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Tallinn, Estonia. 13/06/2024

Dissemination event on CO<sub>2</sub> capture, transport, use and storage technology (CCUS)

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# **1 \_** CARBON CAPTURE IN WTE SECTOR

## 1.1 \_ A2A presentation

We deal with energy, water and the environment, through a circular use of natural resources.

#### Energy

We invest in the infinite energy generated by the sun, water and the wind.

#### Environment

We protect the environment by transforming waste and surplus material into new resources, reducing wastage.

#### **Smart infrastructure**

We distribute electricity and gas, drinking water and district heating. We light, connect and plan towns, cities and businesses using smart, digital infrastructures.





Total

141



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# **1** CARBON CAPTURE IN WTE SECTOR

## 1.2 A2A decarbonisation vision

#### Commitment to decarbonisation through tangible and measurable actions





#### Action Plan 2024-35

Net zero Scope 2 @20261 -60% Scope 3 upstream fuel2 Electrification of company's fleet 1 plant with Carbon Capture technology Reduction of production from CCGT

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#### Our integrated portfolio | TWh

📰 WtE¹ 📒 Solar 🔜 Wind 🔜 Hydro 🔜 CCGT 📰 Oil & Coal



A2A Strategic Plan 2024-2035















## 1.3 \_ What's a WtE?

The waste-to-energy plant is an essential element in an environmentally, technically and economically sustainable waste management system.

WtE are necessary to minimize waste disposal in landfill and to valorize, from an energy point of view, non-recyclable waste.

Many different technical configurations of WtE are possible (different types of: combustion chamber; flue gas treatment systems; power cycle configuration).

Below is a typical configuration of A2A WtE.

- A Waste bunker
- B Waste hopper **C** Combustion
- chamber
- D Boiler
- E Bottom ash
- F Turbine
- G Generator
- H Condenser/ heat exchanger

- O Dust S DeNO<sub>v</sub> T Cimnev
- M Sodium bicarbonate N Activate carbon
- O Reactor P Fabric filter
- R Ammonia Emission control

Electric energy

J Thermal energy

K ESP

CCUS chain demonstration

L Fly ash

(district heating)





Silla 2 WtE (Milano, Italy)







## 1.4 \_ WtE flue gas characteristics – Silla 2 (Milano WtE – year 2022)

Parameter	Process (average)	Process (max)	Stack (average)	Stack – legal emission limits (daily average)
0 <sub>2</sub> (%v)	7,95		10,45	
H <sub>2</sub> O (%v)	14,58	26,64	13,97	
CO <sub>2</sub> (%v) (*)			10,08	
CO (mg/Nm <sup>3</sup> )	10,04	407,01	10,84	
HCI (mg/Nm <sup>3</sup> )	743,12	2658,94	2,37	5
$NH_3$ (mg/Nm <sup>3</sup> )	0,67	45,24	0,92	5
NOx (mg/Nm <sup>3</sup> )	349,89	538,67	37,77	60
SOx (mg/Nm <sup>3</sup> )	87,12	431,73	2,65	15
TOC (mg/Nm <sup>3</sup> )			4,64	5
Dust (mg/Nm <sup>3</sup> )			0,24	3

Process: boiler outlet flue gas, before treatment.

Stack: flue gas at the point of emission (chimney).

Three elements must be considered in the application of carbon capture in WtE:

- High oxygen concentrations (in the range of 8 to 13%v).
- Low CO<sub>2</sub> concentrations, around 9 10% (compared to the typical value for: TGCC of 4%v; coal-fired power plant 14%v).
- Presence, although in small concentration, of some pollutants that can be critical for some types of carbon capture technologies. For example, SOx for MCFC.















#### **1.5** <u>Carbon Capture technologies</u>

Carbon capture technologies can be classified into **three main families**: pre-combustion, oxy-combustion and postcombustion.

The same technology can have different **Technological Readiness Level** (TRL) Depending on the specific application.

