

Control of a Laboratory Distillation Column with Methanol-Water Mixture

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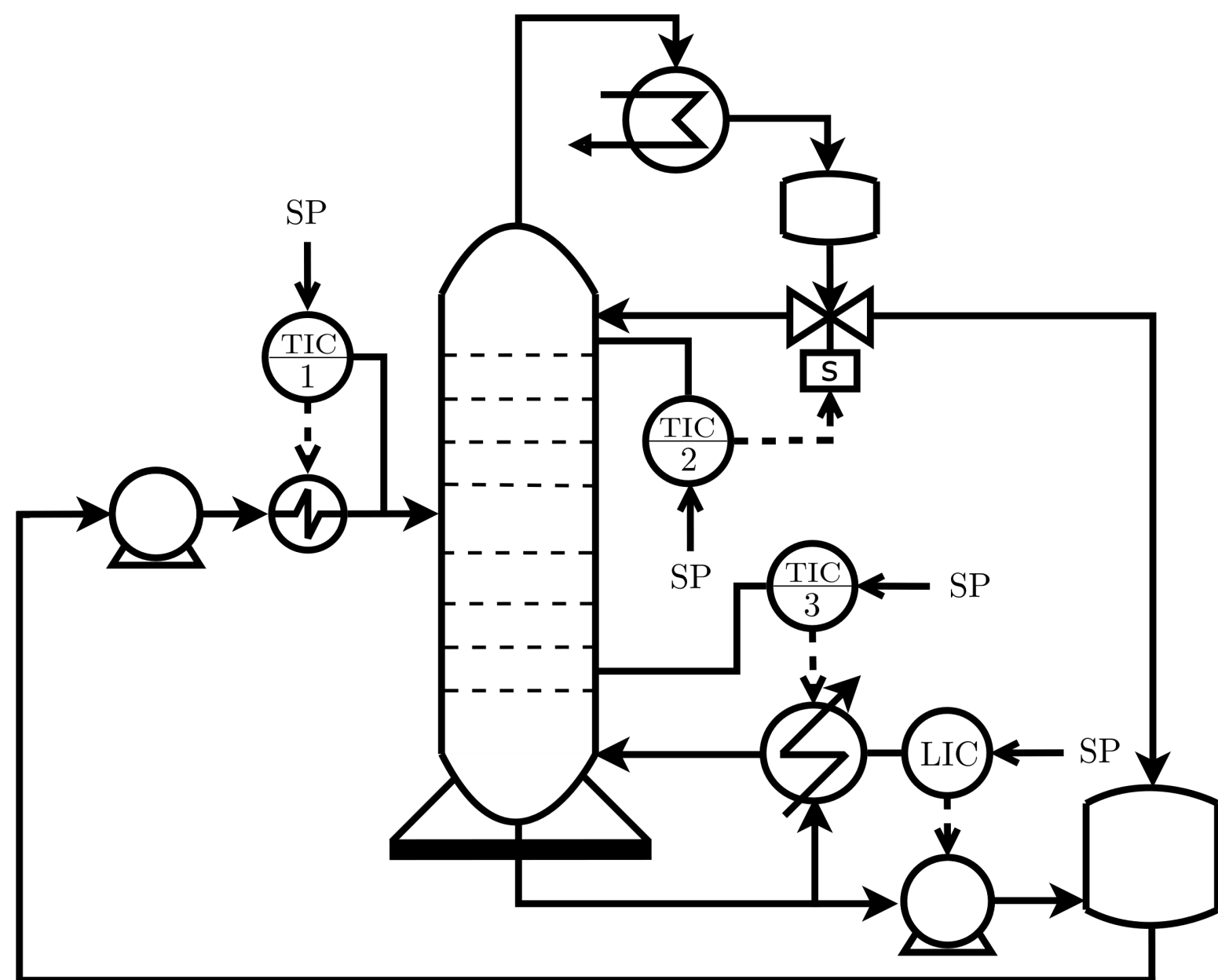
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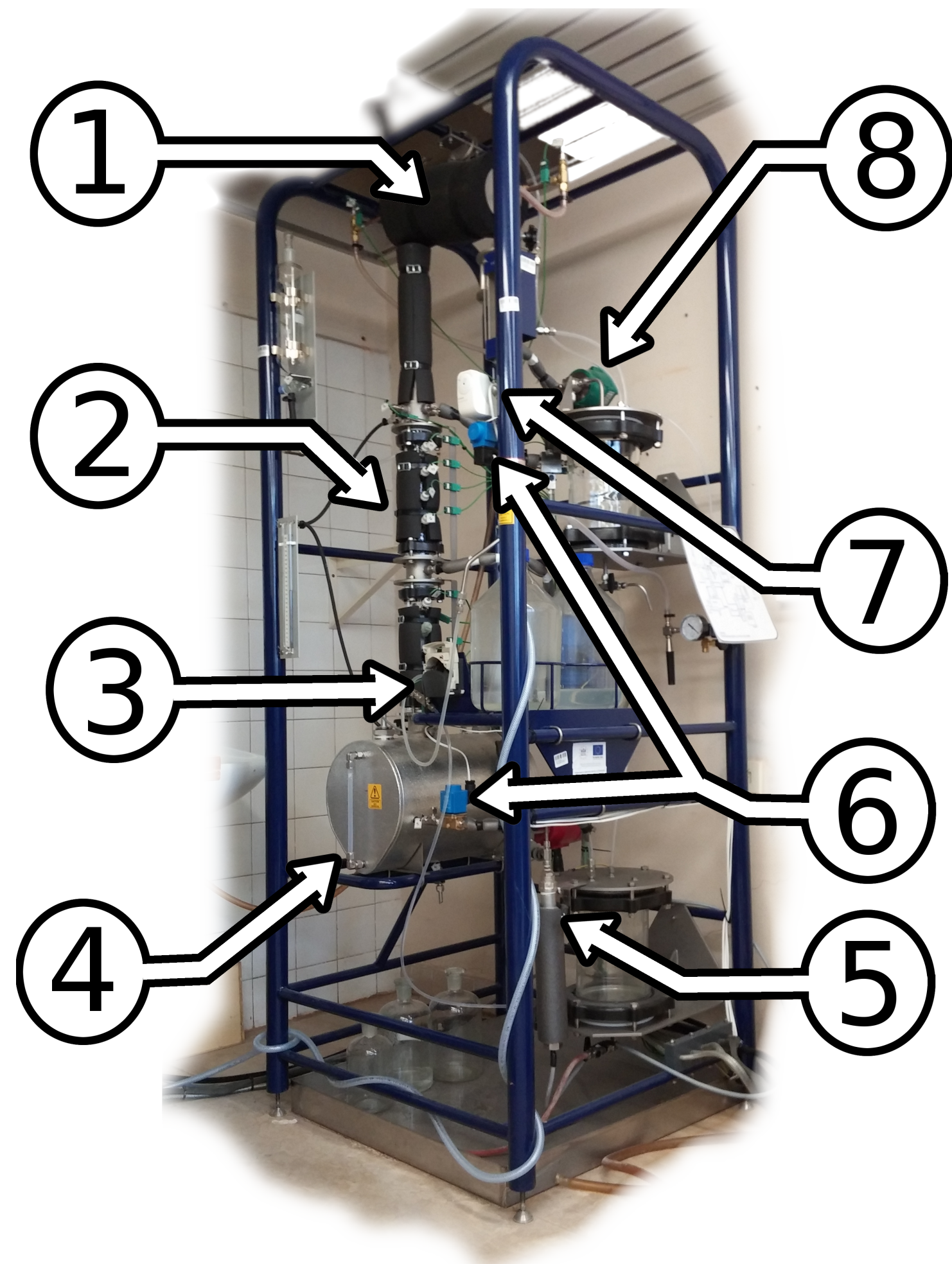
Goals

