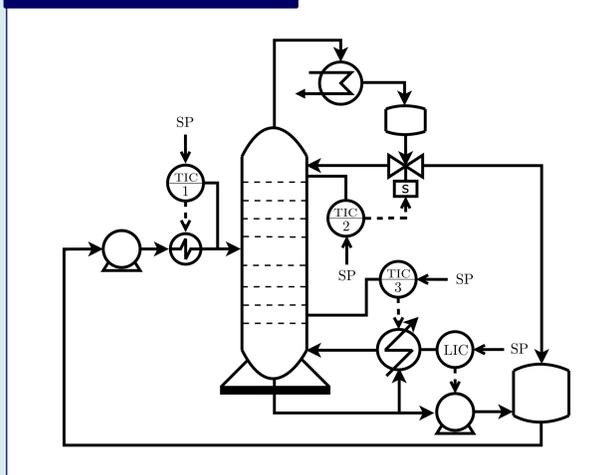


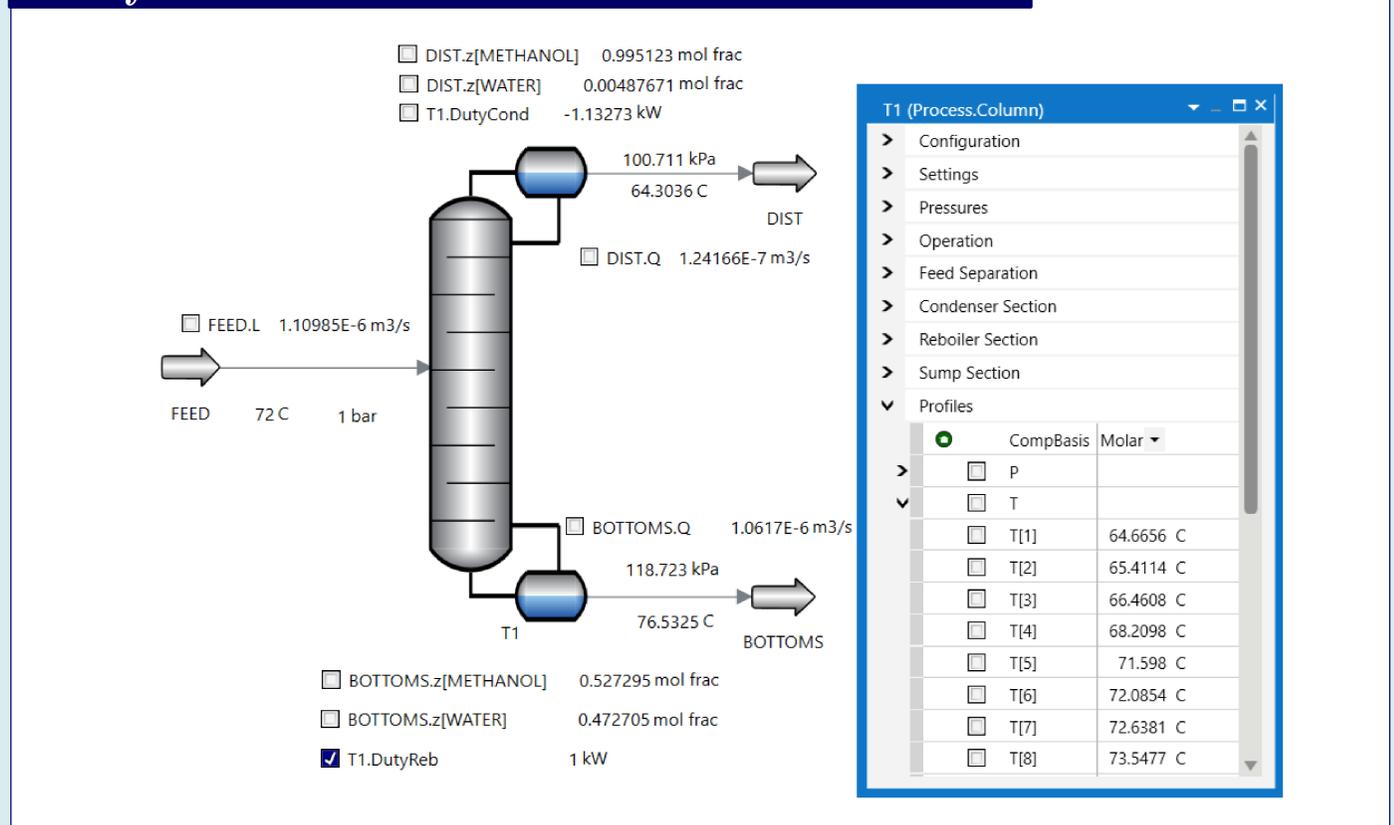
## Goals

Distillation columns are essential units in chemical engineering used for separating mixtures into their individual components. They operate based on the principle differences in volatility between the components of a mixture. Our goal is to control a laboratory distillation column with methanol-water mixture.

