the Rh-rich crystallites in the big Ga particle amounts to 12-15 at. %. This measured value can be slightly underestimated due contributions from amorphous Ga overlapping in projection direction. Three of the known candidate phase [8, 9, 10], namely, Ga₁₆Rh₃ (15.9 Rh at. %), Ga₂₁Rh₄ (16 Rh at. %) and Ga₉Rh₂ (18.2 Rh at. %) fit into this range. Comparing the position and intensity of the diffraction lines of the three phases with the experimental ring pattern, the strong lines seem to all fit. Upon closer inspection, large amount of minor lines expected in the Ga₉Rh₂ phase cannot be identified, while both Ga₁₆Rh₃ and

Ga₂₁Rh₄ seem to match almost perfectly to the experimental pattern (Fig. S12, only Ga₁₆Rh₃ phase superimposed).

While Ga_9Rh_2 (space group *Pc*) take the form of the pristine E_9T_2 phase (E = Al or Ga, T = transition metal), with building blocks of [RhGa9] antiprism polyhedral, the $Ga_{16}Rh_3$ (or $Ga_{64}Rh_{12}$, space group *Ccca*) and $Ga_{21}Rh_4$ (or $Ga_{63}Rh_{12}$, space group *Cmca*) are closely related to the Ga_5Pd phase, with building blocks of [RhGa10] icosahedral cages sharing corners. The small difference of the Rh concentration in these two phases can be understood as result of stacking polymorphism. Indeed, stacking disorder is very frequently observed by HRTEM images in our samples.



Figure S14: Crystal phase analysis with electron diffraction. The experimental zero-loss filtered electron diffraction patterns of pure Ga particles (left half) and a sample with average Rh content of 2.5 at. %. The kinematic powder diffraction intensities (white lines) and calculated nano-crystalline diffraction intensities (assuming isotropic round particle with diameter of 20 nm) with Ga₁₆Rh₃ phase (ICSD No. 415871) are superimposed on the right half. Contrast of the patterns is inverted and brightness scaled for better visualization.





Figure S15: BF-TEM images of sample with (left) Rh 0.6 at. %, (middle) Rh 3 at. % and (right) Rh 6 at. %. The corresponding EDX spectra (measured with a beam illuminated area of 8 μ m) are show at the bottom of each image. With increasing Rh concentration, the shape of the particles become more irregular and the size of the particles increases (notice the larger scale bar in the right most image).

In situ heating and electron diffraction

In situ heating experiments were carried out using a Gatan Heating Holder (Model 652). With this holder, temperature is measured by a thermocouple integrated into the furnace. Independent temperature measurement and comparison to chip-based heating holder was carried out previously [11, 12]. In the experiments, temperature was raised manually by increasing the current send through the furnace at the tip, so that the sample was heated up slowly in a stepwise manner (steps of ~ 100°C). Each ramp took about 1 min., which should be long enough to reach a steady and homogeneous temperature at the sample region. The temperatures at each step was held at least 1 min. In particular, the temperature was hold for more than 10 min at about 400 °C for the sample with x = 36, and at about 300 °C, 500 °C and 580 °C for the sample with x = 105. The temperature was logged manually against the image frame numbers with an uncertainty of a couple of seconds. A short (up to 10 s) and small (typically 10 °C, max 40 °C) overshooting of temperature at the end of each ramp step can happen. We estimate the uncertainty of temperature at the end of each ramp step can happen. We estimate the uncertainty of temperature for the given frames as shown in Fig. 1 (main manuscript) to be ±10°C.

To inspect the melting of the nanocrystallites, *low dose* zero-loss filtered selected area electron diffraction (SAED) was carried out in the range from RT to 540 °C. A 1.25 nA electron beam was spread over a large sample area of about 8 μ m in diameter. Under this condition, the beam dose rate is about 1.5 e⁻/Å²·s. Due to the huge number of diffracting nanocrystallites, and zero-loss energy filtering,

diffraction patterns with very high contrast can be recorded at 10 fps. BF-TEM images taken before and after the *in situ* experiment, show unaltered particle morphologies in regions illuminated by electrons during low-dose *in situ* electron diffraction at elevated temperatures (Fig. S14). Therefore, potential beam induced effects during the *in situ* diffraction study of the melting behavior can be safely neglected.