Distillation columns are essential units in chemical engineering used for separating mixtures into their individual components. They operate based on the principle differences in volatility between the components of a mixture. Our goal is to control a laboratory distillation column with methanol-water mixture.

P&ID Scheme

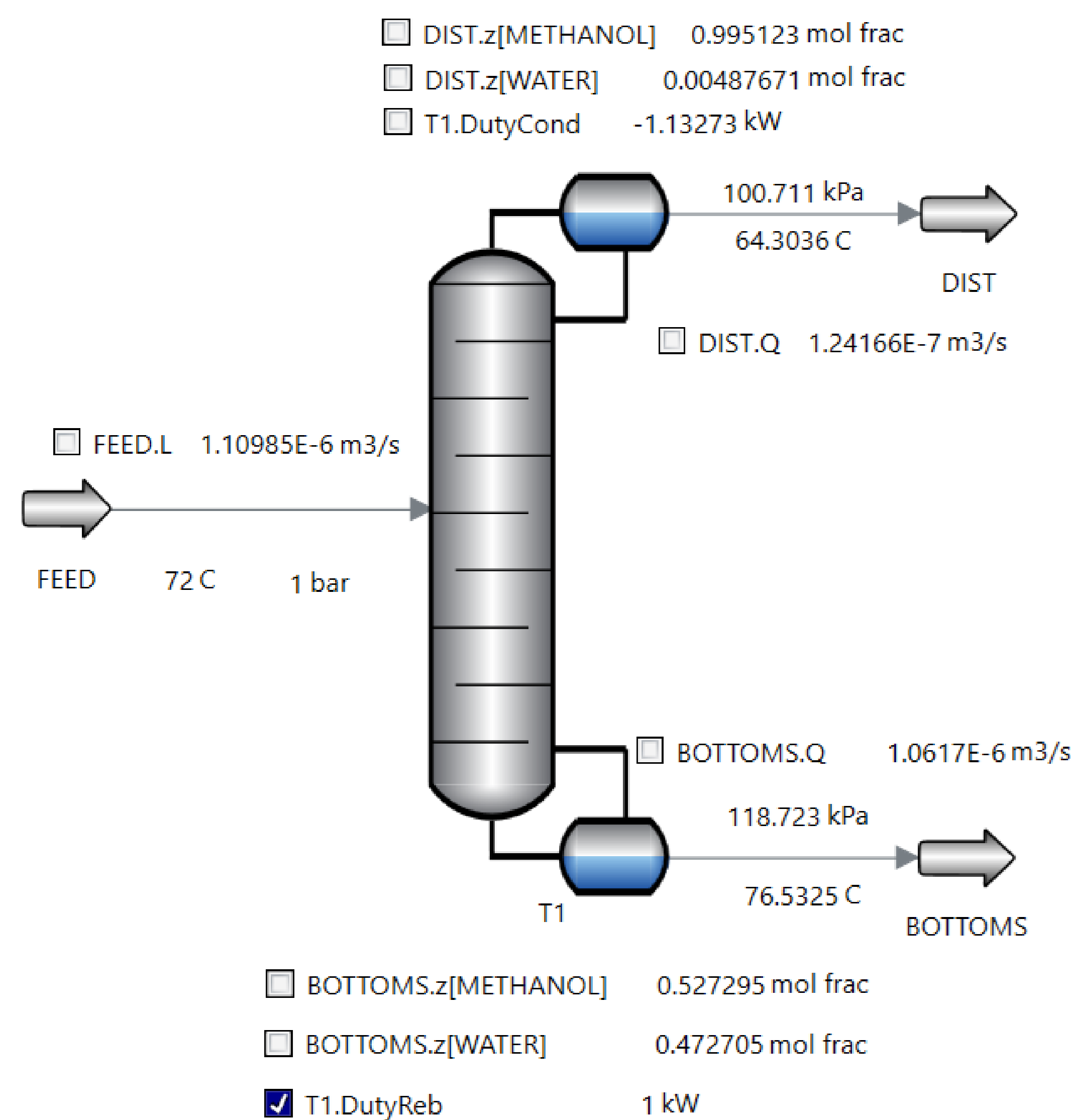


Laboratory Plant



1 - Condenser, 2 - Stages of the column,
3 - Feed pump, 4 - Reboiler, 5 - Feed
preheater, 6 - Product valves, 7 - Cooling
water valve, 8 - Reflux valve

Steady-State Model in AVEVA Process Simulation



T1 (Process.Column)		
>	Configuration	
>	Settings	
>	Pressures	
>	Operation	
>	Feed Separation	
>	Condenser Section	
>	Reboiler Section	
>	Sump Section	
>	Profiles	
>	CompBasis	Molar
>	P	
>	T	
>	T[1]	64.6656 C
>	T[2]	65.4114 C
>	T[3]	66.4608 C
>	T[4]	68.2098 C
>	T[5]	71.598 C
>	T[6]	72.0854 C
>	T[7]	72.6381 C
>	T[8]	73.5477 C