Three of these technologies are currently the most promising, for WtE applications:

- Amines.
- Molten carbonate fuel cells (MCFC)
- Calcium Looping.









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This slide was kindly provided by Maurizio Spinelli (researcher at Leap - <u>https://www.leap.polimi.it/</u>)





- MCFCs are fed by natural gas (NG) or other gaseous fuels converted into H<sub>2</sub> and electricity with high efficiency (up to~50%)
- They require a simple CO<sub>2</sub> purification unit (CPU) for (i) separating unconverted syngas and (ii) reaching CO<sub>2</sub> purity specifications
- CO<sub>2</sub> can potentially be captured to 90%, while enhancing electrical and thermal output of the host plant
- They have been lab tested for CO<sub>2</sub> capture from flue gas of coal- and NG-fired plants, but never on flue gas from WtE plants
- Low tolerance against side pollutants (e.g. SO<sub>2</sub>, metals)
- They feature very high CAPEX and OPEX (limited durability of the active layers of MCFC stacks, that must be substituted every 5-7 years)

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#### **1.5** <u>Carbon Capture technologies - Ammine</u>

Ammine are a commercially available technology with a high  $CO_2$  capture efficiency (over 90%) but currently characterized by high energy consumption per ton of  $CO_2$  captured

More information on amine technologies will be provided in the next slides by TPI, an EPC contractor with great expertise in this technology.







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#### 1.5 \_ Carbon Capture technologies - Calcium Looping



- The sorbent is regenerated by the reverse reaction (calcination,  $CaCO_3$ +heat -> CaO + CO<sub>2</sub>) sustained by oxyfuel combustion
- A continuous sorbent make-up (and a corresponding purge) is required to keep high reactivity and low ash build-up
- The high quality CaO-rich purge can be valorized as raw material for the production of clinker, cement or binders





## 1.5 <u>Carbon Capture technologies – Calcium Looping</u>

From the point of view of A2A, owner and operator of waste-to-energy plants, the Calcium Looping technology presents several positive and critical aspects, which must be studied.

plant or construction of a completely new plant).

Positive elements:

- Possibility of integration with current waste-to-energy technologies.
- Use of recovered solid fuel (CSS) for the calcination process.
- High CO2 capture efficiency.

Critical aspects to investigate:

- Process complexity (power cycle integration, treatment of combustion gases entering the CPU, ..).
- Implementation cost (two possible options: revamping of an existing plant or construction of a completely new plant).



Conceptual configuration of an integrated EfW+CaL power plant (by Herccules grant request documentation)







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## **2.1 \_ W.P.3 tasks and partners**

- Task 3.1: Engineering and erection of the dual fluidized bed CaL pilot with the CO<sub>2</sub> Purification Unit (CPU)
- Task 3.2: Preliminary characterization of Ca-based sorbents exposed to waste and sludge derived flue gases
- Task 3.3: Demonstration of the EfW-CaL system at TRL7-8
- Task 3.4: Process simulations and economic analysis of pilot and full-scale plants, calculation of KPIs and comparison with benchmark processes

Number of international partner involved:

- Leap (LABORATORIO ENERGIA AMBIENTE PIACENZA) and Polimi (POLITECNICO DI MILANO), for scientific coordination
- CSIC (AGENCIA ESTATAL CONSEJO SUPERIOR DE INVESTIGACIONES CIENTIFICAS), support at test matrix definition and Ca-based sorbent characterization
- LUT (LAPPEENRANNAN-LAHDEN TEKNILLINEN YLIOPISTO), performing CFD simulations of the oxyfuel calcination
- Sumitomo FW, technological provider leader in Calcium Looping technology (CaL unit engineering, construction and maintenance)
- Tecno Project Industriale, technological provider leader in CO2 Recovery Plants and biogas treatment process
- Air Liquide, technological provider responsible for liquid oxygen tank engineering, construction and maintenance and the service for the collection and valorization of the captured CO<sub>2</sub>
- A2A leader of WP3, owner and operator of the WtE plant in Milan, responsible for the connection of the pilot plant to the WtE in Milan and its operation.