In contrast, we have observed highly reproducible electron beam induced effects during *in situ* TEM imaging experiments, which require a much higher electron dose. Ga was "repelled" from the electron beam illuminated area at a beam dose rate of $50 - 5000 \text{ e}^{-/}\text{Å}^2$ ·s and typical total experimental time of 10 – 20 min. This phenomenon was found to be *dose dependent* and *independent* of the supporting substrate (SiO₂ or SiN) and is very likely related to carbon contamination during imaging in the vacuum of the TEM column (in the range of 10^{-7} mbar), which may have altered the phase equilibrium and diffusion behavior of the atoms.

According to the equation of dose-limited resolution [8]:

$$\delta = (SNR)(DQE)^{-\frac{1}{2}}C^{-1}(FD/e)^{-1/2},$$

and typical parameters in (diffraction contrast) BF-TEM observations [8], a resolution of 5 nm requires a minimum dose of ~ 10 e⁻/Å². Considering *in situ* observation, at typically 3 – 10 fps, a dose rate of 50 e⁻/Å²·s is the minimum requirement to observe the melting of Ga-Rh nano-particles in real space. Since under these conditions electron beam induced effects cannot be neglected the melting behavior of the precipitates have been studied by *low-dose* electron diffraction (see above).



Figure S16: BF-TEM overview images of the sample before and after in situ heating and low dose SAED studies. Electron beam induced effects are not observable.

Super-saturated Rh-Ga amorphous solid phase and the oxide shell

Super-saturated Rh-Ga amorphous phase was observed when heating the sample with x = 105 (Rh = 0.9 at. %) up to ~320 °C until the sharp crystal rings completely fade out, and then slowly cool down to room temperature. Figure S17 shows the STEM-EDX and electron diffraction results. The lack of sharp diffraction rings like that in Fig. 5 and Fig. S1 and existence of the 3 broad diffuse rings suggest the particles take amorphous solid phase. Formation of the super-saturated Rh-Ga amorphous solid phase is likely related to the existence of the oxide shell. Figure S18 shows the STEM-EDX and electron diffraction results of the same sample, measured at RT after it has been heated to 580 °C. The oxide shell is no more observable, and the typical two-phase microstructure recovered.



Figure S17: (left) STEM-EDXS maps: Gray (simultaneously acquired STEM Z-contrast image), yellow (Rh), red (oxygen) and blue (Ga). The oxides shell can be seen clearly in the oxygen map. Electron diffraction measured at RT (middle) show amorphous ring pattern.



Figure S18: (*left*) *STEM-EDXS maps: Gray (simultaneously acquired STEM Z-contrast image), yellow (Rh), red (oxygen) and blue (Ga). The oxides shell was removed after the sample has been heating to 580 °C. Electron diffraction measured at RT (middle) show sharp crystal rings.*

The broad diffraction rings

The diffraction patterns from the sample with x = 105 at RT and $540 \pm 10^{\circ}$ C, and the azimuth averaged profile is show in Fig. S17. The profile is fitted by five Gaussian peaks. While the two broad background peaks are due to the amorphous SiO₂ membrane, the superimposed three peaks at about q = 2.6 nm⁻¹, 4.2nm⁻¹ and 5.1 nm⁻¹ are attributed to disordered Ga-Rh phase. At $540 \pm 10^{\circ}$ C, the second and third peaks are reduced dramatically.



Figure S19: Diffraction pattern and the azimuth integrated intensity profile with Gaussian peak fitting superimposed from solid amorphous Ga-Rh phase (top) and liquid Ga-Rh phase.

