

Pathways to national-scale adoption of enhanced geothermal power through experience-driven cost reductions: supplementary information

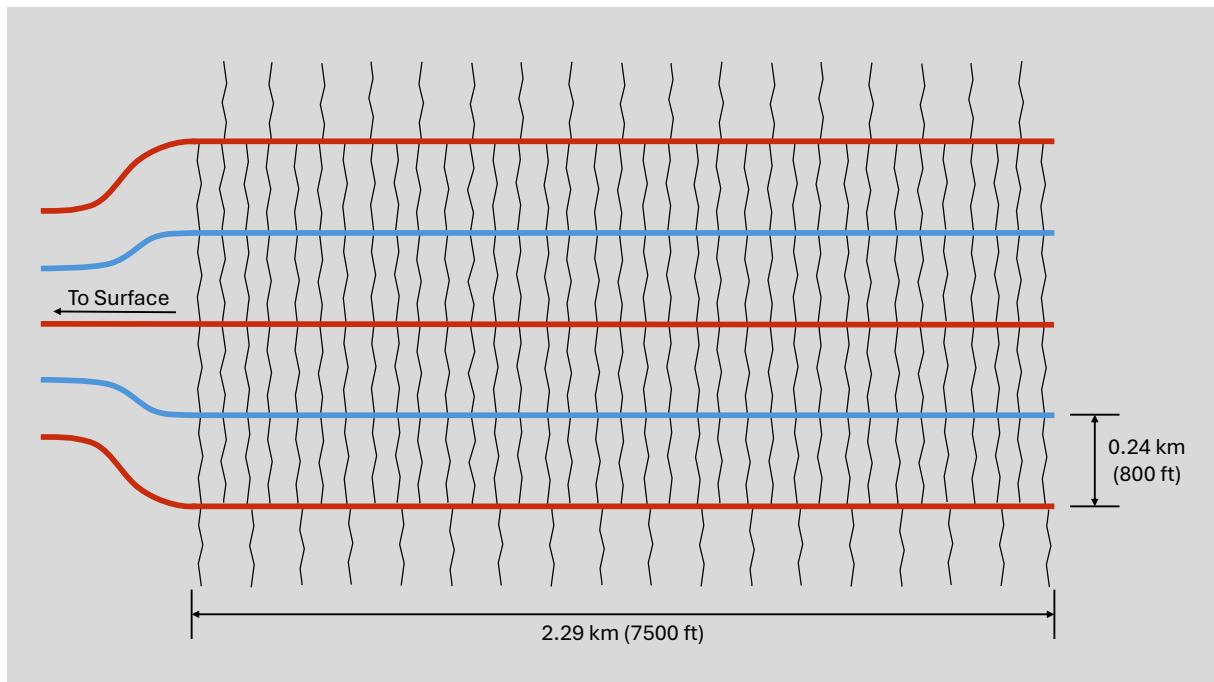
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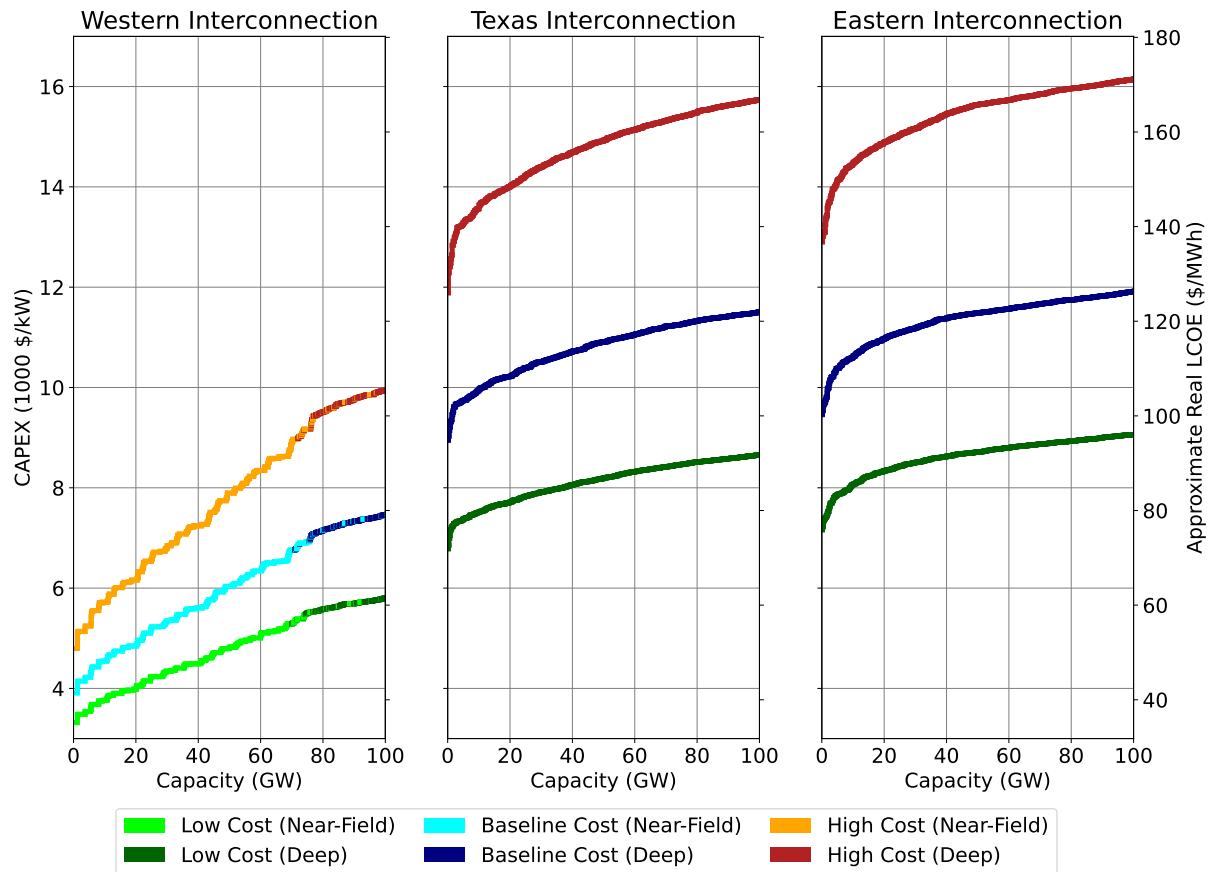
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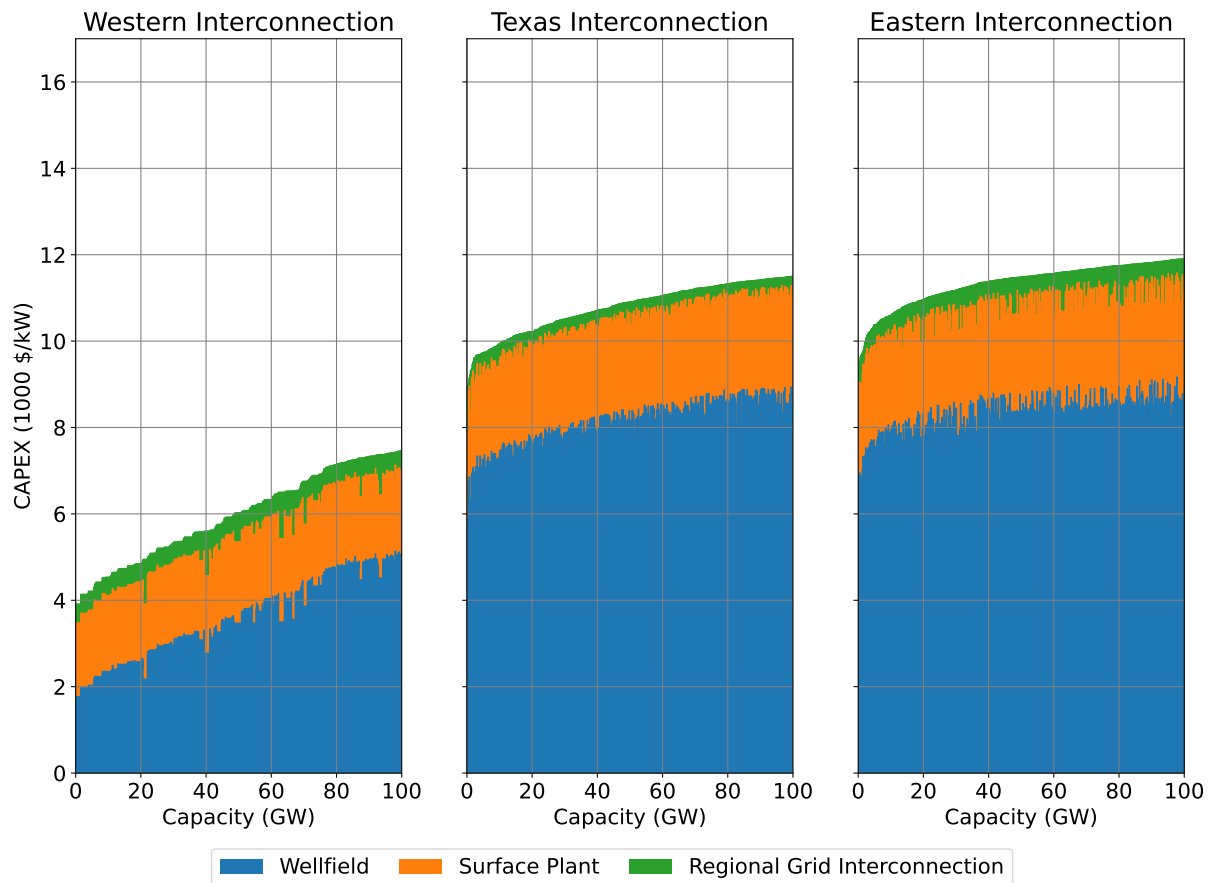
Supplementary Note 1: Supplementary Figures



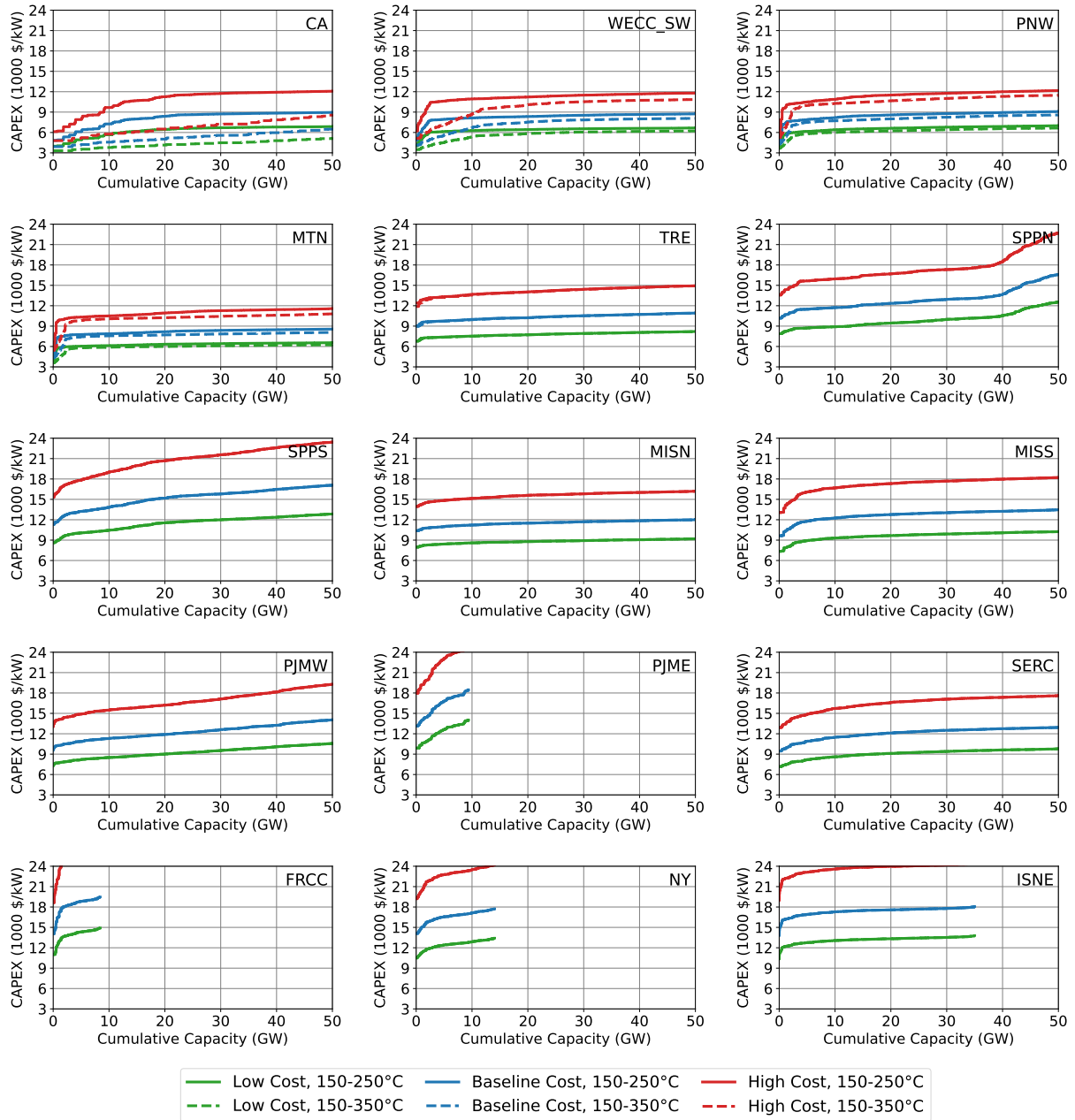
Supplementary Figure 1: Top-down schematic of the near-term commercial EGS reservoir design used in this work. Injection wells are shown in blue and production wells in red. Individual fractures are drawn for illustrative purposes and do not reflect simulated or expected real world fracture geometries.