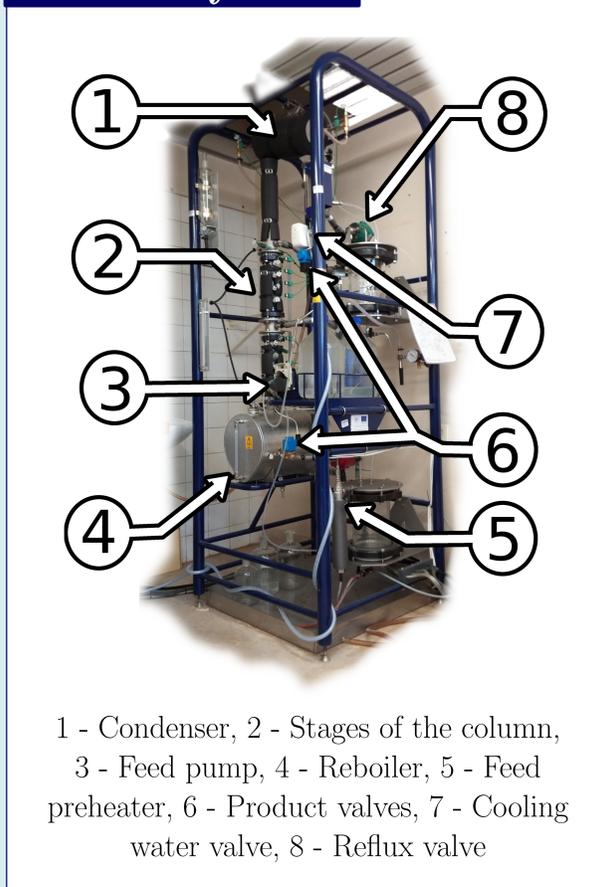
## P&ID Scheme



## Steady-State Model in AVEVA Process Simulation



## Laboratory Plant



## PI Controller Tuning

Plant model - transfer function (TF):

$$G(s) = \frac{\text{outputs } Y(s)}{\text{inputs } U(s)} = \frac{K}{Ts + 1} e^{-\tau s}$$

TF (bottom temperature and reboiler duty):

$$G(s) = \frac{T_8(s)}{Q_B(s)} = \frac{7.5}{8.3s + 1}$$

TF (top temperature and reflux ratio):

$$G(s) = \frac{T_1(s)}{R(s)} = \frac{-0.1142}{112.1s + 1}$$

Control law (PI controller):

$$u(t) = K_p(w(t) - y(t)) + \frac{K_p}{T_i} \int_0^t w(t) - y(t) dt$$

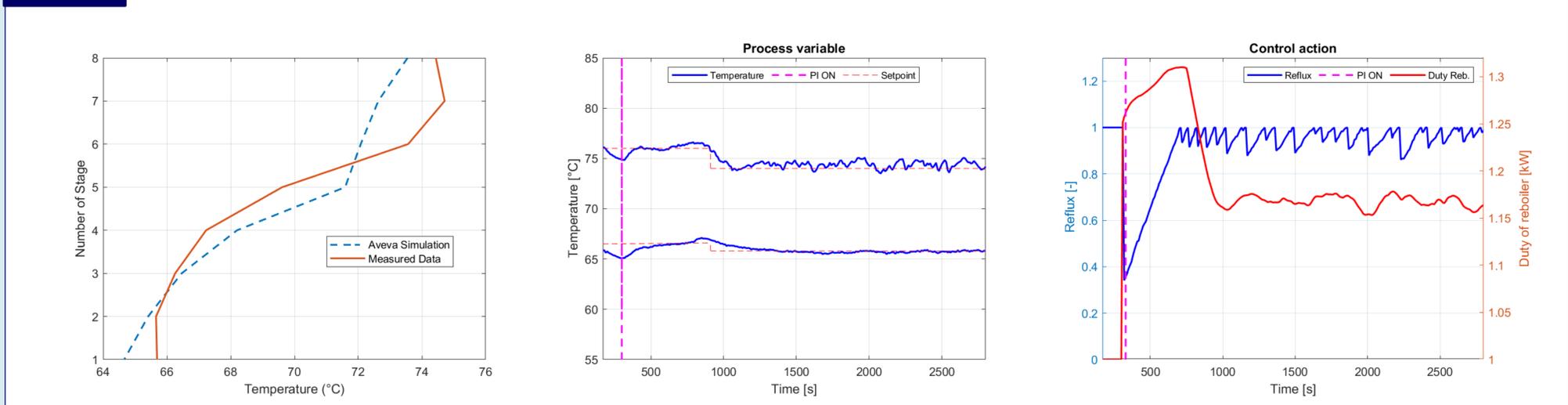
Proportional gain:

$$K_p = \frac{T}{K(T_c + \tau)}$$

Integral time constant:

$$T_i = \min[T, 4(T_c + \tau)]$$

## Results



## Conclusions

The experimental column control exhibited promising results, with stable temperature and composition profiles very similar to the steady-state model. This highlights the efficacy of the control algorithm in optimizing process parameters and ensuring high-quality product output.