In addition to the sharp diffraction rings from crystallites, at least two broad diffraction rings can be seen throughout the series at positions $q = 2.6 \text{ nm}^{-1}$ and 4.2 nm^{-1} , with the second marked by the white arrows in the patterns. They are very close to expected positions of disordered (i.e., amorphous solid and/or liquid) Ga phases [13]. Due to the structural similarity of amorphous solid phase and liquid phase of Ga, and expectedly also for the Rh-poor Ga-Rh system, it is not immediately obvious to discriminate the two possible phases from the diffracted intensities. Nevertheless, the intensity ratio between the second and first broad ring, which is related to the different structure factor of amorphous solid and liquid phase [14], could serve as a qualitative indication of liquid or solid phase. In case of the sample with x = 36, this ratio did not change at all upon ramping the temperature from 480 to 530°C (the highest temperature tested for this sample) and changed by only less than 10% when compared to RT results. We deduce, therefore, that a fully liquid phase is present in samples with x < 36 above 530 °C. In the case of the sample with x = 105, this ratio at temperatures above ~ 350 °C shows a dramatic reduction of more than 50 % compared to the ratio at RT (cf. ESI Video 2), supporting that the particles with x = 105 are in full liquid state at the catalysts working temperatures. In the diffracted intensities normalized to the first diffraction ring (Fig. 5e) the intensity of the second ring decreased significantly and broadened at temperatures of 420±10°C and 540±10°C. The existence of this intermediate Ga-Rh amorphous solid phase might be a size effect. From these observations, we conclude that at the working temperature conditions, only the low Rh concentration samples are in a fully liquid phase, which is consistent to the conclusion obtained from XPS and simulations.

Video S1. Electron diffraction series of sample with x = 36, temperature 400 - 530°C, 20x accelerated. Video S2. Electron diffraction series of sample with x = 105, temperature 550 - RT °C, 20x accelerated.

COMPUTATIONAL METHODS

All density-functional theory calculations were performed using the "Vienna Ab Initio Simulation package" (VASP) employing the projector augmented wave (PAW) method to represent the atomic cores and a plane wave basis set [15, 16, 17]. Exchange-correlation effects were treated within the GGA approach applying the functional of Perdew, Burke and Ernzerhof (PBE) [18]. Dispersion interactions were incorporated in the investigation of adsorption processes by the D3 correction of Grimme et. al. [19].

Ab initio DFT-based molecular dynamics (AIMD) simulations were conducted to study the behavior of the liquid Ga/Rh. The liquid-vacuum interface was represented by a periodic slab model with a tetragonal unit cell (12.69x12.69x36.15 Å) consisting of 162 Ga and 18 Rh atoms and a vacuum layer of ~12 Å in z-direction (perpendicular to the surface) to decouple periodic images. In calculations without any adsorbates an energy cutoff for the plane wave basis set of 350 eV was used. The equations of motion were integrated with a Verlet algorithm in time steps of 10 fs, which was previously shown to be sufficient for a system containing Ga and a heavier metal component (Pd, Rh) [20, 21]. After equilibration for at least 10 ps, a Nosé-Hoover thermostat [22] was employed to simulate a canonical ensemble at 450 °C. A Fermi-smearing was used with a smearing parameter corresponding to the temperature conditions [23]. The first Brillouin zone was sampled by a Γ -containing 2x2x1 k-point mesh. To obtain good energy conservation during the AIMD simulation, the SCF convergence criterion was set to 10^{-7} eV. 15 trajectories were sampled with an overall simulation time of 5.88 ns. Each trajectory was running for at least 240 ps, the longest trajectory for 638 ps. These AIMD simulations showed that the time evolution of the mean square displacement (MSD) function of the Ga and Rh atoms from their initial position exhibits a linear behavior for both species indicating the catalyst to be in a liquid state in the simulations (see ESI, Fig. S18). Similar to the previously studied GaPd system [21], a layered catalyst surface structure in combination with a Rh surface

Supporting Information

depletion can be observed from the corresponding density profile along the direction perpendicular to the surface (the z-direction) which represents the probability of finding a Ga or Rh atom in intervals of 0.1 Å in that direction (depicted in ESI, Fig. S19). Our calculations reveal that less than 0.02 % of the alloy surface atoms are Rh atoms if the first maximum of the Ga-density is used to define the first layer (or 0.7 % if the first minimum of the Ga density is used). Therefore, it can be assumed that isolated Rh atoms appearing dynamically at the surface are responsible for the catalytic reaction with the approaching reactants.