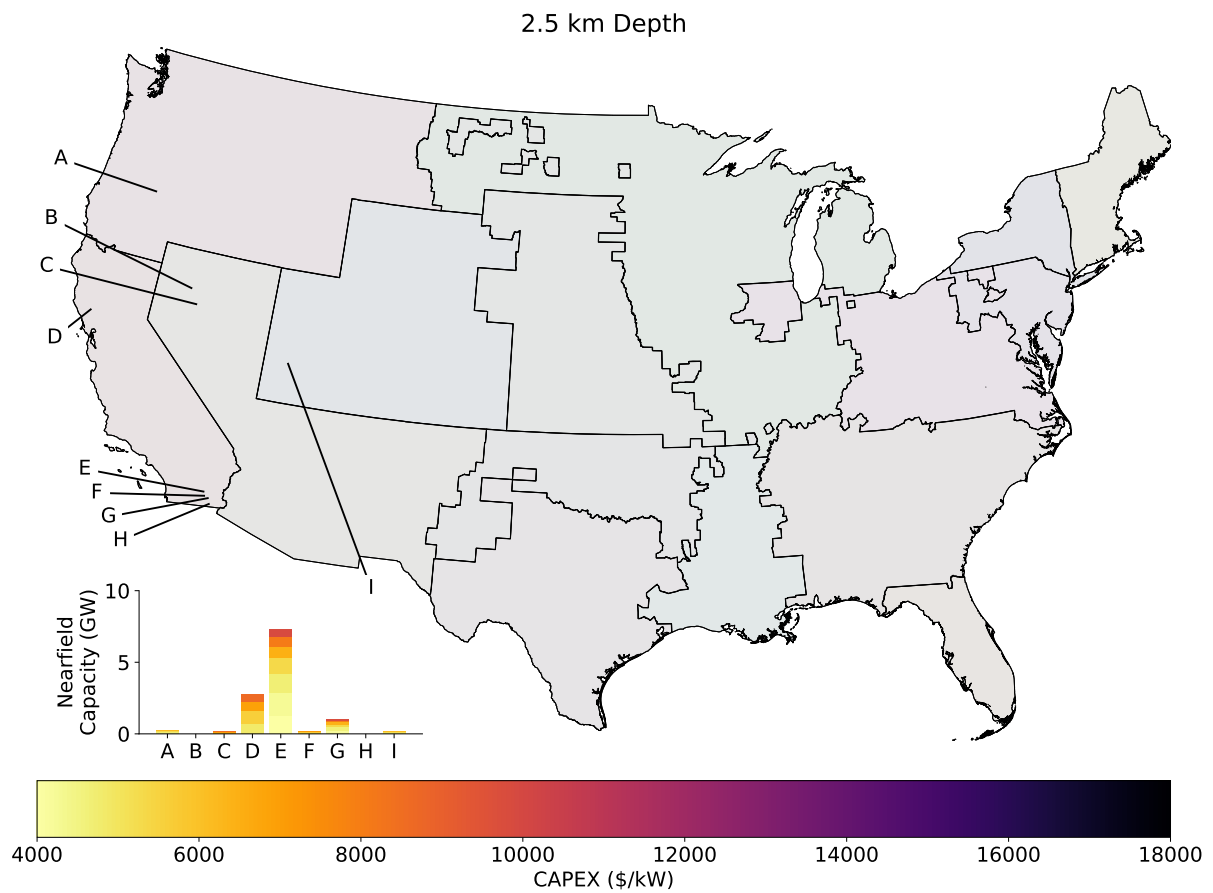
Supplementary Figure 2: Same as Figure 1 in the main paper, for resources with reservoir temperatures in the 150-350°C range. A higher temperature threshold enables more extensive exploitation of high-quality near-field resources.



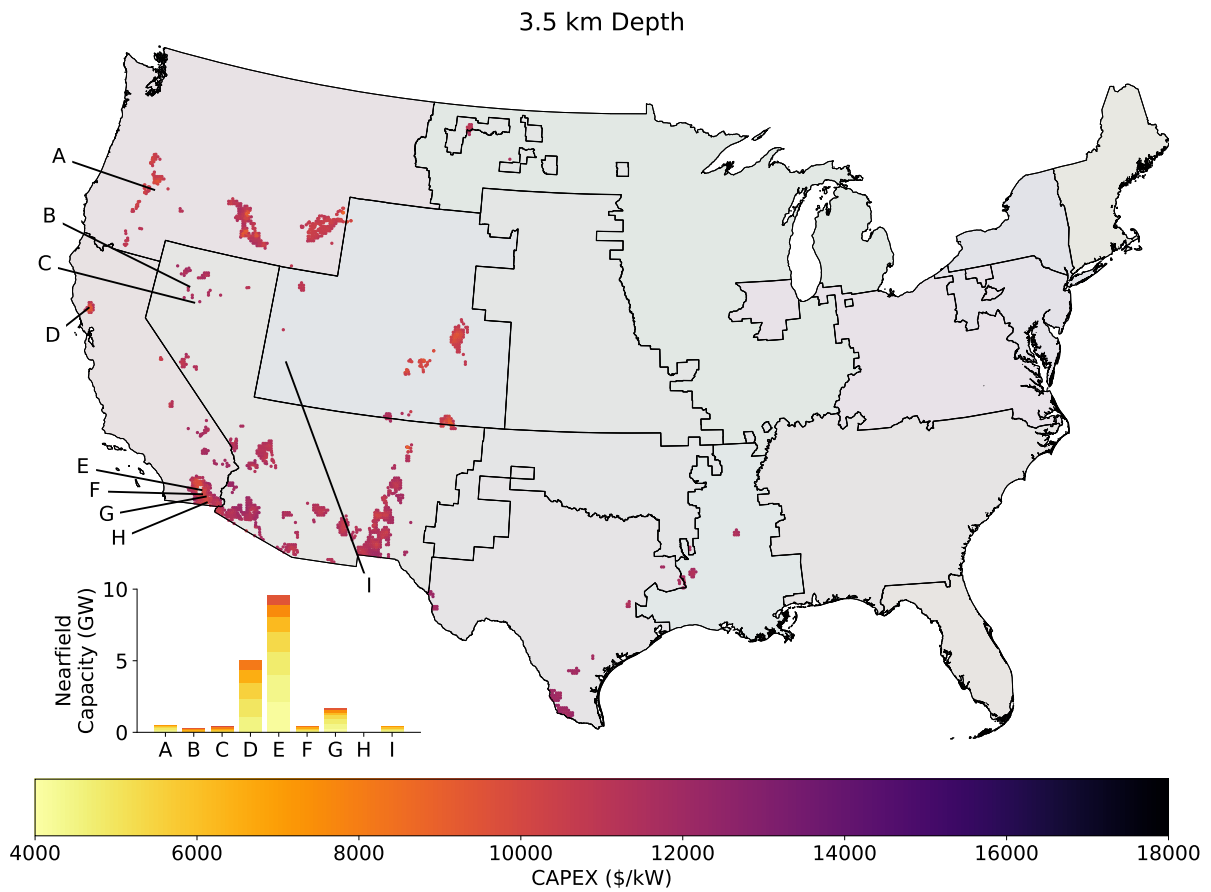
Supplementary Figure 3: Breakdown of near-term unsubsidized EGS CAPEX by cost component, for the baseline cost case supply curve shown in Figure 1 in the main paper. The wellfield is the largest cost component in most cases. Some otherwise high-quality resources are made more expensive by high interconnection costs.



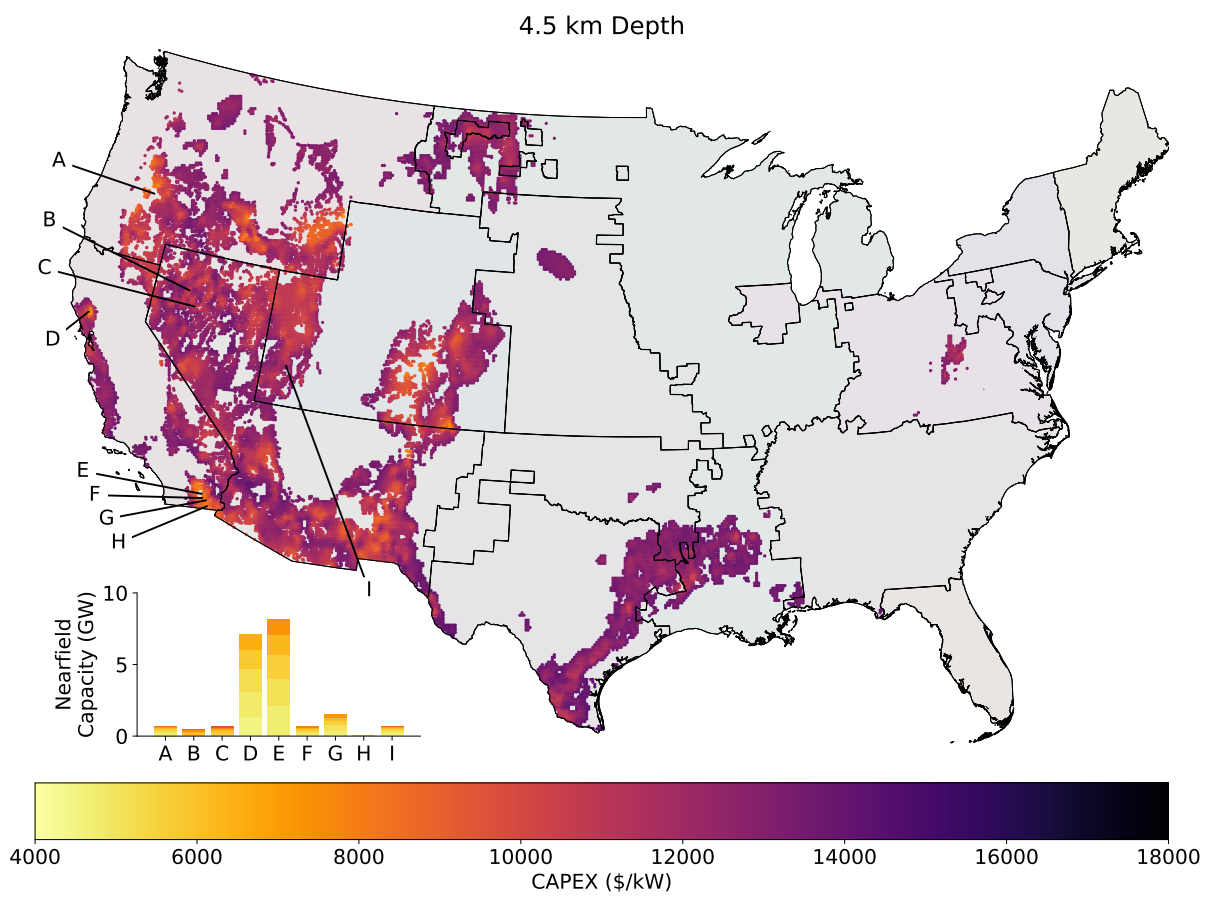
Supplementary Figure 4: EGS supply curves for 15 US grid regions used in electricity sector capacity expansion modeling in this work (see Supplementary Figure 10), for resources in the 150-250°C and 150-350°C ranges, under three different wellfield cost scenarios.



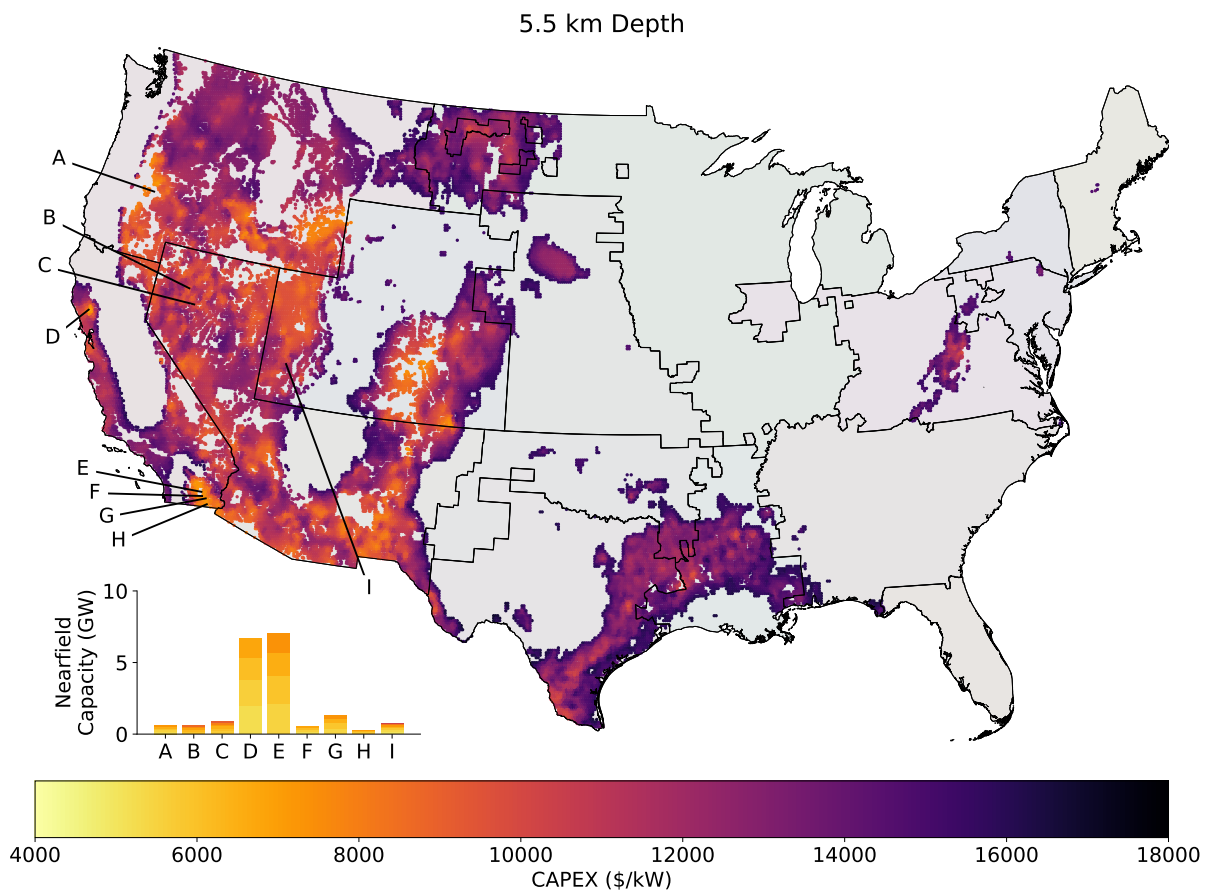
Supplementary Figure 5: Map showing CAPEX for developable EGS capacity near nine large hydrothermal systems in the western US at a depth of 2.5 km, for reservoir temperatures in the 150-350°C range, under baseline cost assumptions. Grid regions used in electricity sector capacity expansion modeling are also shown.