PI Controller Tuning

Plant model - transfer function (TF):

$$G(s) = \frac{\text{outputs } Y(s)}{\text{inputs } U(s)} = \frac{K}{Ts + 1} e^{-\tau s}$$

TF (bottom temperature and reboiler duty):

$$G(s) = \frac{T_8(s)}{Q_B(s)} = \frac{7.5}{8.3s + 1}$$

TF (top temperature and reflux ratio):

$$G(s) = \frac{T_1(s)}{R(s)} = \frac{-0.1142}{112.1s + 1}$$

Control law (PI controller):

$$u(t) = K_p(w(t) - y(t)) + \frac{K_p}{T_i} \int_0^t w(t) - y(t) dt$$

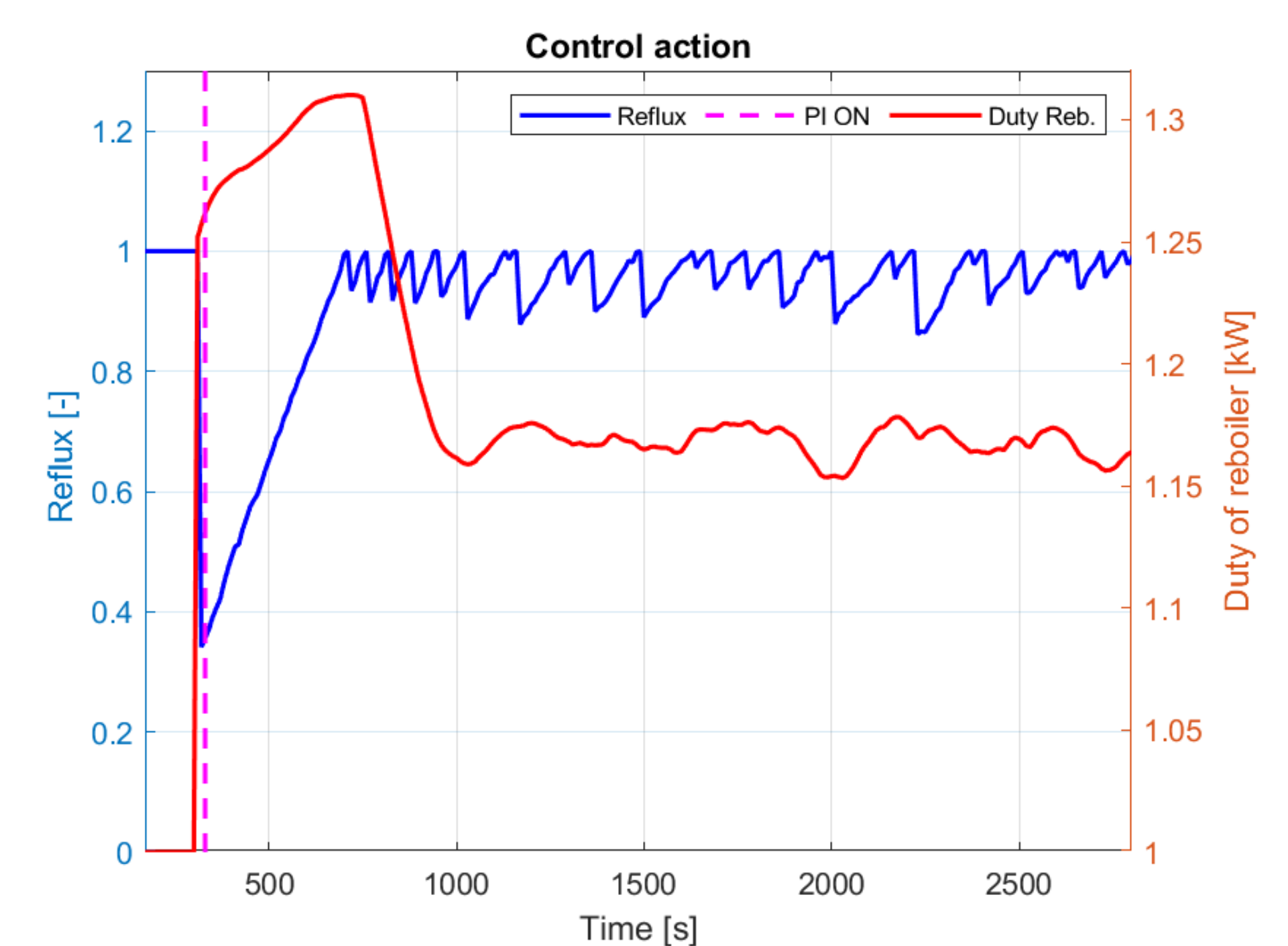
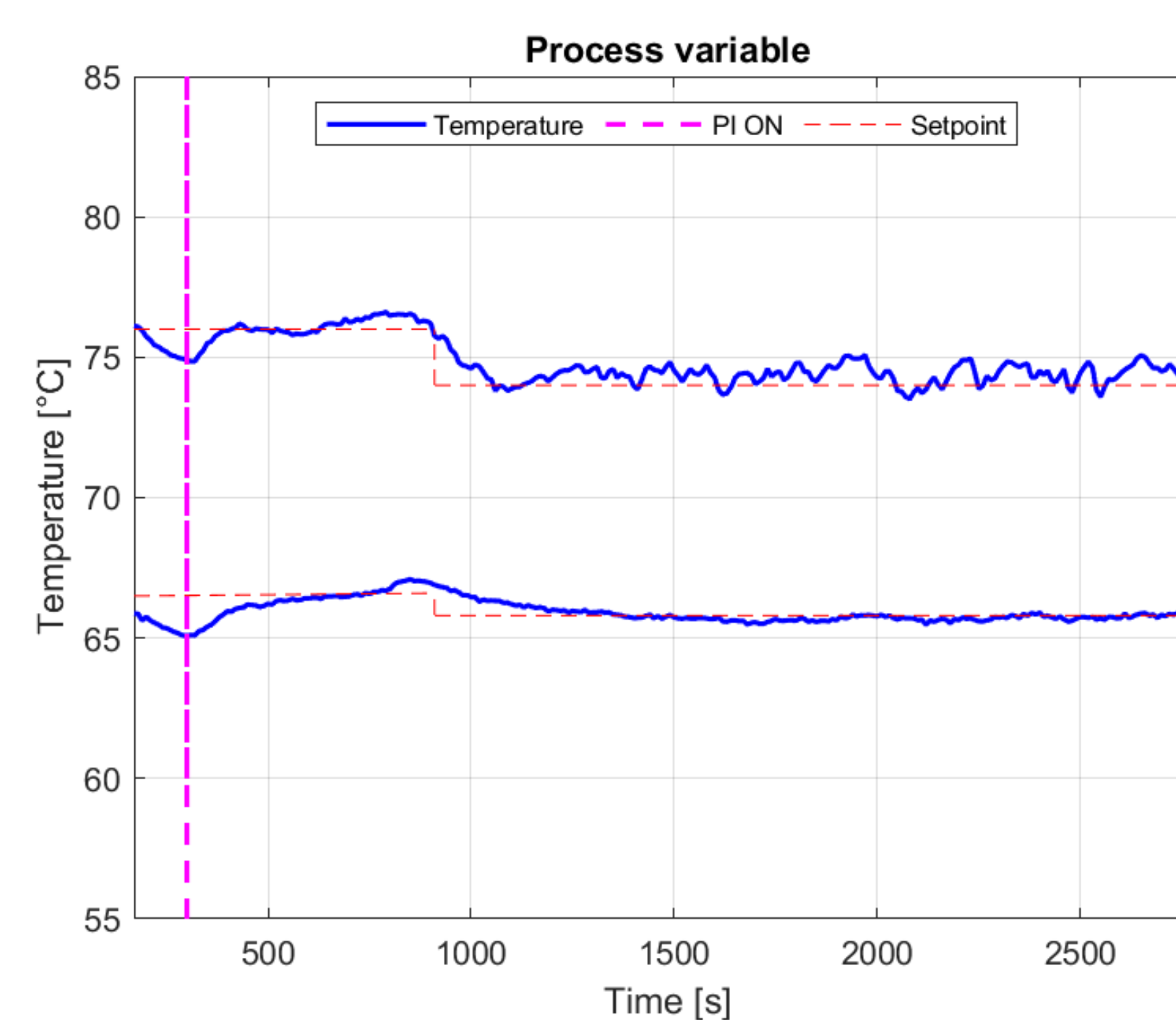
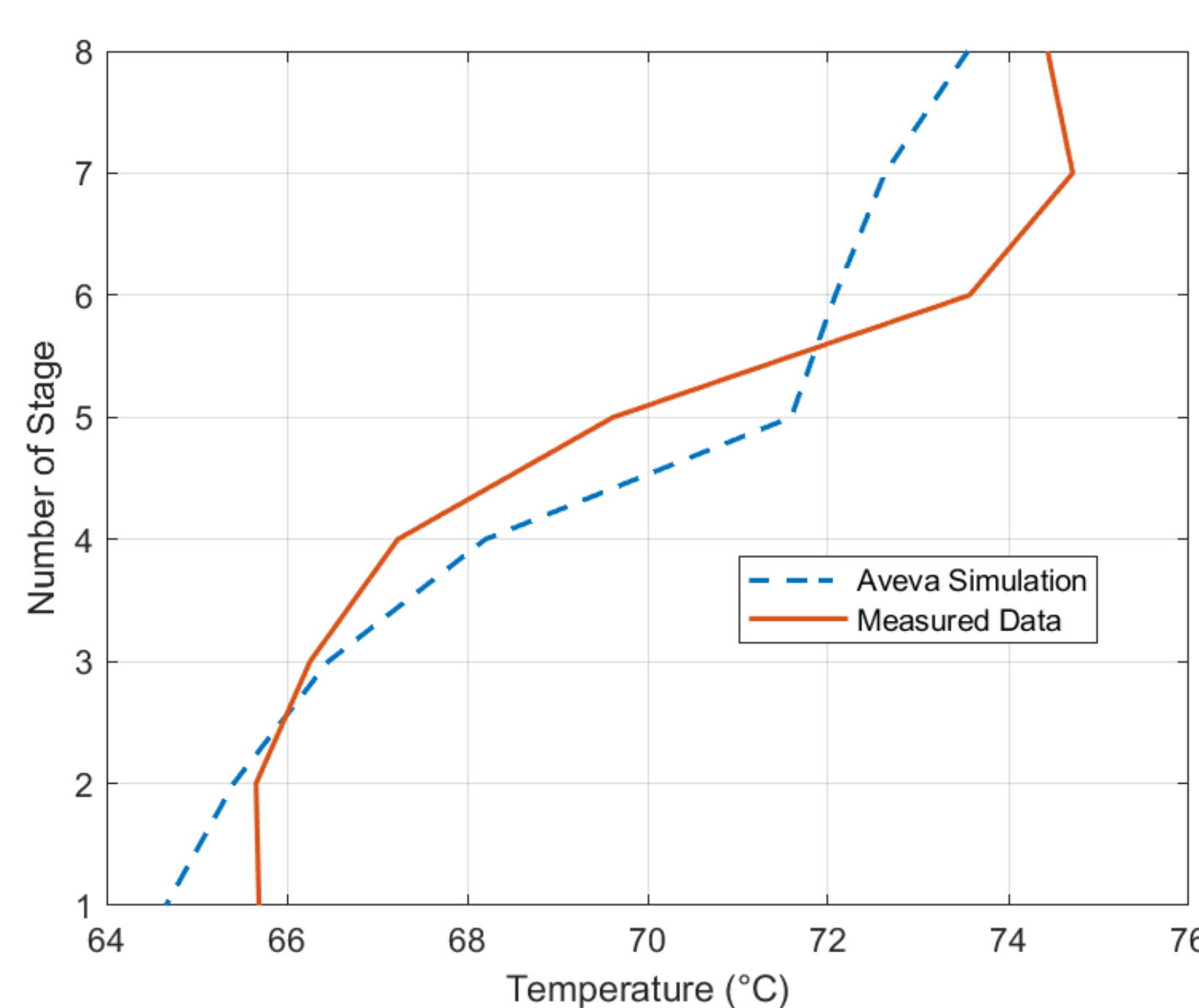
Proportional gain:

$$K_p = \frac{T}{K(T_c + \tau)}$$

Integral time constant:

$$T_i = \min[T, 4(T_c + \tau)]$$

Results



Conclusions

The experimental column control exhibited promising results, with stable temperature and composition profiles very similar to the steady-state model. This highlights the efficacy of the control algorithm in optimizing process parameters and ensuring high-quality product output.