The adsorption of CO was investigated using the same tetragonal cell, however containing 178 Ga atoms and 2 Rh atoms, one on each surface of the slab with one or two adsorbed CO molecules on-top of the Rh atoms. For this system, the time step in the MD was decreased to 2 fs. Additionally, the plane wave cutoff energy was set to 450 eV. We obtained vibrational spectra by computation of the Fourier transform of the velocity-velocity autocorrelation function using the trajectory analyzer code TRAVIS [24, 25]. For Rh(CO)₂ five trajectories were sampled, each trajectory for 20 ps, starting from different initial geometries. The obtained power spectra were then averaged. For the RhCO species the power spectrum is computed from a trajectory running for 38 ps.

To test if adsorption of species which are involved in the catalytic process can retain the catalytically active center at the surface, we placed different adsorbates at the Rh atom, namely propylene, a propyl residue and an additional hydrogen atom or two hydrogen atoms, at the beginning of our simulation. The time evolution of the z-position (Fig. S20) shows that as long as the adsorbate is bound to the Rh atom, the latter is kept at the surface until the adsorbate desorbes. After desorption, the Rh atoms directly diffuse away from the surface. In these simulations the timestep was reduced to 1 fs and the mass of the hydrogen atoms was set to the deuterium mass.

The coverage dependence of the CO stretch frequency on top-Rh was assessed by computing the vibrational frequencies of CO on a Rh(111) surface using varying super cell sizes, namely 2x2 (3/4 and 1/4 ML with 3 and 1 CO molecules, respectively), 3x3 (1/9 ML) and 4x4 (1/16 ML) in harmonic approximation using a finite differences approach with a displacement of 0.01 Å in all spatial directions. The Rh(111) surface was modeled by a 6 layer Rh slab with the three bottom layers fixed to the calculated bulk geometry (with a lattice constant of 3.79 Å), while the three surface layers were free to relax with an additional vacuum layer of 12 Å in direction perpendicular to the surface. CO was adsorbed in top position for all coverages, however for 3/4 ML the experimentally observed structure with one CO in top and two CO in threefold hollow positions was considered [26]. To obtain well converged forces the plane wave cutoff was set to 480 eV and a SCF converge criterium of 10⁻⁸ eV was chosen. The geometries were relaxed until the forces on all atoms became smaller than 0.01 eV/Å. A Methfessel-

Paxton smearing of first order with a smearing parameter of $\sigma = 0.2$ eV was applied [27] with a 19x19x1 k-point mesh for the 1x1 cell and corresponding sizes for larger cells.

To investigate the dehydrogenation of propane, a solid model system was created, that consists of a fcc-Ga(IV) slab with an isolated Rh-adatom in a surface hollow position to mimic the situation in the liquid catalyst system (see Fig. S21). The Ga(IV) bulk structure is a high pressure fcc-Ga phase with a computed lattice constant of a=4.18 Å. The bulk and the corresponding (100)-surface (as 3x3x3 supercell) were relaxed with Γ -including 25x25x25 and 8x8x1 k-point meshes, respectively. For the 6-layer surface slab (with 14 Å vacuum), again the 3 bottom layers were kept fixed at the bulk geometry and structures were relaxed until the forces on all atoms became smaller than 0.001 eV/Å. The SCF convergence criterion was set to 10⁻⁶ eV. Again, a Methfessel-Paxton smearing of first order with a smearing parameter of $\sigma = 0.2$ eV was chosen. For geometry optimizations with adsorbates the forces were converged to less than 0.005 eV/Å. Different sites for the additional Rh atom were tested, yielding that the most favorable position after geometry optimization is a slightly distorted hollow position in the first surface layer.