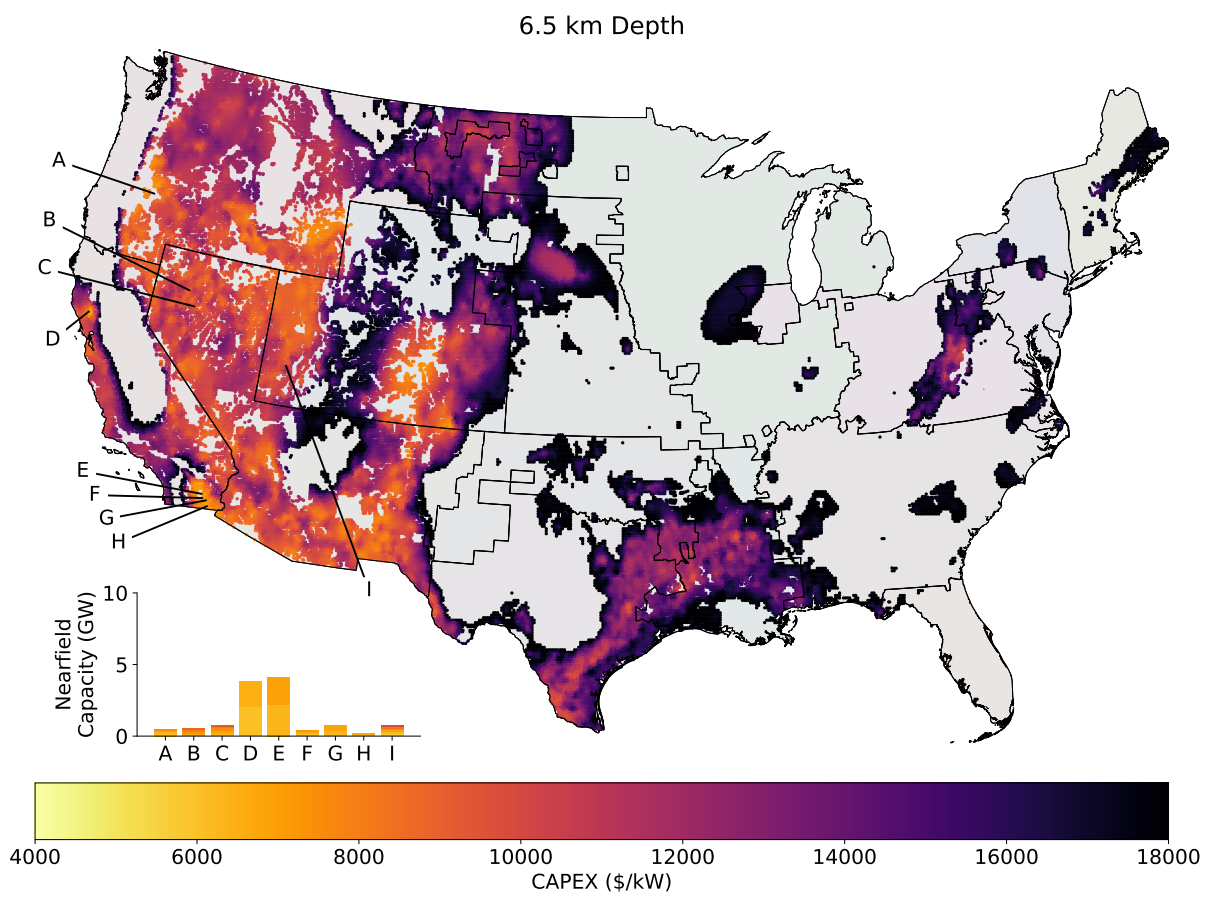
Supplementary Figure 6: Map showing CAPEX for developable EGS capacity near nine large hydrothermal systems in the western US and at deep EGS candidate project areas nationwide (using temperature-at-depth data sourced from Blackwell et al. [1]) at a depth of 3.5 km, for reservoir temperatures in the 150-350°C range, under baseline cost assumptions. Grid regions used in electricity sector capacity expansion modeling are also shown.



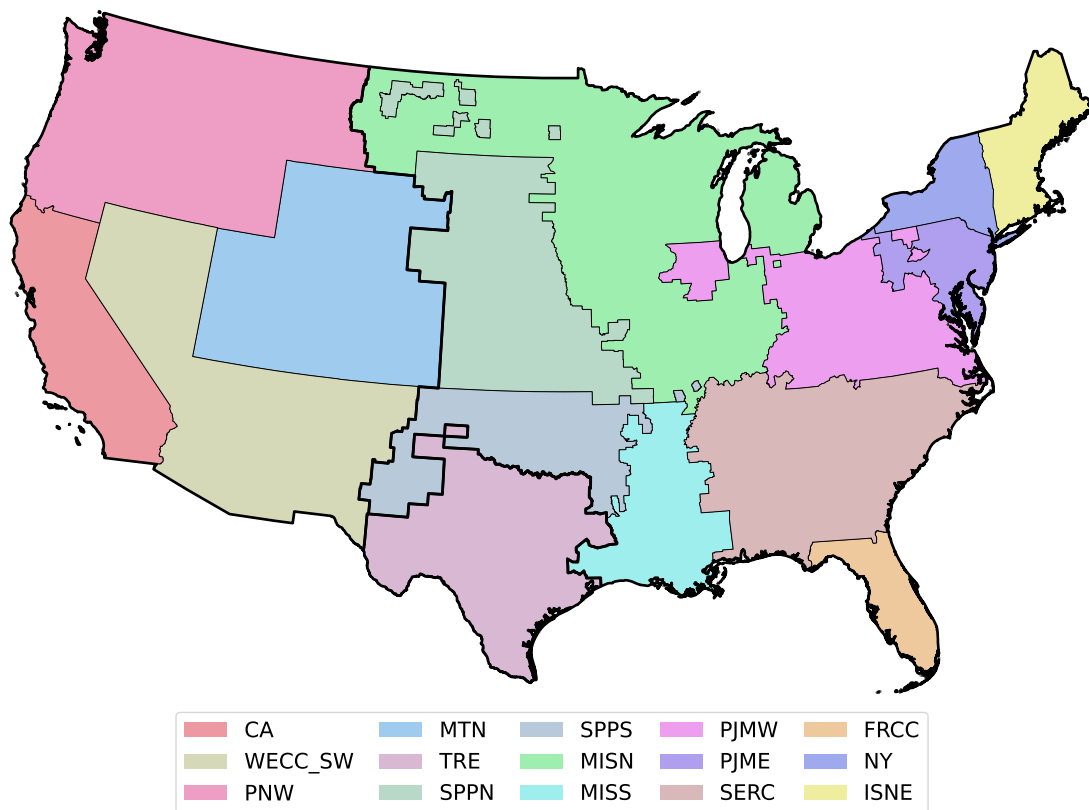
Supplementary Figure 7: Same as Supplementary Figure 6, for resources at a depth of 4.5 km.



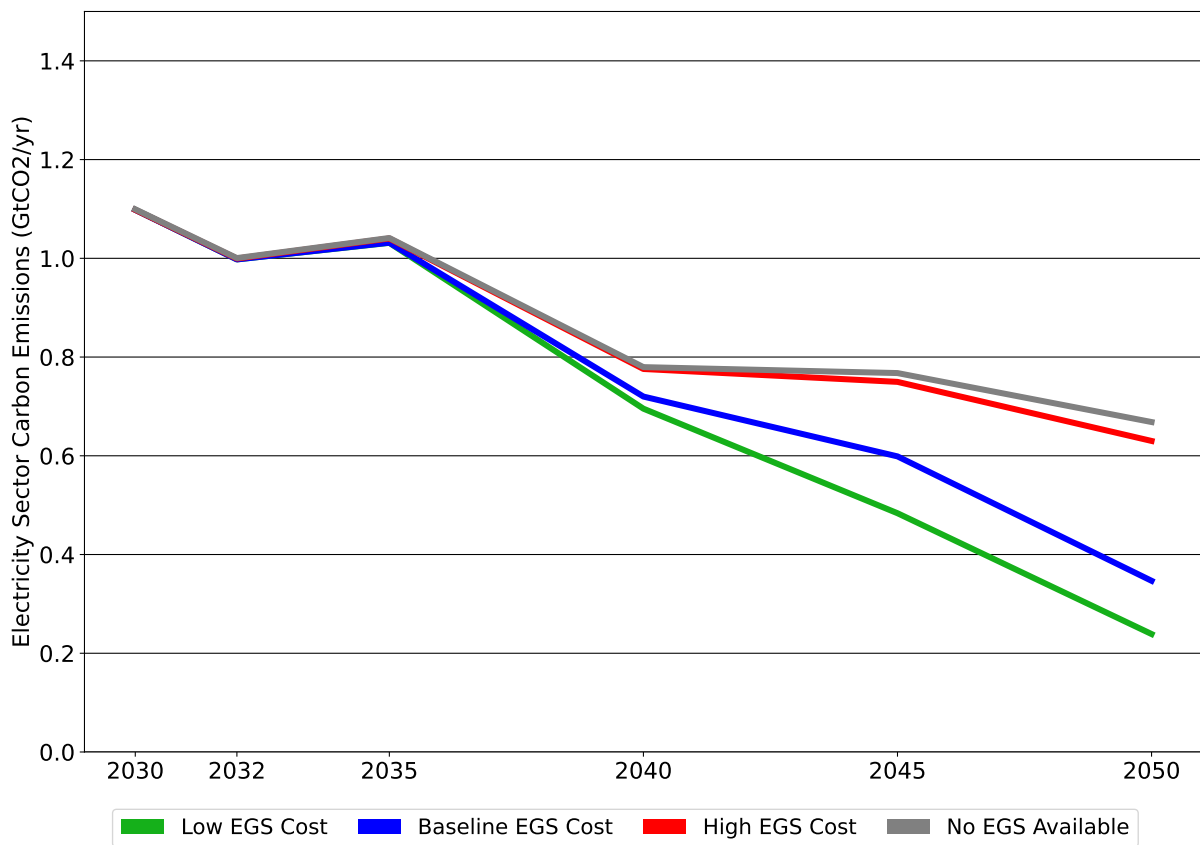
Supplementary Figure 8: Same as Supplementary Figure 6, for resources at a depth of 5.5 km.



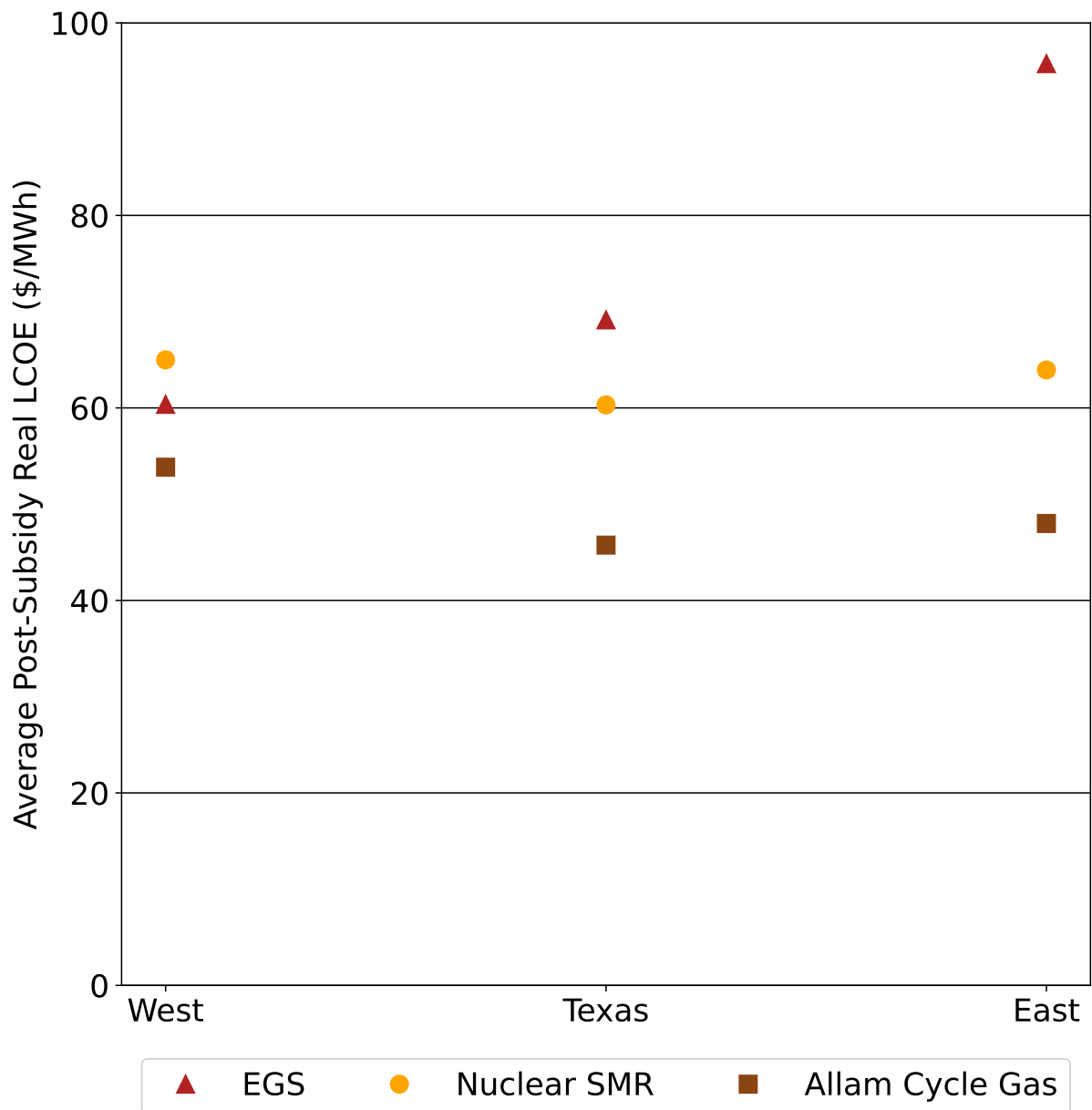
Supplementary Figure 9: Same as Supplementary Figure 6, for resources at a depth of 6.5 km.



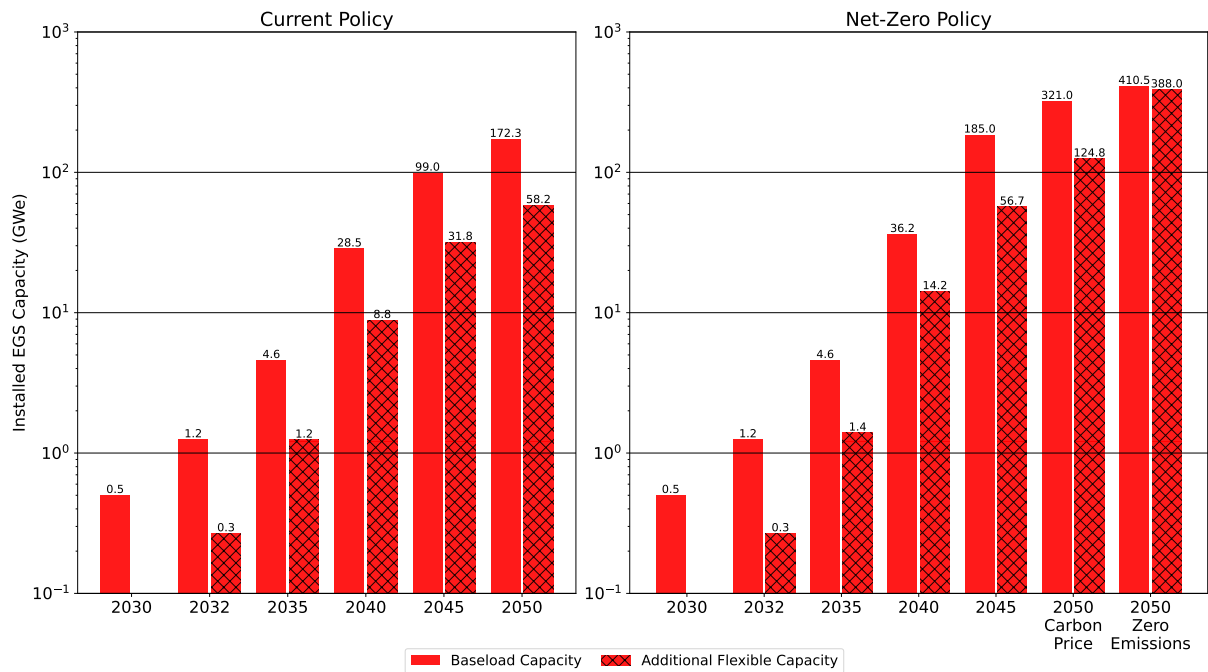
Supplementary Figure 10: 15-zone topology used to represent the regional structure of the contiguous US electricity system within the GenX electricity system capacity expansion model. Zones are aggregated to minimize internal transmission bottlenecks. The three major synchronous interconnections that make up the US grid are outlined in bold.