# 2 \_ HERCCULES



## 2.2 \_ CaL pilot plant scheme

#### MAIN DATA

- Flue gas in input at the carbonator: 1,500 Nm<sup>3</sup>/h
- Cumulated hours of testing: > 4,000 hours
- Two kind of test:
  - at least 20 short tests;
  - 2 long duration tests (8 weeks each).
- SRF consumption: <200 kg/h
- Carbon dioxide captured: 2,500 (cumulative value)





# **12\_ HERCCULES**

## 2.3 \_ CaL pilot plant installation site

WtE Plant Milan – main data:



529.000 t/year WASTE BURNED covers the need for Milan city and part of the





hinterland



WtE Plant Milan - CaL Pilot Plant Installation Site







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# **3** TPI company



Design, production and installation of **CO<sub>2</sub> Carbon Capture** and CO<sub>2</sub> Recovery and Liquefaction Plants for all its applications according ISBT and EIGA quality guidelines



 $(\mathbf{CO}_2)$ 

With the support of SIAD, TPI offers optimized solutions for **Biomethane** liquefaction



Full range of **integrated service solutions**, digital services and aftersales. Remote supervision and direct access to After Sales Support - 24/7





# **3** TPI company



Ziemann Holvrieka

Carbacid (CO<sub>2</sub>) Limited





**SOL**GROUP a breath of life









\* list not exhaustive (TPI supplies covered by NDA)









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Clarke

Engineer - Install - Maintain

her A KOHLER COMPANY



AVR.

E.

# **3** TPI company

TPI's expertise in CO2 recovery encompasses Carbon Capture systems and liquefaction process.

Depending on CO2 concentration of the flue gas sources:

- Rich  $\rightarrow$  CO2 > 95%  $\longrightarrow$  Only liquefaction needed •
- Medium  $\rightarrow$  CO2 > 40% Poor  $\rightarrow$  > 10 % •
- Need extraction process
- •

General sources of CO2 are:

- Natural •
  - Deep wells
  - Natural Gas
- Waste streams from chemical process ٠
  - Ammonia (NH3) synthesis •
  - Ethylene Oxide
  - Bioethanol
  - Steam Reforming
  - Flue gas from combustion processes
- **Biological processes** 
  - Fermentation (bioethanol production)
  - Biogas







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CCUS chain demonstration









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#### **RESULTS FROM EXTRACTION SECTION**

- From a CO2 concentration at the inlet of the CO2 capture plant of **around** • 10%
- After the extraction section, a CO2 gas stream with **95% purity** is ready for recovery and liquefaction unit

#### UTILITIES

- **MEA consumption**: the «dirtier» the gas, the higher the consumption. It can be considered 2.5 – 3.0 kg MEA per ton LCO2 extracted
- Steam consumption: it can be considered 1.8 – 2.0 kg steam/kg LCO2 extracted
- **EE consumption**:

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- Extraction system: 220 250 kW/ton of LCO2 produced
- Next EE consumption  $\rightarrow$  CO2 recovery system: around 180 kW/ton of LCO2 produced















# 1 \_ CO2 recovery and liquefaction section









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# **1** CO2 RECOVERY AND LIQUEFACTION PLANTS











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# 3\_ LCO2 storage tanks



- Final product has **CO2 purity > 99,9%v/v**
- **CO2** is storaged in cryogenic tanks:
  - pressure at 11 / 18 barg
  - temperature between -35 / -20 ° C
- Lastly, transfer pumps are used to fill roadtanks



Image taken from AVR website - https://www.avr.nl/en/







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# **3\_ Some pictures from The Netherlands**



3D model from Press release - 29-05-2018 - AVR website - https://www.avr.nl/en/

Image taken from AVR website - https://www.avr.nl/en/









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## **3\_ Some pictures from The Netherlands**







Images taken from AVR website - https://www.avr.nl/en/







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