Transition states were determined using the climbing-image nudged elastic band method (cNEB) as implemented in VASP according to Henkelman et al. [28] with a force convergence criterion of 0.025 eV/Å. All other settings in the cNEB calculations are equal to the geometry optimizations of initial and final states. The highest energy image of the cNEB calculation was used as initial guess for a dimer search to further converge the transition states until the forces were lower than 0.01 eV/Å. [29] Local minima and transition states were verified by vibrational analysis. Helmholtz free energy corrections were calculated in the simple harmonic limit using the thermochemistry module of the Atomic Simulation Environment (ASE) [30]. Here, the real vibrational frequencies of the adsorbate and the surrounding surface atoms were used to calculate the correction. Comparing the uncorrected DFT energies (see Fig. 4c) with the Helmholtz free energies, it is obvious that the reaction profile is only slightly changed. The overall reaction barrier remains almost the same.



Figure S20: Calculated mean square displacement (MSD) of Ga and Rh atoms from their initial positions in liquid GaRh. The shown MSD is calculated as an average of all 15 calculated trajectories.



Figure S21: Simulated density profile for Ga and Rh perpendicular to a liquid GaRh (ratio 9) slab at 450 °C (a.u., arbitrary units). The probability of finding Ga or Rh atoms in intervals of 0.1 Å along the z-direction is plotted. The Rh-density (ρ_{Rh}) is scaled such that values are comparable to the Ga density (ρ_{Ga}). Due to the smaller number of heavy Rh atoms, the Rh-density is not perfectly converged.



Figure S22: z-position of Rh atoms with different adsorbates as function of time. a, Propylene. b, Propyl residue and one hydrogen atom. c, Two hydrogen atoms. For each adsorbate two trajectories were sampled, thus there are two lines at the bottom and two at the top surface. Dashed vertical lines indicate the desorption (a) or the reaction of H and propyl to propane or of the two H atoms to H₂ with subsequent desorption (b and c) for each trajectory in the corresponding color. The Ga-density is given as orientation. Horizontal dashed lines indicate the first maximum of the Ga density. In all cases the Rh atoms are kept at the surface by the adsorbate and move into the slab after the adsorbate has desorbed.



Figure S23: Top view on the solid model catalyst system; a fcc-Ga slab with one Rh adatom adsorbed in a slightly distorted fourfold hollow position. Ga atoms are depicted in blue, Rh atoms in light red. The black line indicates the surface unit cell.



Reaction coordinate

Figure S24: Free energy diagram for the dehydrogenation of propane. Ga is depicted in blue, Rh in light red, C in black and H in white. Reaction intermediates are indicated by blue lines and transition states by red lines.

We estimated the uncertainty of the properties determined by the AIMD simulations by comparing the values we obtain from single trajectories with the one obtained as average over all trajectories.

1. Vibrational spectra: Five trajectories were sampled for the $Rh(CO)_2$ vibrational spectrum, each simulated from different initial configurations. The average value of the CO vibrational frequency over all five trajectories is calculated to be 2002 and 1978 cm⁻¹ for the symmetric and asymmetric CO stretching frequencies, respectively. From single trajectories we obtain for the peak maximum of the symmetric CO frequency values in the range of 2012-1998 cm⁻¹ and for the asymmetric CO stretching value from 1982-1975 cm⁻¹. Adding or removing single trajectories from the average has only minor impact on the average value.

2. MSD: To quantify the uncertainty of the MSD values we evaluated diffusion coefficients from the slope of the x-and y-component of the MSD for Ga in the 15 different trajectories. The average value for the Ga diffusion coefficient calculated from all trajectories is $3.81*10^{-5}$ cm² s⁻¹. The largest deviations from this value for single trajectories are

3.29 *10⁻⁵ cm² s⁻¹ and 4.67*10⁻⁵ cm² s⁻¹. Again, adding or removing single trajectories from the average results only in minor deviations.