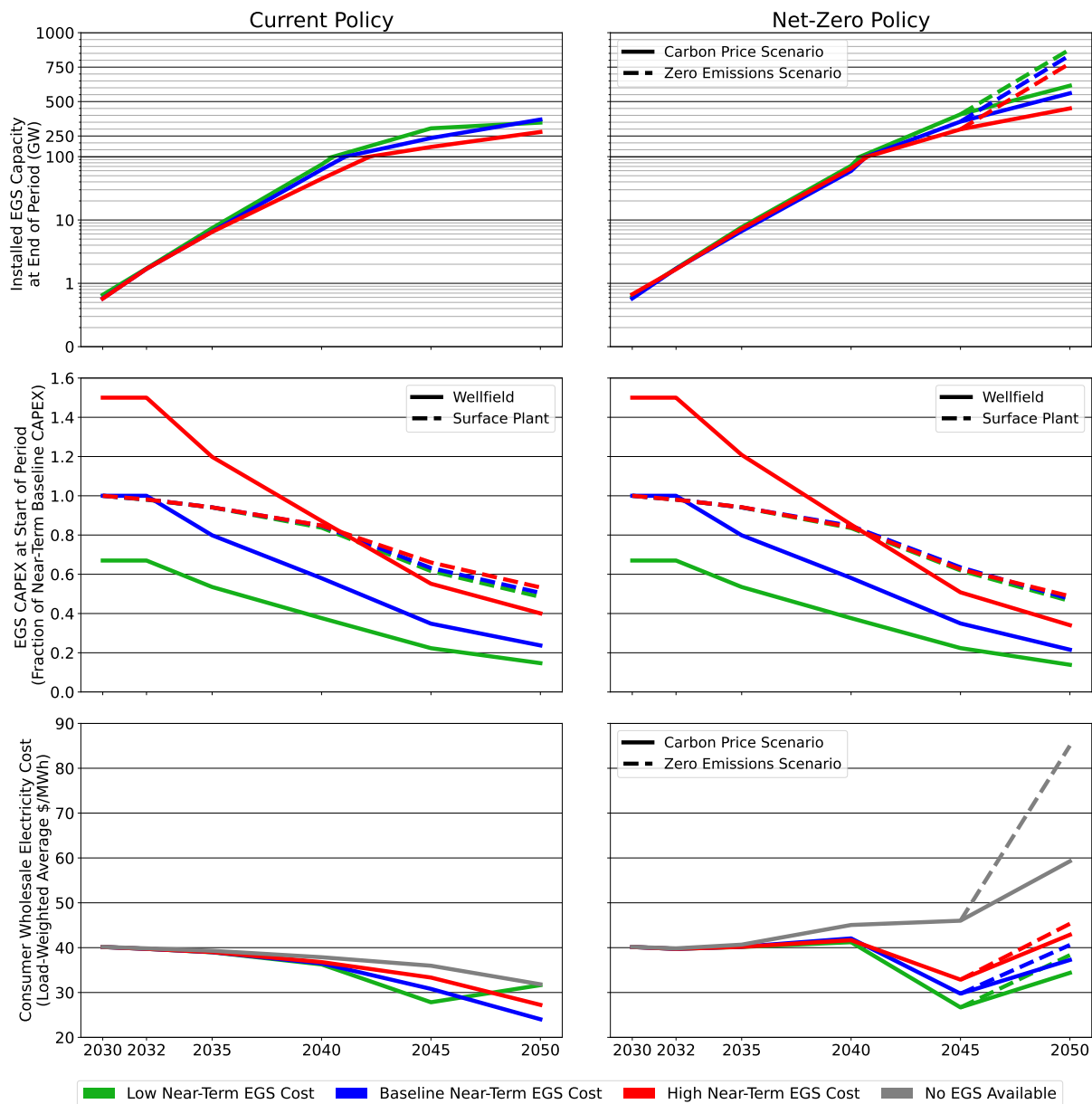
Supplementary Figure 11: Trajectories of contiguous US power sector CO₂ emissions for three EGS cost cases, and a case where EGS is unavailable, under a current policy scenario.



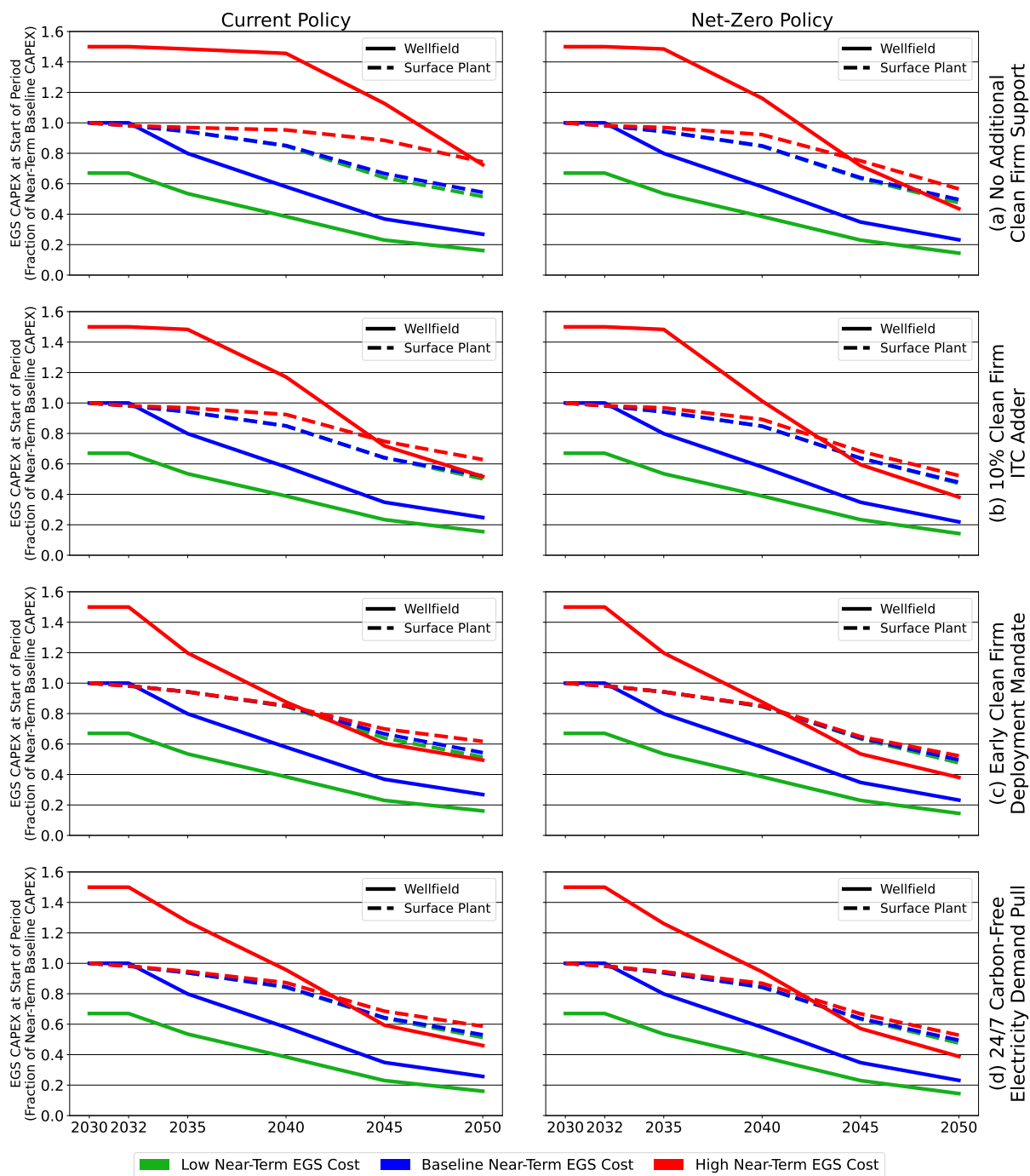
Supplementary Figure 12: Average post-subsidy real LCOE for EGS at baseline costs (among all sites available for deployment in the model), nuclear SMRs, and Allam cycle gas power plants in the 2031-2032 planning period, for the three synchronous grids serving the contiguous US.



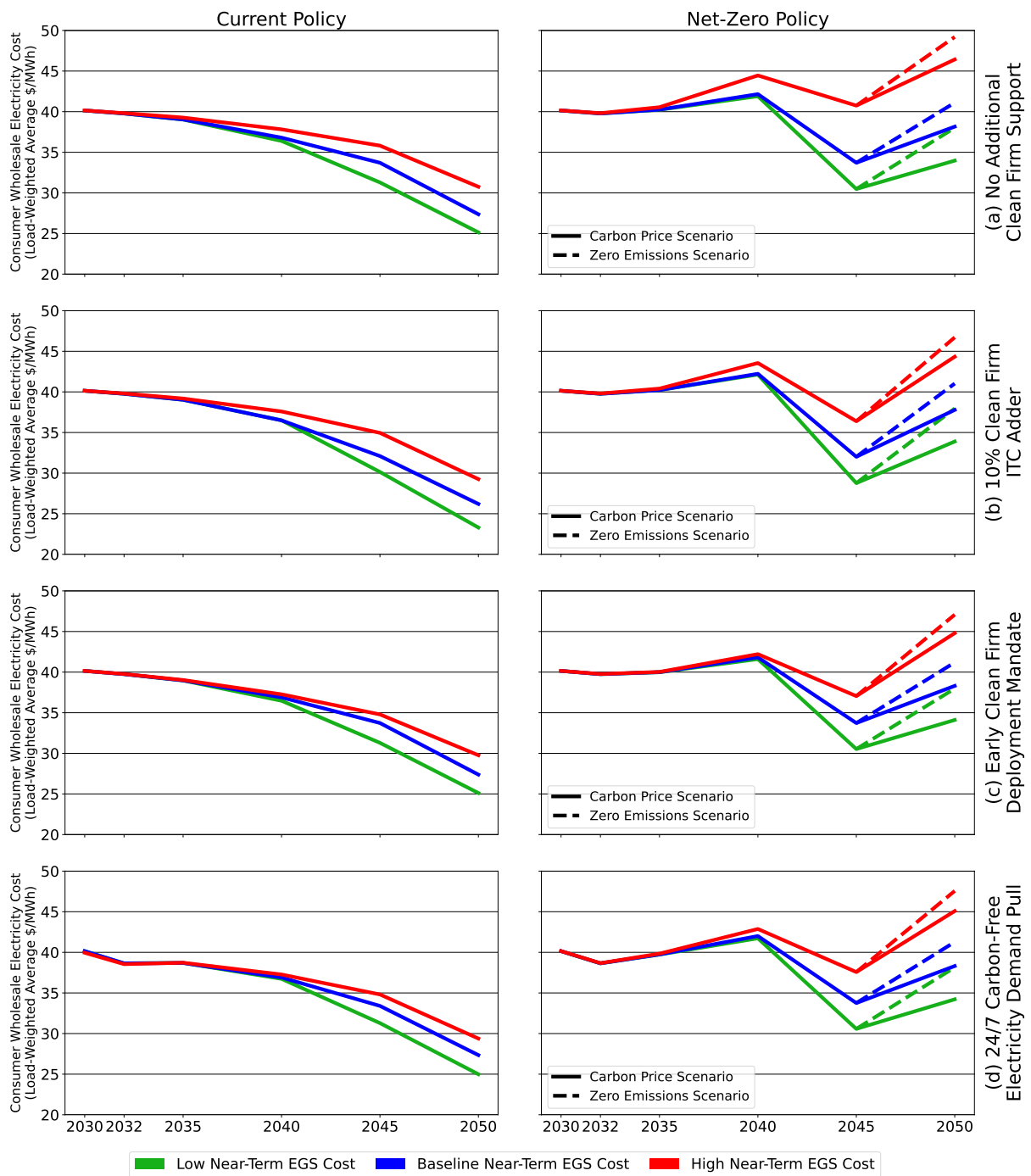
Supplementary Figure 13: Nationwide installed EGS baseload capacity (the capacity at which the well-field can produce power at a constant rate under design point conditions while maintaining the target thermal decline rate) and additional flexible capacity (used to enable greater power production for limited durations) for the same scenarios shown in Figures 3 and 4 in the main paper. Note that the sum of baseload and flexible capacities in this figure is not equal to the maximum interconnection capacity shown in Figure 3, as low ambient air temperatures can cause the power plant to generate above its rated design point capacity.