3. Z-positions of Rh atoms in the slab (see Figure 4a and Figure S20): For each adsorbate that was tested two trajectories starting from different initial configurations were sampled to test the reliability of the results. In all cases the two trajectories give qualitatively the same results as described in the main text.

Charge analysis was performed on the all-electron charge density using the Bader program as implemented in the VASP Code [31, 32].

INFRARED SPECTROSCOPY

Reactor setup for infrared measurements

Diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) was performed using a homebuilt reactor system in combination with a Bruker Vertex 80v FTIR spectrometer. Figure S24 shows a section of the layout. The reactor chamber and Praying Mantis diffuse reflectance accessory (Harrick) are situated in the sample compartment of the spectrometer, which is evacuated during the measurements. By evacuating the complete optical path, we ensure high stability during long-term experiments. The reactor is equipped with CaF_2 windows and a type K thermocouple in contact with the sample, which leads to excellent temperature control. CO (Linde, 4.7) and Ar (Linde 5.0) were dosed using mass flow controllers (MFCs, Bronkhorst), the pressure in the system is adjusted using three pressure controllers (PCs, Bronkhorst). The automatized operation of the system enables accurate and reproducible changes of temperature, pressure and gas composition in the system.

Prior to the pulse experiment, the sample was reduced at 450°C in 1 bar CO. To study the surface properties of GaRh supported on Al_2O_3 , we exposed the samples to pulses of CO at 100, 200, 300, 400 and 450 °C. A sequence of five CO pulses was performed at each temperature in the following way: After 5 min CO dosing (15% in Ar) at 1 bar the CO gas phase was removed to resolve features that are otherwise hidden underneath the broad rotational-vibrational structure of CO. This was achieved by evacuation (< 10 mbar, 1 min) and subsequent Ar dosing (4 min) at 1 bar. The sample was heated in 1 bar Ar to 450 °C to remove all residual CO adsorbates, before continuing with the next pulse sequence at a different temperature.



Figure S25: Schematic depiction of the reactor layout

All spectra were recorded with 20 s acquisition time. The background spectrum was recorded at 450 °C under Ar with an acquisition time of 2 min. The spectra shown are normalized to compensate for changes in reflectivity upon heating and/or cooling and plotted as difference spectra $n_{diff} = n_{seq} - n_{clean}$ with n_{clean} being a spectrum recorded at the respective temperature in Ar, n_{seq} being the spectrum after CO exposure, and n_{diff} being the difference spectrum.

DRIFT experiments

All DRIFT spectra were acquired immediately after removal of the last CO pulse at the respective temperature. Note that the spectra are not recorded under steady-state conditions and the peak intensities change during Ar purging, especially at higher temperatures. In the following, we neglect the temporal evolution but aim at the qualitative characterization of the species that are present.

First, we focus on the monometallic samples that are presented in the main manuscript. The Rh/Al₂O₃ sample shows a pronounced double feature at 2093 cm⁻¹ and 2023 cm⁻¹. The peak intensities decreases with increasing temperatures, but the peak centers doe not shift. A smaller band, observed at 2065 cm⁻¹ at 100 °C, shifts to lower wavenumbers upon heating and disappears above 200 °C. In accordance with the literature, the two signals at 2093 and 2023 cm⁻¹ are assigned to the symmetric and asymmetric stretching frequency of Rh¹(CO)₂.[33,34,35] The smaller peak at 2065 cm⁻¹ is assigned to on-top Rh⁰CO species, which is reported to show lower thermal stability than the Rh¹(CO)₂ dicarbonyl.[36]