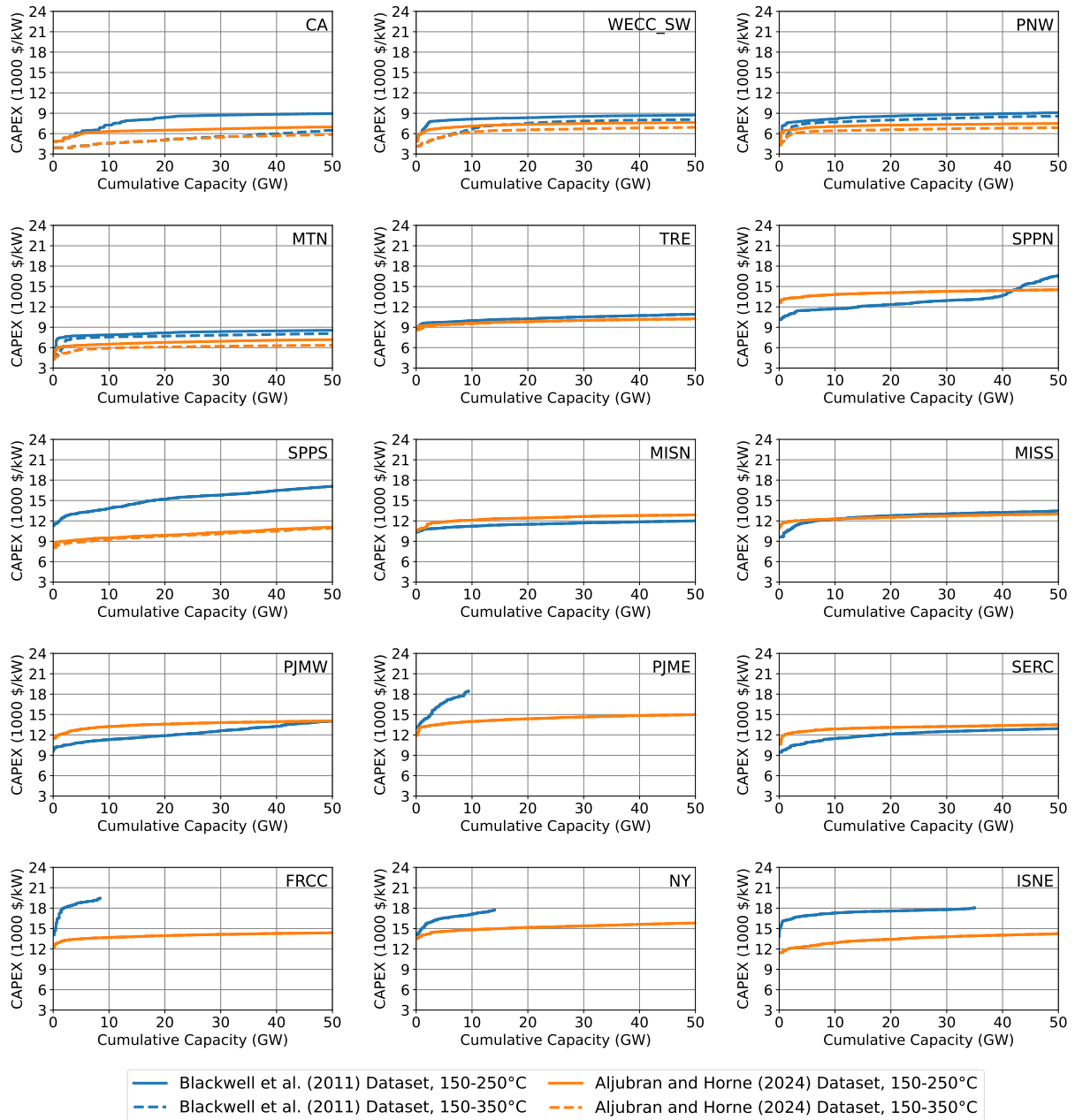
Supplementary Figure 14: Same as Figure 2 in the main paper, for cases where an additional 20% adder is made available for firm carbon-free resources under the Section 48E Investment Tax Credit, and for carbon sequestration under the 45Q CCS tax credit. We note that the scenario with low EGS costs under current policies reaches the emissions threshold at which Inflation Reduction Act clean electricity tax credits phase out during the 2040-2045 planning period, leading to higher effective EGS costs in 2045-2050 and relatively lower deployment than in scenarios where the phase-out does not occur.



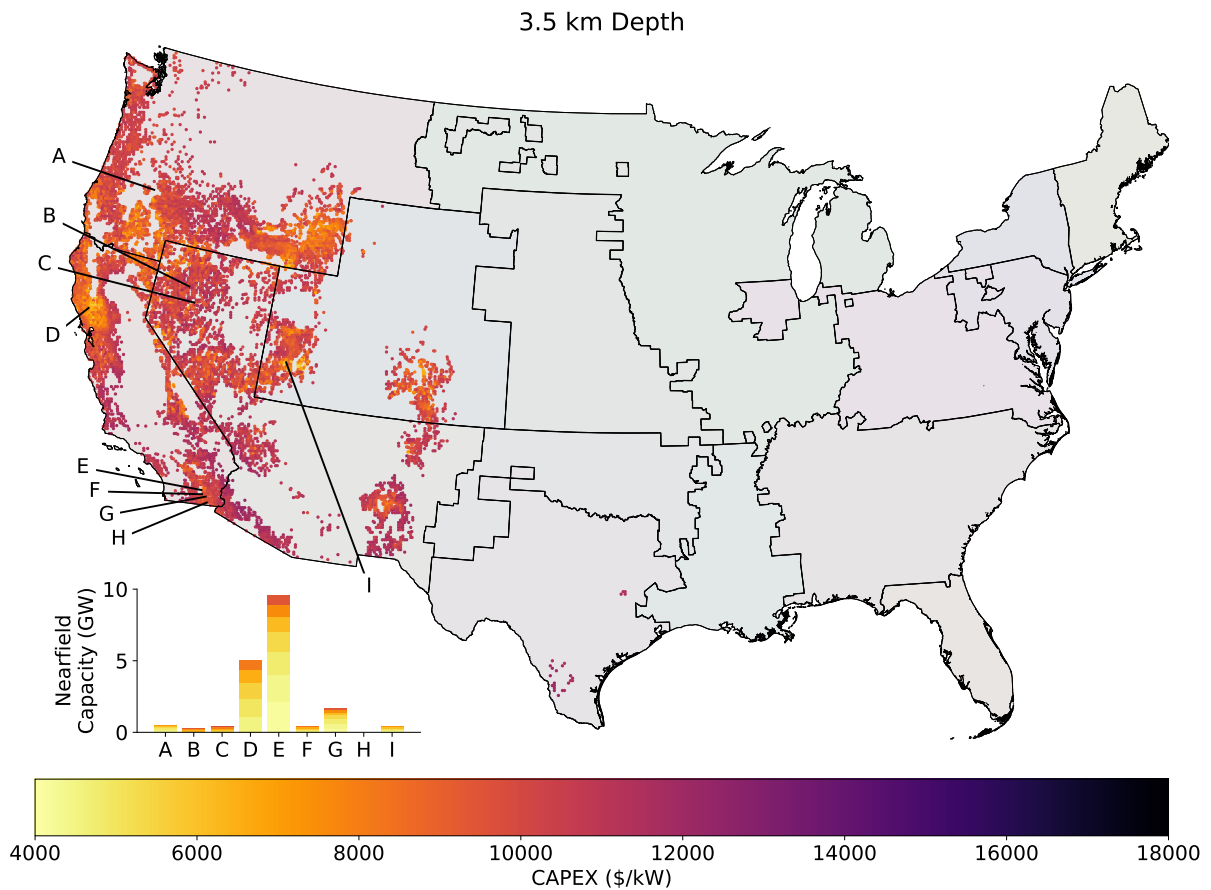
Supplementary Figure 15: Trajectories of EGS capital costs for the same scenarios shown in Figure 6 in the main paper.



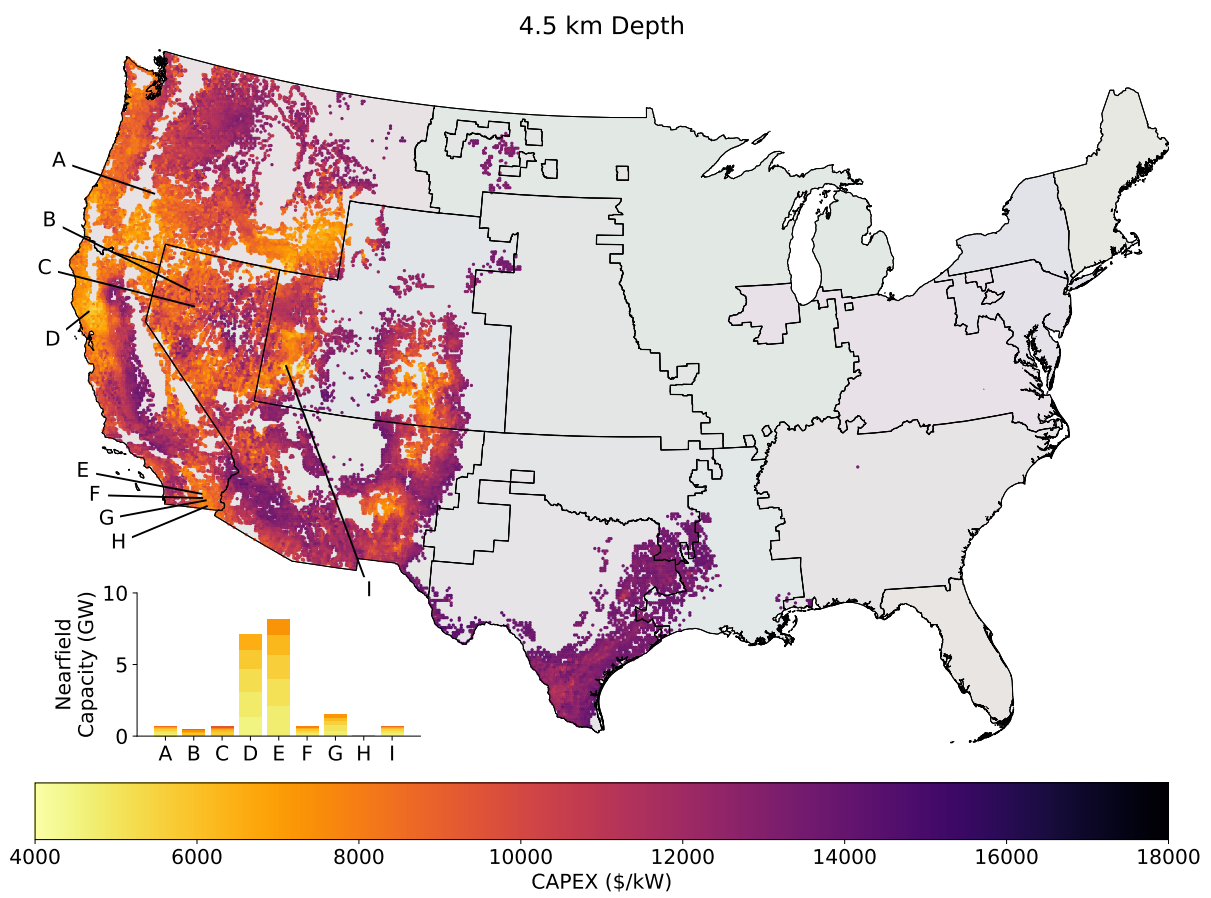
Supplementary Figure 16: Trajectories of consumer electricity costs for the same scenarios shown in Figure 6 in the main paper.



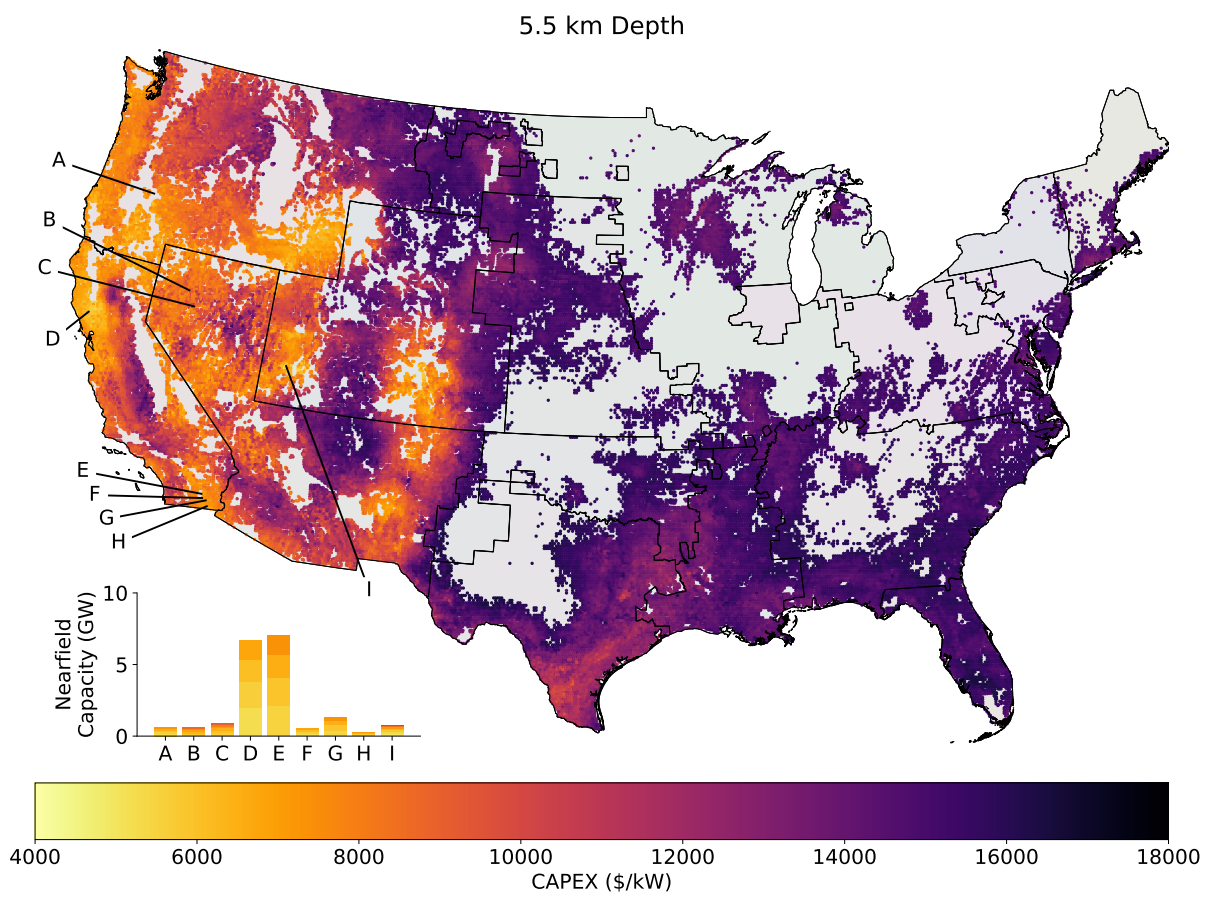
Supplementary Figure 17: EGS supply curves for 15 US grid regions used in electricity sector capacity expansion modeling in this work (see Supplementary Figure 10), for resources in the 150-250°C and 150-350°C ranges, under baseline cost assumptions, using deep temperature-at-depth data from Blackwell et al. [1] and Aljubran and Horne [2].