For the Ga/Al₂O₃ sample, two broad bands evolve at 2021 cm⁻¹ and ~1880 cm⁻¹ upon heating. The appearance of the bands and their temperature-dependence indicates the formation of Ga-H species. Ga-H peaks are typically observed above 250°C and increase in intensity upon heating as has been observed, for instance, on pure Ga and Ga-Pd catalysts.[37] Although no H₂ was dosed during the experiment, residual H₂O and OH groups on the support can lead to the formation of hydride species. The peak at 2021 cm⁻¹ is characteristic for hydrides on metallic Ga, whereas the band at ~1880 cm⁻¹ is tentatively assigned to oxidic Ga species. This shows that Ga may not have been completely reduced under the present conditions (heating in CO to 450 °C) in the case of the Ga/Al₂O₃ sample. In contrast, no peak is visible at ~1880 cm⁻¹ on samples which contain Rh and full reduction to metallic Ga is found. This further confirms our assumption that oxidic Ga species are completely reduced in the presence of Rh under reductive conditions (see also statements above).

In Figure S25, we show the CO stretching frequency region of $Ga_{25}Rh_1/Al_2O_3$ and $Ga_{125}Rh_1/Al_2O_3$ samples. For the $Ga_{25}/Rh_1/Al_2O_3$ SCALMS sample, the spectra show two pronounced peaks at 2099 and 2021 cm⁻¹ at 100 and 200 °C. These bands were previously assigned to Rh¹(CO)₂ (see above). A complex pattern of additional bands between 2100 and 2030 cm⁻¹ is present above 200 °C. Distinct peaks are visible at 2100, 2088, 2072, 2054 and 2031 cm⁻¹ in the spectra. The Rh-Ga phase diagram suggests that at these Ga/Rh ratios even heating to 450 °C may not be sufficient to cross the liquidus curve of the system[38]. In accordance with our microscopic and XPS data we assume that liquid Ga and solid Ga-Rh phases coexist under these conditions. This is in-line with the observation of several well-defined peaks in the spectra pointing to a heterogeneous system with a variety of CO adsorption sites. Due to the complex shape of the spectra, it is not possible to assign each band unequivocally. It is nevertheless clear that the peaks correspond to Rh on-top species. As they are not observed for the Rh/Al₂O₃ reference sample, we conclude that they are due to CO adsorbed on-top of Rh atoms in a Ga environment or at solid Rh-Ga intermetallic phases.

For the $Ga_{88}/Rh_1/Al_2O_3$ sample, an additional feature at 1974 cm⁻¹ was observed up to 300 °C that was not found in the other samples with lower Ga to Rh ratios. We assume that this band originates from a Rh carbonyl species formed at very low Rh loadings only. Frank et al. assigned bands at 1999 and 1954 cm⁻¹ to on-top CO adsorbates on very small Rh deposits on Al_2O_3 . Still, it is fair to say that their studies were conducted in ultra-high vacuum at low temperatures[39].



Figure S26: CO stretching region of the DRIFT spectra obtained from Ga_x - Rh_y/Al_2O_3 samples in Ar atmosphere after treatment with CO. The temperature in °C and the scaling factors are indicated on the left and right side of each panel, respectively.

For the Ga₁₂₅-Rh₁/Al₂O₃ sample, the Rh-Ga phase diagram [40] suggests that the system forms a homogeneous and fully liquid phase upon heating to 450 °C. The spectra depicted in Figure S25 show two features at 2095 and 2024 cm⁻¹ which originate from the Rh¹(CO)₂ dicarbonyl. At 200 °C and 300 °C, an additional band at 2057 cm⁻¹ is observed which matches the Rh⁰(CO) species. At 400 °C, a weak and broad feature is present at ~ 2027 cm⁻¹, whereas at 450°C the band is well-defined. In accordance with data obtained from the Ga₈₈Rh₁ and pure Ga sample we again assign the band at 2027 cm⁻¹ to hydrides on reduced Ga. The sample shows no clear feature below 2000 cm⁻¹. We assume that due to the low amount of Rh in the sample the intensity of carbonyl features in a liquid Ga matrix is below our detection limit or the peak is covered by the more intense Ga hydride peak at elevated temperatures.

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