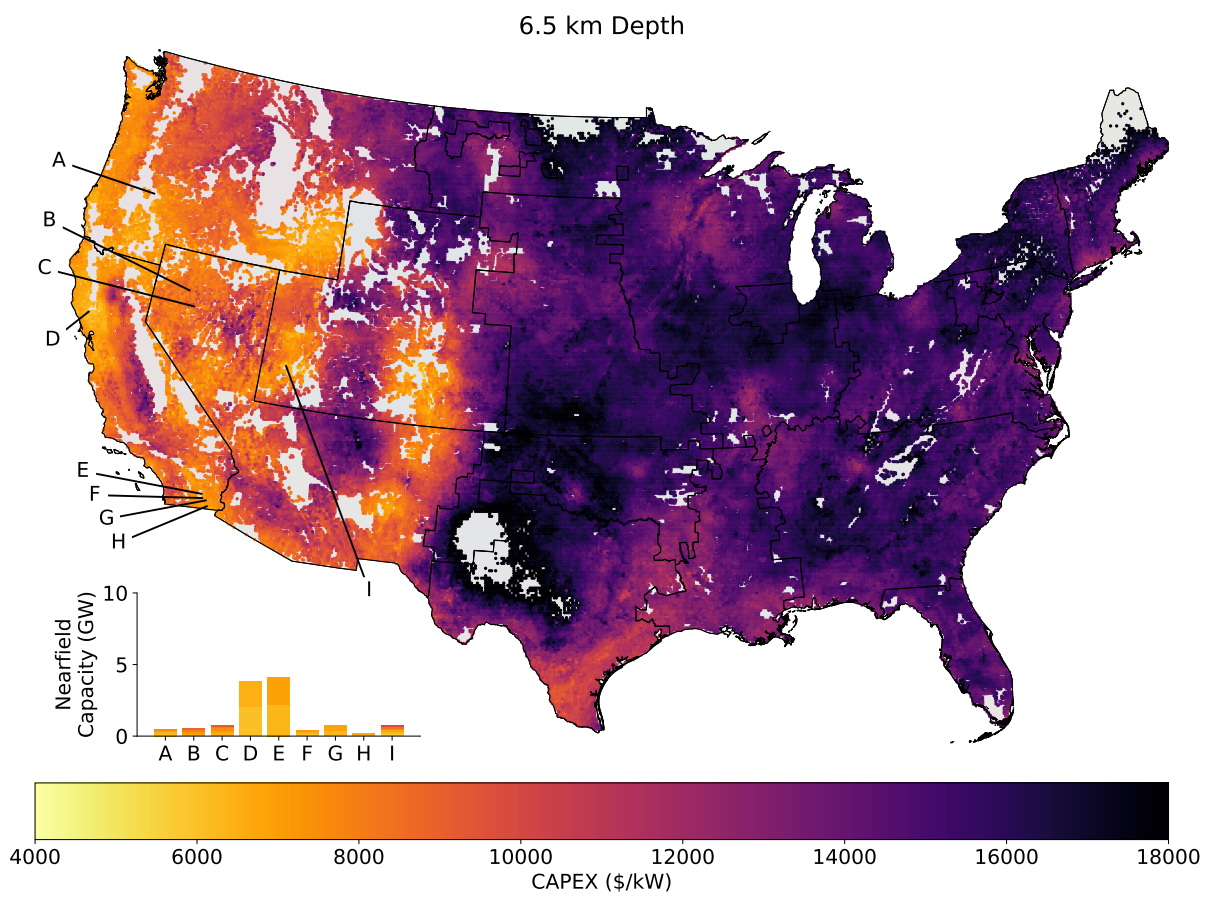
Supplementary Figure 18: Map showing CAPEX for developable EGS capacity near nine large hydrothermal systems in the western US and at deep EGS candidate project areas nationwide (using temperature-at-depth data sourced from Aljubran and Horne [2]) at a depth of 3.5 km, for reservoir temperatures in the 150-350°C range, under baseline cost assumptions. Grid regions used in electricity sector capacity expansion modeling are also shown.



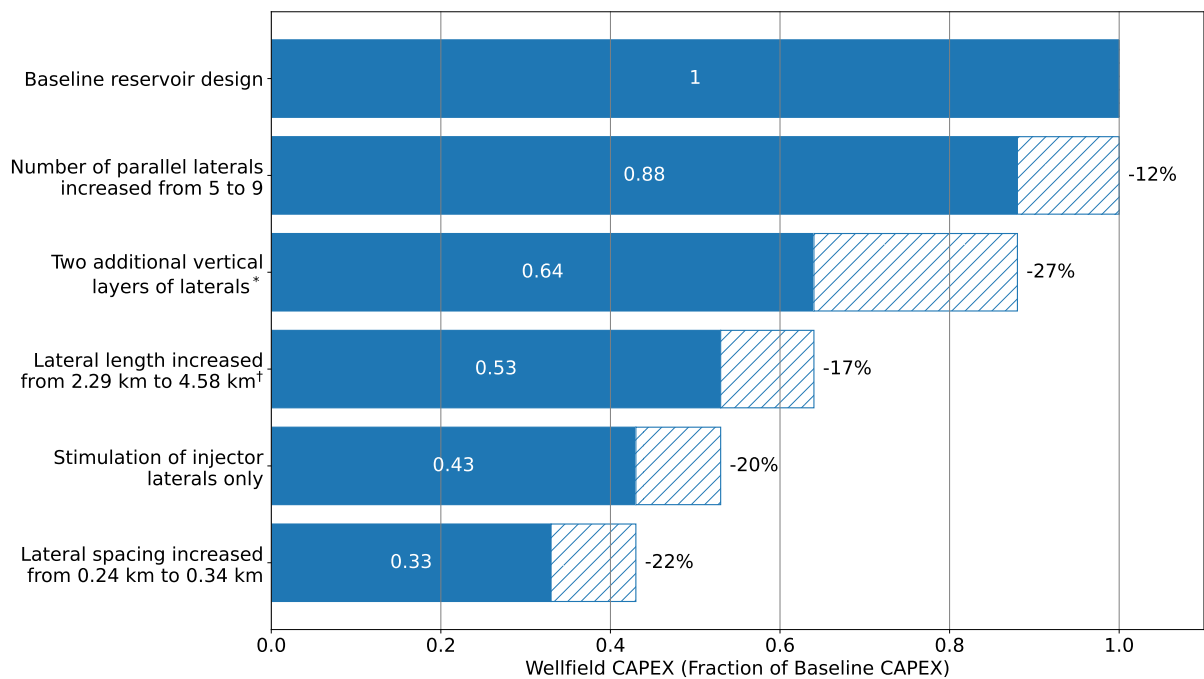
Supplementary Figure 19: Same as Supplementary Figure 18, for resources at a depth of 4.5 km.



Supplementary Figure 20: Same as Supplementary Figure 18, for resources at a depth of 5.5 km.



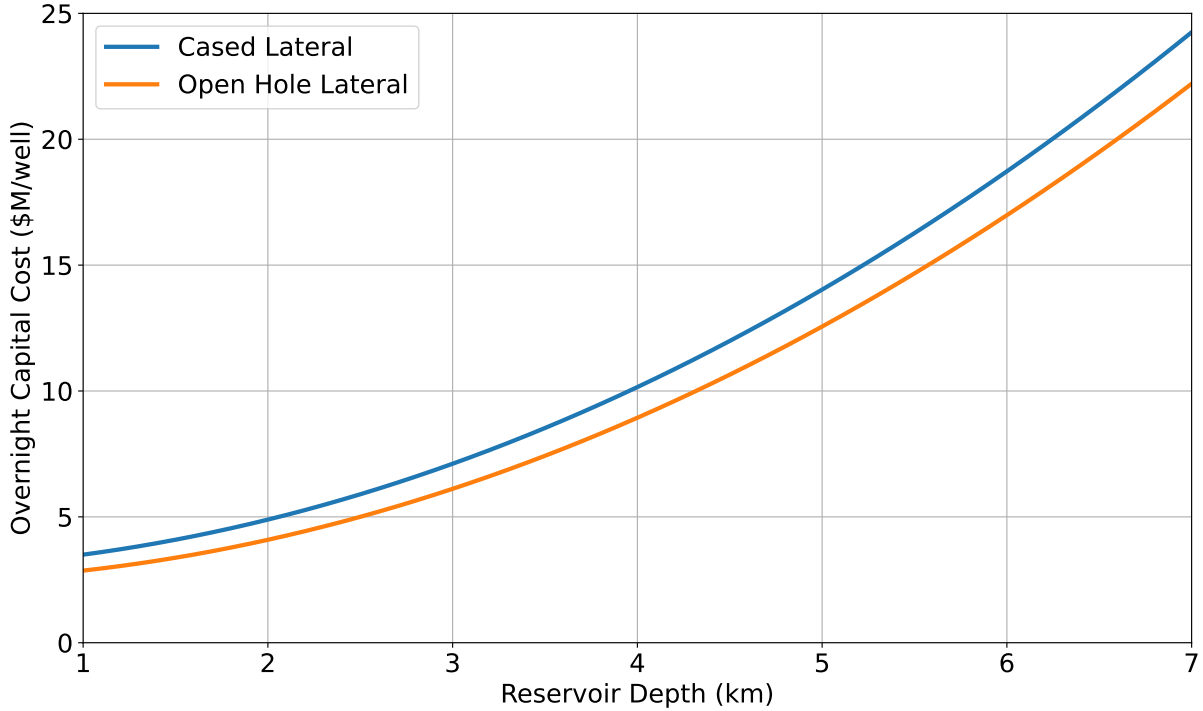
Supplementary Figure 21: Same as Supplementary Figure 18, for resources at a depth of 6.5 km.



Supplementary Figure 22: Impact of changes in reservoir design on EGS wellfield per-kW cost. Costs for different reservoir designs are calculated using the EGS cost model discussed in Supplementary Note 2.1, and presented reductions are equal to the average values observed for representative EGS resources with temperatures of 175-300°C and depths of 2.5-6.5 km. Listed design changes are retained moving down the chart. For iterations marked with * and †, average well costs are increased by 10% and 20%, respectively, to account for greater diameters needed to handle higher flow rates while minimizing parasitic pumping losses.

Supplementary Note 2: Supplementary Methods

Supplementary Note 2.1: EGS Cost and Performance Assumptions

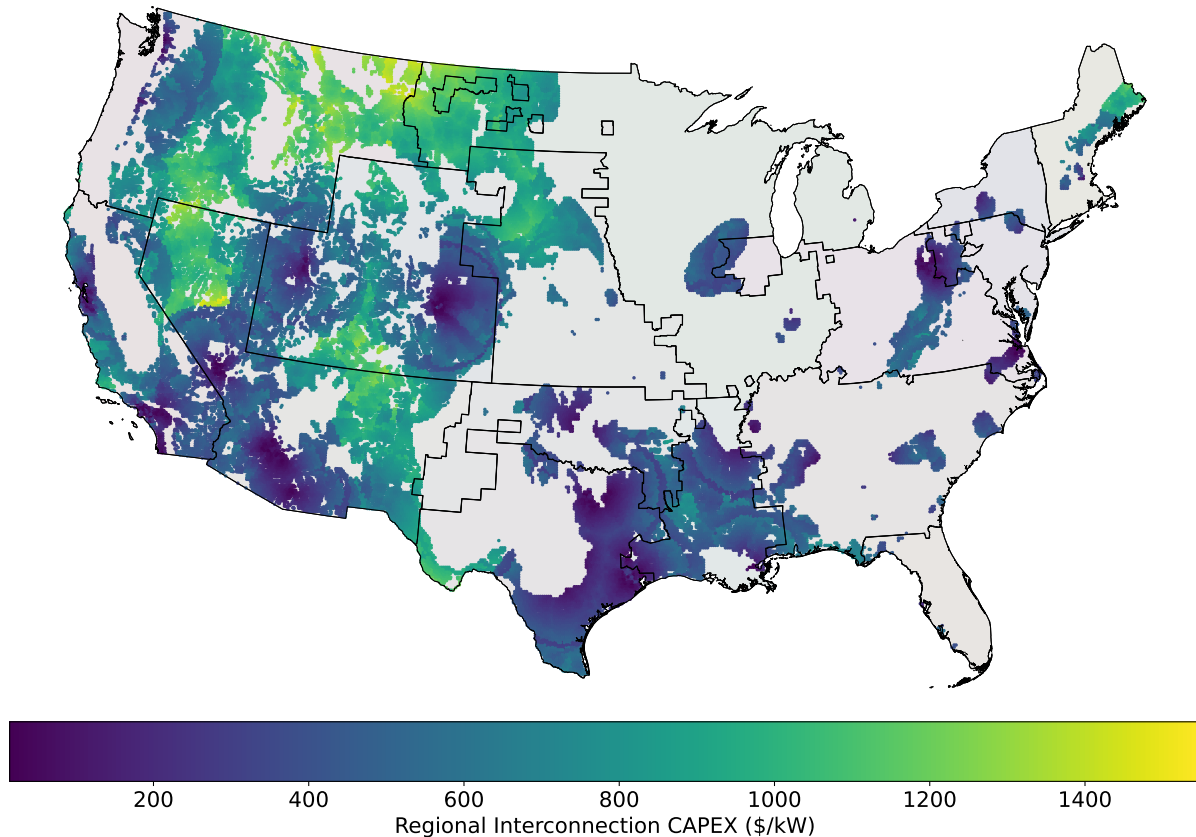


Supplementary Figure 23: Drilling cost as a function of total vertical depth, for wells with 24.4 cm outer diameter and 2.29 km lateral length. Laterals are assumed to be cased by default, and open hole completion is only used if laterals are not stimulated (e.g. in Supplementary Figure 22).

We use results from numerical EGS reservoir simulations described in Ricks et al. [3] to calculate a thermal decline profile for the reservoir over a 30-year operational lifetime and the impact of this decline on a plant's net present value. While the simulations from Ricks et al. [3] predict an average thermal decline of 28°C (or a 44% decline in power output) after 30 years of operation for a reservoir with 2.29 km lateral length, 0.34 km lateral spacing, and a 160 l/s flow rate per injection well, these simulations assumed a perfectly uniform fracture network that is unlikely to be replicated in real-world EGS reservoirs. Because nonuniformities in fracture structure and flow rate can accelerate thermal decline compared to uniform systems, we assume here that the 28°C decline occurs after 25 years rather than 30, leading to a 35°C decline in temperature (or a 58% decline in power output) after 30 years. Using a real weighted average cost of capital for EGS projects of 5.48% adopted from ATB [4], we calculate that this thermal decline leads to a 6.4% decline in the net present value of an EGS project. This reduction is applied to the modeled capacity factor of all EGS plants, as discussed in the following section. Because the reservoir design used in this paper has a lateral spacing 29% lower than the one simulated in Ricks et al. [3], we reduce the steady-state flow rate in our assumed reservoir design by 23% to maintain the same thermal decline rate, using scaling relations for lateral spacing and flow rate from Doe and McLaren [5].

In line with Ricks et al. [3] and Geo [6], we assume that all EGS surface plants are air-cooled binary-cycle, offering zero emissions, greatly reduced water consumption, and increased operational flexibility compared to flash or dry steam plants. We update the surface plant cost model to calculate labor costs as a function of installed capacity, in line with Mines [7], and adjust labor and surface plant costs to the 2021 dollar year based on the relevant producer price indices. The full updated EGS cost model incorporating these and the above assumptions is available as a Python script at Ricks and Jenkins [8], alongside all other relevant input data and results for the present study.

Supplementary Note 2.2: EGS Supply Curves



Supplementary Figure 24: Map of regional grid interconnection costs for all EGS CPAs without land use barriers and with resource temperatures greater than 150°C at 6.5 km depth in the Blackwell et al. [1] dataset.

We use the EGS cost model discussed above to calculate EGS cost and developable capacity for over 80,000 candidate project areas (CPAs) at depths of 3.5 km, 4.5 km, 5.5 km, and 6.5 km based on deep temperature-at-depth values from Blackwell et al. [1] and alternatively from Aljubran and Horne [2]. Because the Aljubran and Horne [2] maps are provided for depths of 1-7 km at 1 km intervals, we linearly interpolate between layers to extract predicted values at the same depths as the Blackwell et al. [1] maps. We assume conservatively that each depth band can host a single ‘layer’ of reservoirs, and we further de-rate developable capacities for all CPAs by 80% to account for potential land acquisition challenges and subsurface barriers such as fault lines.

As noted in Aljubran and Horne [2], neither of these deep temperature-at-depth datasets explicitly models the highly convective thermal regimes found at and near hydrothermal sites, and both may thus severely underestimate temperatures in these regions. Because there exists no prior comprehensive assessment of this ‘near-field’ EGS potential, we use reservoir volume and temperature data for these systems from Williams et al. [9] in combination with a detailed temperature-at-depth survey for the Roosevelt Hot Springs geothermal area in Utah (the site of FORGE and ongoing private EGS demonstrations) [10] to estimate the developable near-field EGS capacity at all known hydrothermal sites in the contiguous US. We use the Roosevelt data to assess the cross-sectional subsurface area that exists within different 25°C temperature bands at a depth of 2.5 km around this site, and compare these measurements with the volume and temperature of the hydrothermal reservoir as provided in Williams et al. [9]. We fit a linear relationship between these quantities (see ‘FORGETemp.xlsx’ in Ricks and Jenkins [8] for details) and apply this relationship to all other hydrothermal sites in the Williams et al. [9] dataset. While the relationship between temperature-at-depth and reservoir properties from Roosevelt is likely not perfectly representative of other near-field sites, we do find that it largely agrees with coarser estimates presented

in MIT [11] of the near-field resource available near the large Geysers hydrothermal reservoir in northern California. While the Roosevelt relationship estimates an area of $\sim 900 \text{ km}^2$ at temperatures greater than 150°C near the Geysers at a depth of 2.5 km, the site-specific maps presented in MIT [11] suggest an area of just over 1000 km^2 at the same temperature and depth. In addition to near-field temperature-at-depth data for the 2.5 km depth band, we also use an assumed 50 C/km geothermal gradient (slightly more conservative than the 70 C/km observed at Roosevelt) to calculate similar values for depths of 3.5 km, 4.5 km, 5.5 km, and 6.5 km. We cut off near-field data at all depths for bands where the temperature is below either 150°C or the temperature of the nearest site at the same depth in the deep temperature-at-depth dataset. We apply the same costing methodology to near-field sites that is used for deep CPAs, but derate near-field resources by 60% rather than 80% to account for more established land rights and electricity system interconnections at these sites.

Finally, we calculate hourly capacity factor time series for each geothermal CPA for the 2012 weather year based on hourly surface ambient temperature data, following the same procedure outlined in Ricks et al. [3]. This calculation assumes that all surface power plants are air-cooled to minimize water consumption. We modify these time series by subtracting 6.4% from the effective output in each hour, reflecting the net present value impact of thermal decline in the reservoir over the lifetime of a project as described above.

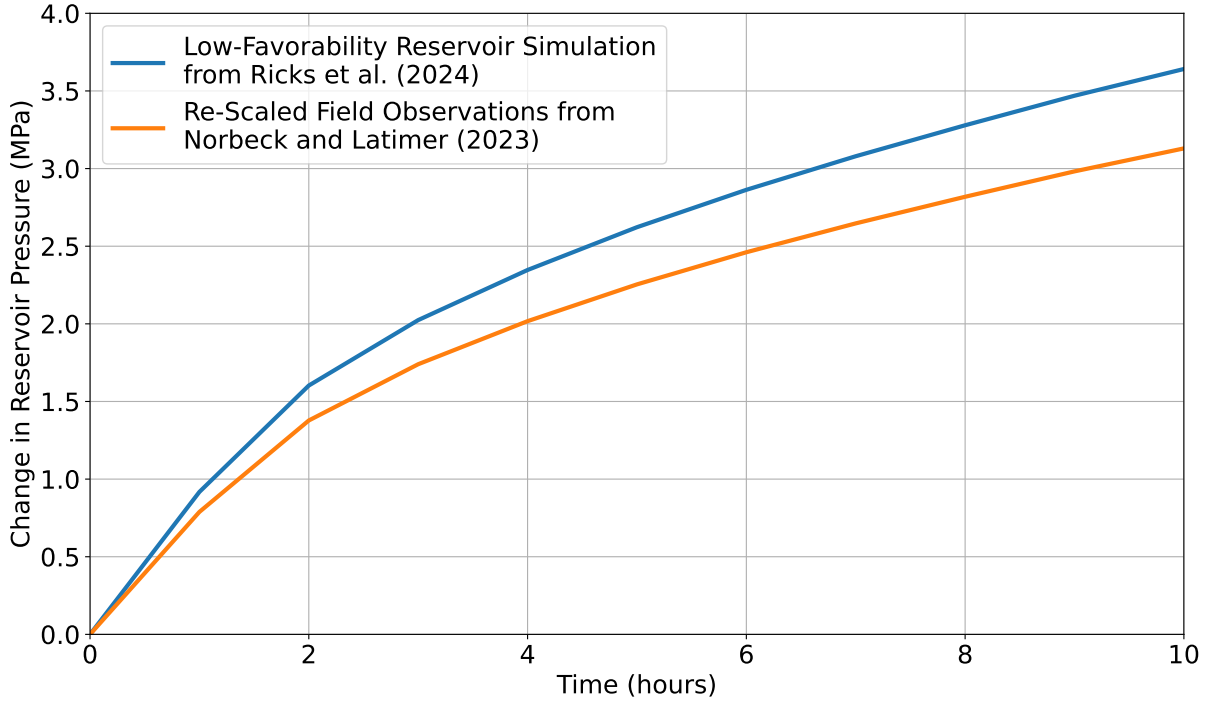
Supplementary Note 2.3: EGS Model Structure and Inputs

As discussed above, we modify the public release of the GenX model in this work to incorporate the flexible EGS module described in Ricks et al. [3]. This module allows for optimization of the sizing of individual EGS plant components and of well flow rates in each modeled timestep. Optimized components include wellfield capacity, surface binary-cycle power plant capacity, grid interconnection capacity, and injection pumping power capacity. To limit model complexity we do not model or optimize the sizing of surface storage for excess produced geofluid, as results from Ricks et al. [3] indicate that this component typically accounts for less than 1% of the total cost of an EGS plant. In addition to component sizing the model optimizes injection and production flow rates for each EGS resource in each timestep, tracking the evolution of reservoir pressure across timesteps via a formulation that accurately captures the pressure behaviors observed in numerical reservoir simulations [3, 12]. Pressure metrics at injection and production well bottomholes are used to calculate parasitic injection pumping power requirements and maximum achievable production flow rates at each timestep, respectively.

In this paper we use the same default model parameters as Ricks et al. [3], with the following exceptions. First, we enforce a minimum production flow rate of 10% of the steady-state production rate for all EGS facilities, reflecting the need to avoid thermal cycling from full production shutdowns that could harm wellbore integrity [13, 14]. Second, we adjust parameters for the pressure differential across the reservoir during steady-state operation to reflect the fracture conductivity values calculated from field tests as described above. We use a power law fit of cross-reservoir pressure differential values from the same set of EGS reservoir simulations described in Ricks et al. [3] to calculate the expected pressure differential for a $1.2 \times 10^{-13} \text{ m}^3$ fracture conductivity value under the same operating conditions, then scale this down to reflect the smaller lateral spacing and flow rate in our baseline reservoir design using Darcy’s law (see calculations in ‘Scenario_Params.xlsx’ in Ricks and Jenkins [8]).

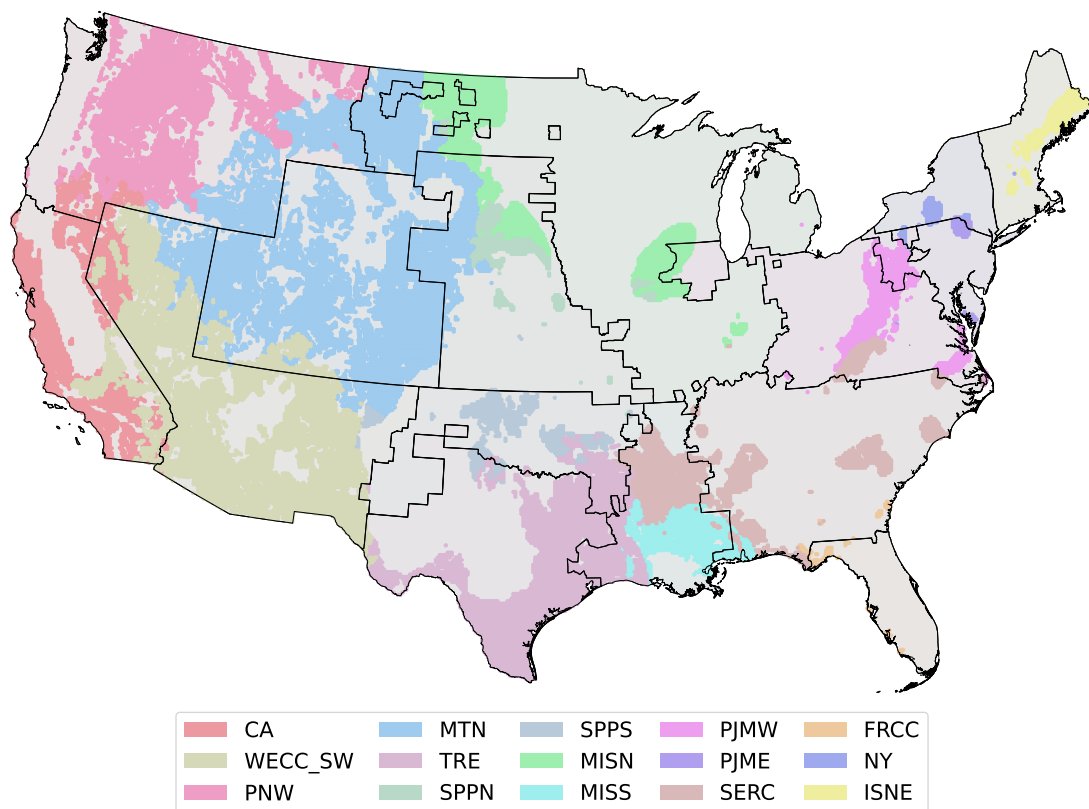
Finally, we use field data from the EGS demonstration project circulation test discussed in Norbeck and Latimer [15] to calibrate the expected pressure response of real EGS reservoirs under flexible operation. As part of this circulation test production and injection flow rates were intermittently modulated over a multi-day period to assess the performance of the system under flexible operating conditions. We select one of these cycles, in which the production flow rate was dropped from approximately 45 l/s to 0 l/s and held at that level for 10 hours while the injection rate remained constant, and use the recorded reservoir pressure response over this period to calibrate the sensitivity of our modeled reservoir bottomhole pressure to changes in flow rates, as described in Ricks et al. [12] and Ricks et al. [3]. While the 10 hour duration is not long enough to provide sufficient input data for the model (at least 50 hours is required), we observe that it is nearly identical in shape to the simulated pressure response functions used in Ricks et al. [3] over that 10-hour period. We therefore use the observed pressure response to scale the simulated response function (choosing the function from the ‘Low Subsurface Favorability’ simulation described in Ricks et al. [3] due to its similar shape), taking into account the different geometries of the field test reservoir and the simulated reservoir. We assume that to first order, the magnitude of the pressure response to a given change in flow rate is directly proportional to the total fracture surface area in the reservoir. Further assuming a similar number of active fracture pathways per unit of lateral

length between the actual and simulated reservoirs (based on the number of individual perforations used in stimulation [15]), we compare the length and cross-sectional dimensions of the reservoirs to obtain a scaling factor (see ‘Field_Coeffs.xlsx’ in Ricks and Jenkins [8]). In this calculation we assume that fractures at the field site occupy the full 0.11 km by 0.24 km cross-sectional area between the injection and production laterals, and half of the 0.24 km by 0.24 km area implied by reported fracture half-length and half-height measurements on the outside of each lateral. The re-scaled field pressure response function is shown alongside the simulated response function for the ‘Low Subsurface Favorability’ case from Ricks et al. [3] in Supplementary Figure 25, and indicates a slightly more muted pressure response to changes in flow than the simulation. We use this scaled response function for all flexible EGS plants modeled in this work, while recognizing the need for further field testing to fully characterize and bound the real-world behavior of these systems.



Supplementary Figure 25: Comparison between the 10-hour simulated reservoir pressure response resulting from an instantaneous reduction in production flow rate of 160 l/s from Ricks et al. [3], and field data from Norbeck and Latimer [15] that have been re-scaled to account for differences in flow rate and reservoir geometry.

To represent the very large number of EGS CPAs in the GenX model while maintaining computational feasibility, we group individual CPAs into larger clusters with similar characteristics. We first divide the full set of EGS CPAs into groups assigned to each GenX model zone, with zone assignment based on the regional grid to which the CPA can be interconnected at least cost (rather than the CPA’s physical location). Supplementary Figure 26 shows the full set of developable EGS CPAs for the Blackwell et al. [1] temperature-at-depth dataset broken down by assigned zones. Next, within each zone we divide CPAs into near-field and deep groupings, and subsequently by depth. Within each of these subgroups, we then apply a k-means clustering algorithm to group CPAs into a specified number of clusters with a specified maximum total capacity, such that variance in total annuitized per-kW cost within each cluster is minimized. For each cluster, all parameters are equal to the capacity-weighted average of the same parameters from its component CPAs. Each cluster is then assigned flexible EGS model parameters based on its temperature and depth following the procedure outlined in Ricks et al. [3] with the modifications described above. Finally, because this procedure creates a very large number of total clusters, we filter the full set by total annuitized cost before each GenX planning period to select only the least-cost options up to a specified maximum total capacity in each model zone, as well as those that had seen buildout of 50 MW or more in previous periods. The total number of selected EGS clusters varies, but is typically between 150 and 350 in each planning period.



Supplementary Figure 26: Map showing assignment of developable EGS CPAs in the Blackwell et al. [1] dataset to the GenX model zones shown in Supplementary Figure 10, based on least-cost interconnection pathways.

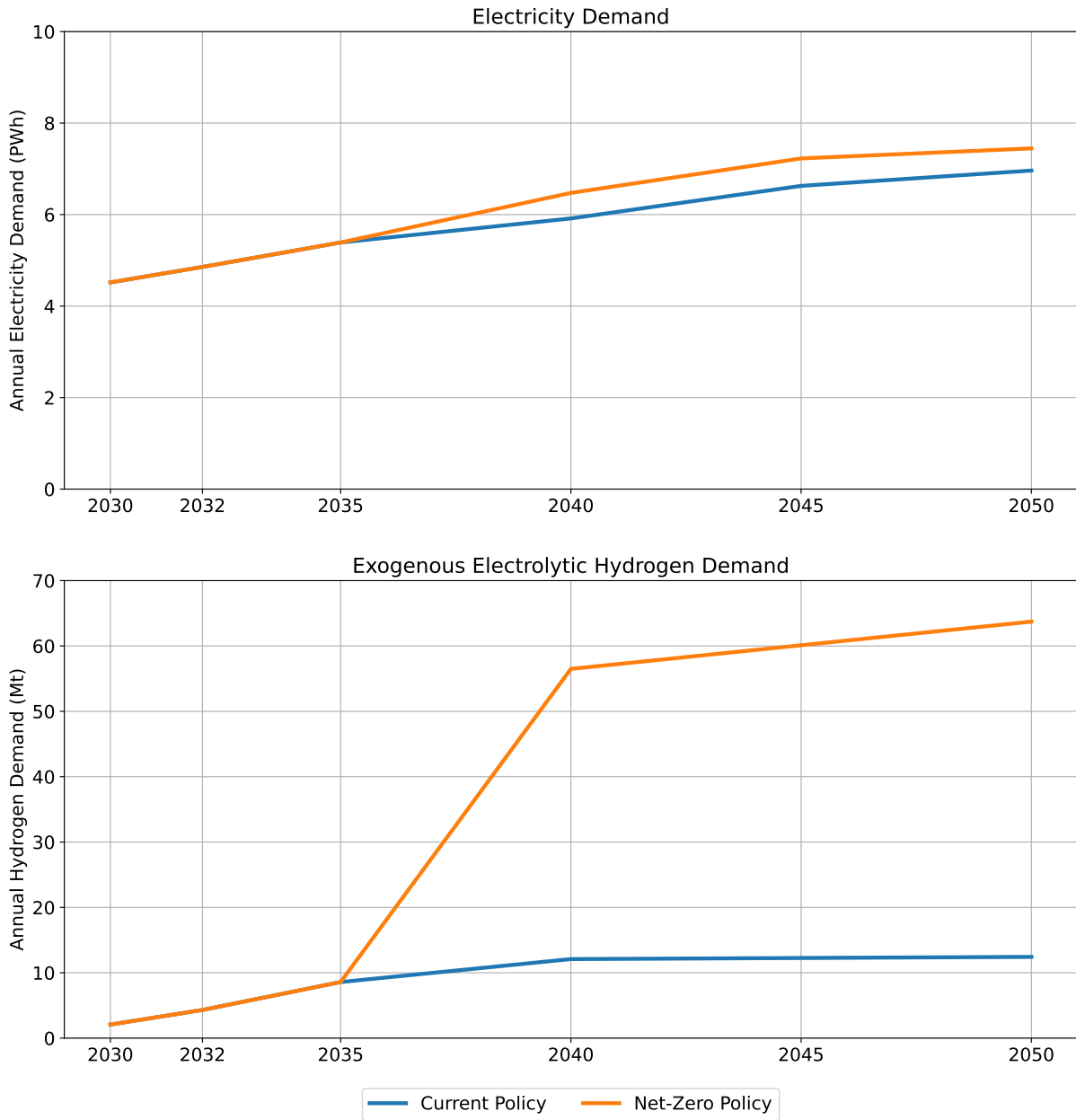
Supplementary Note 2.4: Non-EGS Input Data

The majority of non-EGS cost, system structure, and demand data used as inputs for the GenX model in this work are compiled using the PowerGenome tool [16]. PowerGenome sources projected cost, lifetime, and financial parameters for onshore and offshore wind power, solar photovoltaic power, lithium ion batteries, combined cycle gas power plants, and open-cycle gas combustion turbines from the 2023 edition of the US National Renewable Energy Laboratory’s Annual Technology Baseline (ATB) [4], using the ‘Moderate’ cost case and ‘Market Factors’ financial case for all technologies. For each planning period, technology cost inputs in GenX reflect the average of ATB costs for all years in that period. Capital costs for each new-build technology are modified by regional cost multipliers from the US Energy Information Administration’s Annual Energy Outlook (AEO) [17], and costs for wind and solar CPAs are modified to reflect regional grid interconnection costs using the same transmission routing workflow described above in the case of EGS CPAs. Wind, solar, and lithium ion battery costs for the ‘Low VRE and Battery Cost’ and ‘High VRE and Battery Cost’ are taken from the ATB’s ‘Advanced’ and ‘Conservative’ cost cases, respectively. Regional fuel costs for each planning year are taken from the AEO’s 2022 ‘Reference’ case, and fuel costs for the ‘High Natural Gas Price’ and ‘Low Natural Gas Price’ sensitivity scenarios shown in Figure 7 in the main paper are taken from the ‘High Resource’ and ‘Low Resource’ cases, respectively [18]. New-build and existing wind and solar sites, as well as existing thermal power plants, are grouped into clusters of similar projects using the same k-means clustering approach applied to EGS above, though without the need to filter by resource temperature and depth. Costs for hydrogen electrolyzers and geologic storage are not provided in the ATB, and are instead adopted from other sources. Following Murdoch et al. [19], we assume that electrolyzer costs start at \$1800/kW at present, decline linearly to \$900/kW by 2030 and \$600/kW by 2035, and by 0.5%/yr thereafter. We adopt a cost of \$2/kWh for geologic hydrogen storage from Viswanathan et al. [20], and apply this cost in all model regions. In the ‘Low Electrolyzer Cost and High Hydrogen Demand’ and ‘High Electrolyzer Cost and Low Hydrogen Demand’ sensitivity scenarios shown in Figure 7 in the main paper, we modify electrolyzer fixed costs by -25% and +33%, respectively. Hydrogen combustion turbine cost and performance assumptions are identical to those used for natural gas combustion turbines. For hydrothermal resources, we calculate costs for sites with remaining developable capacities greater than 50 MW listed in Williams et al. [9] using the EGS cost model described above, with the following modifications: costs for well laterals and stimulation are both removed, surface plant unit size is decreased from 50 MW to 25 MW, and all reservoirs are assumed to be at 2.5 km depth. All input data described above and the scripts used to compile it are available at Ricks and Jenkins [8]. Cost assumptions for Allam cycle gas plants and nuclear SMRs are discussed in the following section.

We adopt up-to-date state-level renewable portfolio standard (RPS) and clean energy standard (CES) policy requirement inputs for each planning year from Gagnon et al. [21]. For states or regions with carbon cap-and-trade policies covering the electricity sector (model zones CA, ISNE, NY, PJME, and PNW in Supplementary Figure 10), given non-modeled interactions with other economic sectors and deep uncertainties in future allowance prices, we assume a fixed allowance price of \$20/tCO₂ in all planning periods. At the federal level we model two broad sets of scenarios, ‘Current Policy’ and ‘Net-Zero Policy’. Both scenarios use electricity and exogenous electrolytic hydrogen demand inputs adopted from the mid-range, current policy case from Jenkins et al. [22] for planning periods through 2035. These inputs continue to be used in the Current Policy scenario from 2036 onward, while the Net-Zero scenarios switch to inputs adopted from the net-zero pathway benchmark case from Jenkins et al. [22]. These demand trajectories are shown in Supplementary Figure 27. In the ‘Low Electrolyzer Cost and High Hydrogen Demand’ and ‘High Electrolyzer Cost and Low Hydrogen Demand’ sensitivity scenarios shown in Figure 7 in the main paper, we modify exogenous hydrogen demand by +33% and -25%, respectively. For both current and net-zero policy scenarios we model electricity production, CCS, and clean hydrogen production subsidies put in place under the Inflation Reduction Act (IRA) [23]. We model section 45U tax credits for existing nuclear power plants as a mandate to keep these plants online through 2032. The section 45Q CCS credit and section 45V clean hydrogen production tax credit (PTC) are applied to all carbon sequestration by Allam cycle gas plants and qualifying clean hydrogen production from electrolyzers through 2035, accounting for safe harbor allowances after the official expiry of these credits in 2032. Subsidized clean hydrogen production is required to meet temporal and location matching requirements designed to minimize induced emissions, with locational matching occurring at the level of individual model zones. The Section 45Y PTC and Section 48E investment tax credit (ITC) for carbon-free electricity production and storage are applied through 2035 or whichever model stage sees US electricity sector greenhouse gas emissions fall below 25% of 2022 emissions at an absolute level, or roughly 0.38 GtCO₂e/yr. Emissions results are checked at the end of each model

stage to determine whether the 45Y and 48E subsidies remain in effect in the following stage. Onshore wind and solar resources are assumed to select the Section 48E ITC, and lithium-ion battery, geologic hydrogen storage, offshore wind, hydrothermal, EGS and nuclear SMR resources are assumed to select the 45Y PTC. We assume that all projects meet prevailing wage requirements necessary to unlock the full base credit value. We further assume that all battery, hydrogen storage, offshore wind, hydrothermal, EGS, and nuclear SMR resources benefit from a 10% credit adder for domestic manufacturing, and that nuclear SMR plants can always be preferentially sited to qualify for an additional 10% credit adder for projects located in ‘energy communities.’ For hydrothermal and EGS resources we map individual CPAs to energy communities as defined in Ene [24] and apply the appropriate ITC adder to CPAs that fall within the geographic boundaries of these communities. For wind and solar resources we assume that domestic manufacturing credit benefits largely cancel out the additional cost of domestic over foreign manufacturing, and we therefore do not apply the PTC domestic manufacturing adder for these resources. We use the same mapping approach as for geothermal CPAs to determine qualification of each wind and solar CPA for the PTC energy communities adder. For all resources receiving 45Y credits, we assume that 7.5% of the credit value is lost in the process of monetization. For all resources receiving a PTC (either 45Q, 45V, or 45Y PTCs) where the PTC credit period is shorter than the resource’s financial lifetime, we reduce the modeled value of the credits to reflect an equivalent net present value if applied over the full lifetime of the resource. For hydrogen electrolyzer projects, because the 45V credit represents the vast majority of project revenue, we assume that project financial lifetime is reduced to the PTC length of 10 years rather than the typical 30 while 45V is in effect.

For clean firm policy sensitivity cases shown in Figure 6 in the main paper, we modify model inputs as follows. In the ‘10% Clean Firm ITC Adder’ case, we include a further 10% adder to the 48E ITC for EGS, hydrothermal, and nuclear SMR resources. While we assume that Allam cycle gas plants do not receive 48E due to upstream methane emissions, we increase the 45Q subsidy by 10% as well to reflect similar support for these resources. In the ‘Early Clean Firm Deployment Mandate’ case, we enforce minimum capacity requirements in the model for EGS, nuclear SMR, and Allam cycle technologies of 1250 MW in 2032 and 4450 MW in 2035, close to the maximum allowable growth rate for these technologies. In the ‘24/7 Carbon-Free Electricity Demand’ case, we require that a fixed percentage of electricity demand be met by local, newly-deployed carbon-free resources, defined here as wind, solar, hydrothermal, EGS, nuclear SMRs, Allam cycle gas, and storage charged using these resources. The participating percentage of demand is set at 2.5% in 2032, 5% in 2035, and rises by 5% in every planning period thereafter. This demand is additive to any demand for time-matched carbon-free electricity from hydrogen electrolyzers receiving 45V subsidies.



Supplementary Figure 27: Electricity demand and exogenous electrolytic hydrogen demand assumptions, by year and scenario.

Supplementary Note 2.5: Cost and Learning Assumptions for Emerging Technologies

Initial costs used for emerging technologies are intended to represent ‘second-of-a-kind’ commercial deployments where the technology has been successfully de-risked via at least one large demonstration project but does not yet have a mature supply chain and has not yet benefited from significant learning-by-doing. For nuclear SMRs we adopt initial costs from the ATB [4], using the ‘Conservative’ cost case and ‘Market Factors’ financial case to represent the cost of a technology in the early stages of deployment. For Allam cycle gas plants we adopt CAPEX, fixed O&M cost, variable O&M cost, and heat rate values from White and Weiland [25], and financial assumptions for natural gas power plants with CCS from the ATB. We increase the CAPEX and fixed O&M values reported in White and Weiland [25] by 20% to account for the nascency of the technology, as their analysis assumed fully scaled-up supply chains. We additionally use PowerGenome to calculate CO₂ pipeline and injection facility fixed and variable costs for Allam cycle plants in each GenX model region. Due to the unavailability of suitable injection basins, Allam cycle plants are not deployable in the ISNE, NY, and PJME model regions. Similarly to other technologies, we use regional cost multipliers from the AEO to modify investment costs for nuclear SMRs and Allam cycle plants in each model zone. Average initial cost and performance parameters (not including regional multipliers or CO₂ disposal costs) are shown in Supplementary Table 1. For EGS plants we use site-specific costs calculated using the procedures described above. We adopt cost of capital figures for each emerging technology from the ATB, implicitly assuming that each is sufficiently demonstrated to access financing at typical rates.

Given the inherent lack of empirical data on learning rates for nascent technologies, we use technological analogues and the qualitative framework developed by Malhotra and Schmidt [26] to establish learning rates for nuclear SMRs, Allam cycle gas plants, and EGS. For nuclear SMRs and Allam cycle gas plants we follow the Malhotra and Schmidt [26] classification of these resources as ‘Type 3’ technologies with relatively high complexity but some potential for standardization, and therefore assign them both a default 5% learning rate. Malhotra and Schmidt [26] also classify conventional hydrothermal power as a Type 3 technology, as all aspects of hydrothermal wellfield development and power plant design must be customized to the unique conditions of a given hydrothermal reservoir. By contrast, without its reliance on naturally-occurring hydrothermal reservoirs, EGS offers a pathway to much more standardized reservoir and surface power plant designs. For EGS reservoirs we use unconventional oil and gas extraction - which applies nearly identical drilling and stimulation techniques - as the closest technological analogue. The only literature assessment of learning rates in this technology comes from Fukui et al. [27], who find a 13% learning rate based on wellhead gas prices, though this assessment does not take into account degrading resource quality or other non-learning factors that could affect price. Qualitatively, we consider EGS wellfields to be a ‘Type 2’ technology in the Malhotra and Schmidt [26] framework due to small unit sizes (individual wells) and the potential for mass standardization. We therefore assign a 15% default learning rate representative of this technology type. For binary-cycle EGS surface plants we note that while the technology has been applied at GW scale in hydrothermal contexts, lack of standardization due to small project sizes and variable reservoir conditions has limited opportunities for learning. Akar et al. [28] find that the cost of binary-cycle turbine systems could be reduced substantially through mass standardized manufacturing, implying significant learning potential if these systems are deployed in a standardized EGS context at large scale. We therefore consider binary-cycle surface plants to also be a Type 2 technology when deployed for EGS, but assign them a lower learning rate than wellfields - 10% - in recognition of their greater complexity and larger unit sizes.

Technology	Nuclear SMR	Allam cycle gas
CAPEX	9459	2777
Fixed O&M (\$/kW-yr)	119	74
Variable O&M (\$/MWh)	3	3.25
Heat Rate	10.45	7.07

Supplementary Table 1: Initial national average cost and performance assumptions for non-EGS clean firm technologies.

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